

1 **Investigation of TiO₂-Impregnated Laterite (TIL) as an Adsorbent for**

2 **Arsenic Removal in Aqueous Media**

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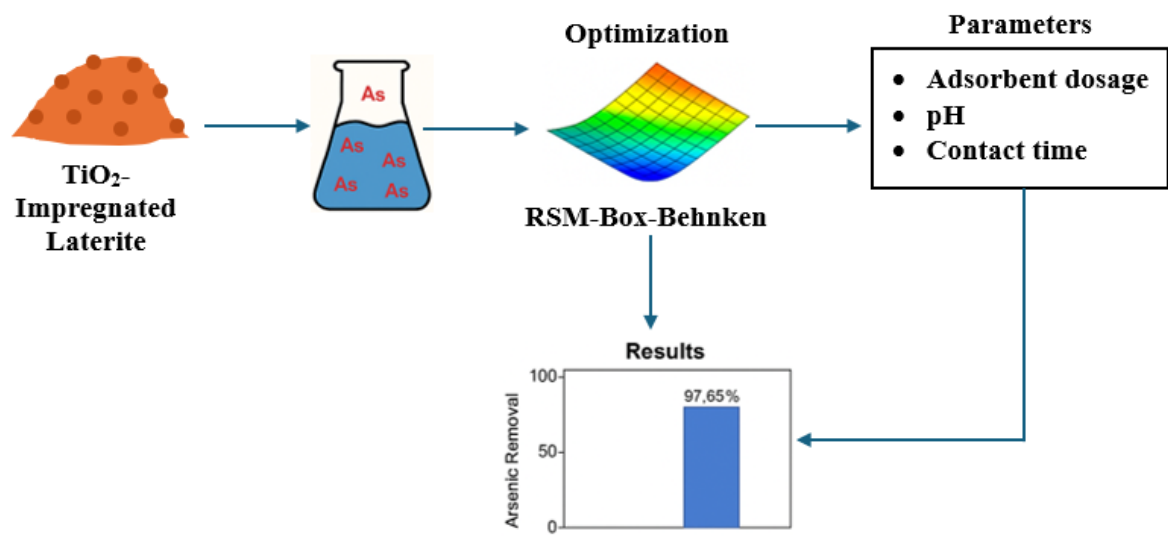
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14 **Graphical Abstract**



15

16 **Abstract**

17 Arsenic contamination in groundwater poses a critical threat to public health, particularly in
18 developing regions. This study investigates the potential of TiO₂-impregnated laterite (TIL) as a cost-
19 effective and sustainable adsorbent for arsenic removal from aqueous solutions. A Box–Behnken
20 design within the framework of Response Surface Methodology (RSM) was employed to optimize
21 three key operational parameters: adsorbent dosage, solution pH, and contact time. The TiO₂-laterite
22 composite was synthesized through impregnation, aging, and calcination processes to enhance
23 adsorption capacity. Experimental results indicated that adsorbent dosage and reaction time had
24 significant effects on arsenic removal efficiency, whereas pH had a minor influence within the tested
25 range. Under optimized conditions (0.99 g dosage, pH 5.3, 71 minutes), the process achieved 97.65%
26 arsenic removal, closely matching the model-predicted 98.82% with $R^2 = 0.996$. These results
27 demonstrate strong model reliability and high performance of the TiO₂-laterite composite. The
28 findings demonstrate that TiO₂-impregnated laterite is a promising material for arsenic remediation,
29 offering high performance, economic feasibility, and scalability. However, further research is needed
30 to validate performance under field conditions, analysis material characterization, assess long-term
31 stability, and explore regeneration capacity.

Key words: TiO₂-Impregnated Laterite, adsorption, arsenic removal, water treatment, process optimization.

1. INTRODUCTION

Arsenic contamination in groundwater poses a critical threat to environmental sustainability and public health, particularly in South and Southeast Asia, where millions of people rely on arsenic-laden aquifers for drinking water and daily use (Shaji et al., 2021). Recognized as a Group I carcinogen by the World Health Organization (WHO, 2019), chronic exposure to arsenic—even at low concentrations—has been associated with a range of severe health conditions including skin lesions, cardiovascular diseases, developmental impairments, and various cancers (Aredes & Pawlik, 2013; Jadhav et al., 2015). Arsenic typically exists in water in inorganic forms as arsenite [As(III)] and arsenate [As(V)], with the former being more mobile and toxic (Smedley & Kinniburgh, 2001). The complex geochemical behavior of arsenic in subsurface environments, coupled with limited infrastructure in many affected regions, makes its remediation particularly challenging (Carrard et al., 2019; McCarty et al., 2011).

A range of physicochemical technologies has been developed for arsenic removal, including ion exchange, membrane filtration, electrocoagulation, and adsorption (Alkurdi et al., 2019; Mollah et al., 2001). Among these, adsorption has emerged as a promising approach due to its operational simplicity, low cost, and scalability, especially in decentralized or resource-limited settings (Simonič, 2009). Naturally occurring materials such as laterite—a weathered soil rich in iron and aluminum oxides—have shown significant potential as cost-effective adsorbents for contaminant removal from water (Iriel et al., 2017). However, the adsorption capacity of unmodified laterite is often limited, prompting research into surface modification strategies to enhance its performance.

The utilization of modified laterite in wastewater treatment has garnered increasing attention due to its potential as an effective and sustainable adsorbent material. Vu et al. (2020) demonstrated that nanocomposite materials based on polyanion-modified laterite, specifically with polystyrene

57 sulfonate (PSS), exhibit high performance in removing antibiotics such as tetracycline from
58 wastewater. This indicates that chemical modification of laterite can enhance its adsorption
59 capabilities for specific contaminants, making it a promising candidate for targeted pollutant removal
60 (Vu et al., 2020). Further research by Nidheesh et al. (2021) explored the application of alkali-
61 modified laterite soil as a heterogeneous catalyst in combined electro-Fenton and electrocoagulation
62 processes for industrial wastewater treatment. The study found that modification of laterite improved
63 the efficiency of pollutant degradation, highlighting the importance of surface modifications in
64 enhancing the reactivity and treatment performance of laterite-based materials (P.V et al., 2021).
65 Similarly, Changduang et al. (2021) developed reactive iron-coated natural filter media, which
66 included modifications to natural materials like laterite, to effectively treat antibiotic residuals in
67 swine wastewater, emphasizing the role of surface coatings in improving contaminant removal
68 mechanisms (Changduang et al., 2021). Besides, Tuan et al. (2025) research team also conducted
69 experiments and investigated the ability to treat Arsenic in wastewater by adsorption of laterite
70 modified with KMnO_4 . The results confirmed that KMnO_4 -modified laterite is a promising material
71 for arsenic remediation, offering a sustainable and scalable solution (Tuan et al., 2025). In addition to
72 chemical modifications, physical and structural enhancements of laterite have been investigated. For
73 instance, Zhao et al. (2020) discussed the broader application of various flocculants, including
74 modified polymeric flocculants, in oily wastewater treatment, suggesting that modifications to natural
75 materials like laterite could be integrated with such flocculants to improve coagulation and
76 flocculation processes (Zhao et al., 2020). Although not specific to laterite, this indicates the potential
77 for combining surface modifications with other treatment agents to optimize removal efficiencies.
78 The environmental implications and scalability of modified laterite are also considered critical. Guo
79 et al. (2023) provided a life-cycle assessment of wastewater treatment processes, including the use of
80 modified materials, emphasizing the need to balance treatment efficacy with energy consumption and
81 resource use (Guo et al., 2023). Surface engineering of nanostructured adsorbents, as discussed by
82 Zhang et al. (2024), further underscores the importance of developing environmentally safe and

83 scalable modified adsorbents, which could include modified laterite, for future wastewater treatment
84 applications (Zhang et al., 2024). Overall, the body of research suggests that chemical and physical
85 modifications of laterite significantly enhance its adsorption and catalytic properties, making it a
86 versatile material for removing a wide range of contaminants from wastewater. These modifications
87 not only improve treatment performance but also align with sustainability goals by utilizing natural
88 and abundant resources, as highlighted across multiple studies.

89 Following the advancement, the recent studies have demonstrated that impregnating laterite with
90 metal oxides or nanoparticles can significantly increase its surface area, active sites, and affinity for
91 specific pollutants (Mostafa et al., 2025; Singh & Maiti, 2024). In particular, titanium dioxide (TiO_2),
92 a widely studied photocatalyst and adsorbent, has attracted attention due to its strong affinity for
93 oxyanions, high stability, and environmental compatibility (Gatou et al., 2024). When immobilized
94 on porous supports such as laterite, TiO_2 can enhance arsenic uptake via surface complexation and
95 redox reactions, while potentially maintaining cost-effectiveness for large-scale deployment (Maiti et
96 al., 2012). Also, TiO_2 offers dual advantages—surface activation and photocatalytic oxidation—
97 which are absent in traditional modifiers like KMnO_4 or PSS. Its environmental safety and proven
98 performance in oxyanion removal justify its selection.

99 This study aims to investigate the effectiveness of TiO_2 -impregnated laterite (TIL) as an adsorbent
100 for arsenic removal from aqueous solutions. A Box–Behnken design within the Response Surface
101 Methodology (RSM) framework was employed to evaluate the effects of key operational
102 parameters—including adsorbent dosage, solution pH, and contact time—on arsenic removal
103 efficiency. The study further seeks to determine the optimal conditions for maximum removal and
104 assess the viability of TIL as a low-cost, sustainable adsorbent for arsenic remediation in real-world
105 applications.

106 2. METHODOLOGY

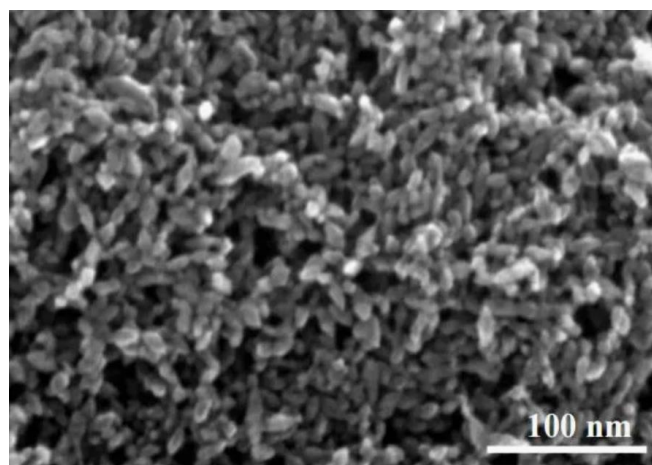
107 2.1. Preparation of Arsenic-contaminated wastewater

108 In this study, approximately 5 liters of synthetic arsenic-contaminated wastewater were prepared by
109 diluting a 500 ppm arsenic AAS standard solution with deionized water to replicate polluted
110 conditions under controlled laboratory settings. The initial arsenic concentration was set at 100 ppb,
111 intentionally higher than typical concentrations found in natural groundwater, to provide a rigorous
112 assessment of the removal efficiency. Prior to the adsorption experiments, the pH of each solution
113 was measured and adjusted to the target values using sodium hydroxide (NaOH) to raise the pH or
114 hydrochloric acid (HCl) to lower it. Once the desired pH was achieved, the adsorption process
115 commenced, enabling the evaluation of arsenic removal performance under consistent and
116 reproducible conditions within the defined experimental parameters.

117 **2.2. Preparation of TiO₂-Impregnated Laterite**

118 Nano titanium dioxide, purity 99.8%, particle size 5-10nm, was provided by Biotio Shanghai Corp
119 Co., LTD. The size characteristics of Nano titanium dioxide are shown in Figure 1. To prepare the
120 TiO₂-impregnated laterite (TIL) adsorbent, natural laterite was first collected, washed thoroughly with
121 tap water followed by deionized water to remove dust and surface impurities, then oven-dried at
122 105°C for 24 hours. The dried material was crushed and sieved to obtain a uniform particle size of 4–
123 5 mm. Take the ordinary laboratory beaker, add 200ml deionized water and 2.0g nano TiO₂ powder,
124 and stir well. The nanometer titanium dioxide has the characteristics of easy precipitation, so it is
125 necessary to add a certain amount of Sodium Lauryl Sulfate (K12) to the beaker, which can make
126 nano titanium dioxide suspended in the beaker uniformly for 30 min. Then put the beaker in an
127 ultrasonic oscillator, so that the nano carbon dioxide can be uniformly dispersed in the deionized
128 water. The laterite particles were then immersed in the TiO₂ solution at a solid-to-liquid ratio of 1:10
129 (weight/volume) and stirred for 4 hours to ensure uniform impregnation. After impregnation, the
130 material was aged at room temperature for 12 hours, followed by filtration and drying at 105°C for
131 another 12 hours. Finally, the dried composite was calcined in a muffle furnace at 450°C for 3 hours
132 to convert the precursor into crystalline TiO₂ and enhance the surface interaction between the laterite

133 matrix and the titanium dioxide coating. The resulting TiO₂-impregnated laterite was stored in airtight
134 containers for further characterization and use in adsorption experiments.



135
136 **Figure 1.** The size characteristics of Nano titanium dioxide¹

137 **2.3. Box–Behnken experimental design**

138 The Box–Behnken design (BBD), a statistical approach within the broader framework of response
139 surface methodology (RSM), is widely utilized to optimize processes and evaluate the influence of
140 multiple variables and their interactions on a given response (Ferreira et al., 2007). In this research,
141 BBD was applied to investigate how key operational parameters affect arsenic removal efficiency and
142 to optimize the adsorption conditions accordingly. Unlike full factorial designs, BBD employs a three-
143 level, incomplete factorial structure, enabling the modeling of nonlinear or quadratic effects with
144 fewer experimental runs. This approach enhances efficiency by reducing the number of required tests,
145 thereby saving time and resources while maintaining statistical robustness.

146 Design-Expert software (version 13) was used to construct the experimental matrix, analyze the
147 results, and determine optimal process conditions for arsenic adsorption. The software facilitated the
148 development of a predictive response surface model by fitting experimental data and estimating the
149 coefficients associated with each factor. The independent variables assessed in this study were
150 adsorbent dosage, solution pH, and reaction time. These parameters were varied within defined

¹ Provided by chemical vendor.

limits—dosage (0.01–1.0 g), pH (2–9), and reaction time (10–80 minutes)—based on prior experimental evidence to ensure relevance. Each factor was encoded at three levels: low (–1), center (0), and high (+1), allowing the exploration of curvature and complex interactions among variables.

In this study, the adsorption of arsenic from aqueous solutions was investigated using TiO₂-Impregnated Laterite to enhance the natural laterite adsorption capacity. Batch adsorption experiments were conducted by mixing known concentrations of arsenic-contaminated water with a fixed dose of the modified laterite under varying conditions of pH, contact time, adsorbent dosage, and initial arsenic concentration as designed by BBD. The mixtures were agitated at constant temperature, then filtered, and the residual arsenic concentration was collected in 200 mL amber bottles to prevent light-induced reactions, and the residual arsenic concentrations were measured using Inductively Coupled Plasma Atomic Emission Spectroscopy (ICP-AES). For accuracy, the initial arsenic concentrations of the synthetic wastewater were also analyzed using the same method, allowing for precise evaluation of removal performance.

The percent arsenic removal was calculated using Equation 1.

$$\%As\ removal = \left(\frac{A_0 - A_t}{A_0} \right) * 100\% \quad \text{Equation (1)}$$

In which:

A₀: Initial arsenic concentration

A_t: Residual arsenic concentration

3. RESULTS AND DISCUSSION

In this study, an initial arsenic concentration of 100 ppb was used in the preparation of synthetic contaminated wastewater to assess the efficiency of the adsorption process. This concentration was selected to reflect a moderate level of arsenic contamination, providing a suitable basis for evaluating removal performance and optimizing operational conditions. The outcomes of the experimental trials are detailed in the following section.

175 3.1. An empirical correlation between the arsenic removal efficiency and the three factors

176 Seventeen experimental runs were performed in total, with each run repeated three times to ensure
177 statistical robustness. Furthermore, the experiment conducted under optimal conditions was also
178 replicated three times to verify the consistency of the results. Table 1 presents the detailed
179 experimental parameters and corresponding arsenic removal efficiencies, all based on an initial
180 arsenic concentration of 100 ppb. From the experimental implementation, the research team realized
181 that the adsorbent material was not uniform between experiments (unlike the solution in the
182 absorption). To avoid errors due to the heterogeneity of the adsorbent material, the research team
183 repeated the experimental results at the center point in the BBD (run 13 to run 17). This helped to
184 achieve uniformity of the adsorbent material between experiments. In a simple term, these center
185 points are like "anchors" to keep the response surface from rotating around the central axis. To ensure
186 reliability, each experiment was conducted in triplicate, with particular emphasis on repeating the
187 center points to reduce variability associated with adsorbent heterogeneity. The high R^2 value (0.996)
188 confirms the statistical reliability of the model.

189 **Table 1.** Box-Behnken design experiment conditions, results of arsenic removal using TiO_2 -
190 Impregnated Laterite

RUN	Dosage (g)	pH	Reaction time (min)	Arsenic removal %
1	0.010	5.5	10	65.19
2	1.000	5.5	10	92.10
3	0.010	5.5	80	74.93
4	1.000	5.5	80	98.15
5	0.010	2.0	45	72.19

6	1.000	2.0	45	96.02
7	0.010	9.0	45	71.64
8	1.000	9.0	45	96.73
9	0.505	2.0	10	75.22
10	0.505	2.0	80	83.00
11	0.505	9.0	10	76.97
12	0.505	9.0	80	81.89
13	0.505	5.5	45	86.95
14	0.505	5.5	45	89.13
15	0.505	5.5	45	86.46
16	0.505	5.5	45	88.65
17	0.505	5.5	45	87.41

191 The experimental results outlined in Table 1 demonstrate the influence of adsorbent dosage, pH, and
 192 reaction time on arsenic removal efficiency using TiO₂-impregnated laterite. Overall, higher dosages
 193 of the adsorbent were strongly associated with greater removal percentages. Specifically, when the
 194 dosage was increased from 0.01 g to 1.0 g, the removal efficiency rose significantly—for example,
 195 from 65.19% (Run 1) to 92.10% (Run 2) at a constant pH of 5.5 and reaction time of 10 minutes.
 196 Similarly, at 80 minutes of reaction time and the same pH, efficiency improved from 74.93% (Run 3)
 197 to 98.15% (Run 4). These trends confirm the critical role of adsorbent quantity in enhancing surface
 198 area and active sites for arsenic adsorption. Reaction time also had a positive effect, particularly at

intermediate dosages (e.g., Run 9 vs. Run 10), indicating that longer contact times facilitate greater arsenic uptake until reaching near-equilibrium. The effect of pH appeared less pronounced, though mildly acidic to neutral conditions (pH 5.5) consistently yielded higher removal compared to strongly acidic (pH 2.0) or alkaline (pH 9.0) conditions. Notably, the central point replicates (Runs 13–17) showed consistent performance, with arsenic removal ranging from 86.46% to 89.13%, confirming the reproducibility and reliability of the experimental design. These findings underscore the importance of optimizing dosage and contact time, while indicating that TiO₂-impregnated laterite is an effective adsorbent across a moderate pH range.

Table 2. ANOVA for percent arsenic removal using TiO₂-Impregnated Laterite

Source	Sum of Squares	df	Mean Square	F-value	p-value	Remark
Model	1498.74	9	166.53	178.38	< 0.0001	significant
A-Dosage	1137.84	1	1137.84	1218.81	< 0.0001	
B-pH	0.0009	1	0.0009	0.0009	0.9767	
C-Reaction_time	30.31	1	30.31	32.47	0.0007	
AB	0.3969	1	0.3969	0.4251	0.5352	
AC	3.40	1	3.40	3.65	0.0978	
BC	2.04	1	2.04	2.19	0.1824	
A ²	0.0671	1	0.0671	0.0719	0.7963	
B ²	50.08	1	50.08	53.64	0.0002	

C ²	105.32	1	105.32	112.81	< 0.0001	
Residual	6.53	7	0.9336			
Lack of Fit	1.41	3	0.4684	0.3653	0.7829	not significant

208 The ANOVA results for percent arsenic removal presented in Table 2 indicate that the quadratic model
209 is highly significant, with a p-value of < 0.0001 and an F-value of 178.38, confirming the model's
210 suitability for predicting arsenic removal efficiency. Among the independent variables, adsorbent
211 dosage (A) was the most influential factor, exhibiting an exceptionally high F-value of 1218.81 and
212 a p-value of < 0.0001, signifying its critical role in enhancing arsenic adsorption. Reaction time (C)
213 also significantly affected arsenic removal (p = 0.0007), suggesting that sufficient contact time is
214 essential for achieving high removal efficiency. In contrast, pH (B) had an insignificant effect (p =
215 0.9767), indicating that within the tested range, changes in pH did not meaningfully impact the
216 adsorption process. Interaction terms (AB, AC, and BC) were also not statistically significant,
217 suggesting minimal synergistic effects between the variables. Among the quadratic terms, B² (pH)
218 and C² (reaction time) were significant (p = 0.0002 and < 0.0001, respectively), revealing that non-
219 linear relationships exist for these variables, particularly at higher or lower levels. The non-significant
220 lack of fit (p = 0.7829) confirms that the model adequately fits the experimental data without
221 substantial unexplained variation. These results highlight that optimizing dosage and reaction time is
222 critical for maximizing arsenic removal, while pH has a negligible effect under the tested conditions.

223 An empirical correlation between arsenic removal efficiency, and three key factors was developed
224 using the Box–Behnken design. A reduced cubic model with an R² of 0.996 was fitted for the process,
225 indicating strong predictive accuracy.

$$\begin{aligned}
As_{(removal)} = & 88.62 + 11.74A + 0.0076B + 1.80C + 0.2159AB - 0.7588AC - 0.4378BC \\
& - 0.1163A^2 - 1.76B^2 - 3.67C^2
\end{aligned}$$

Equation (2)

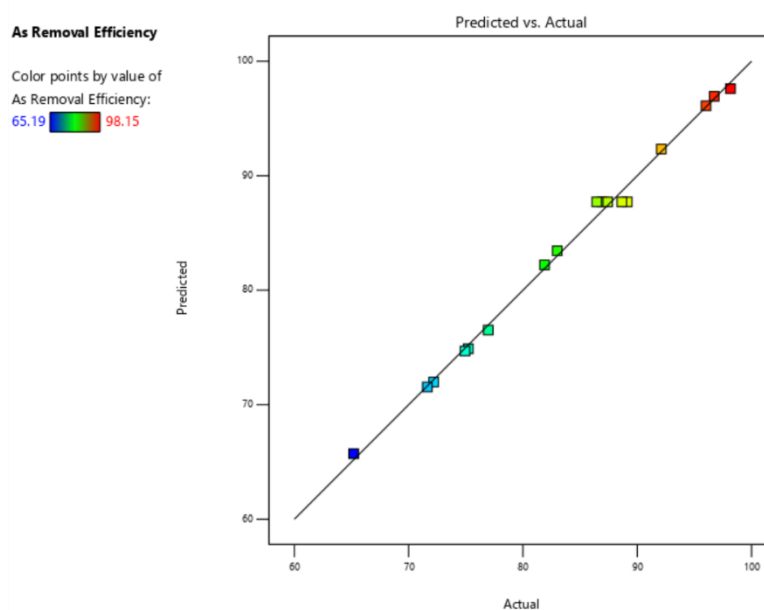
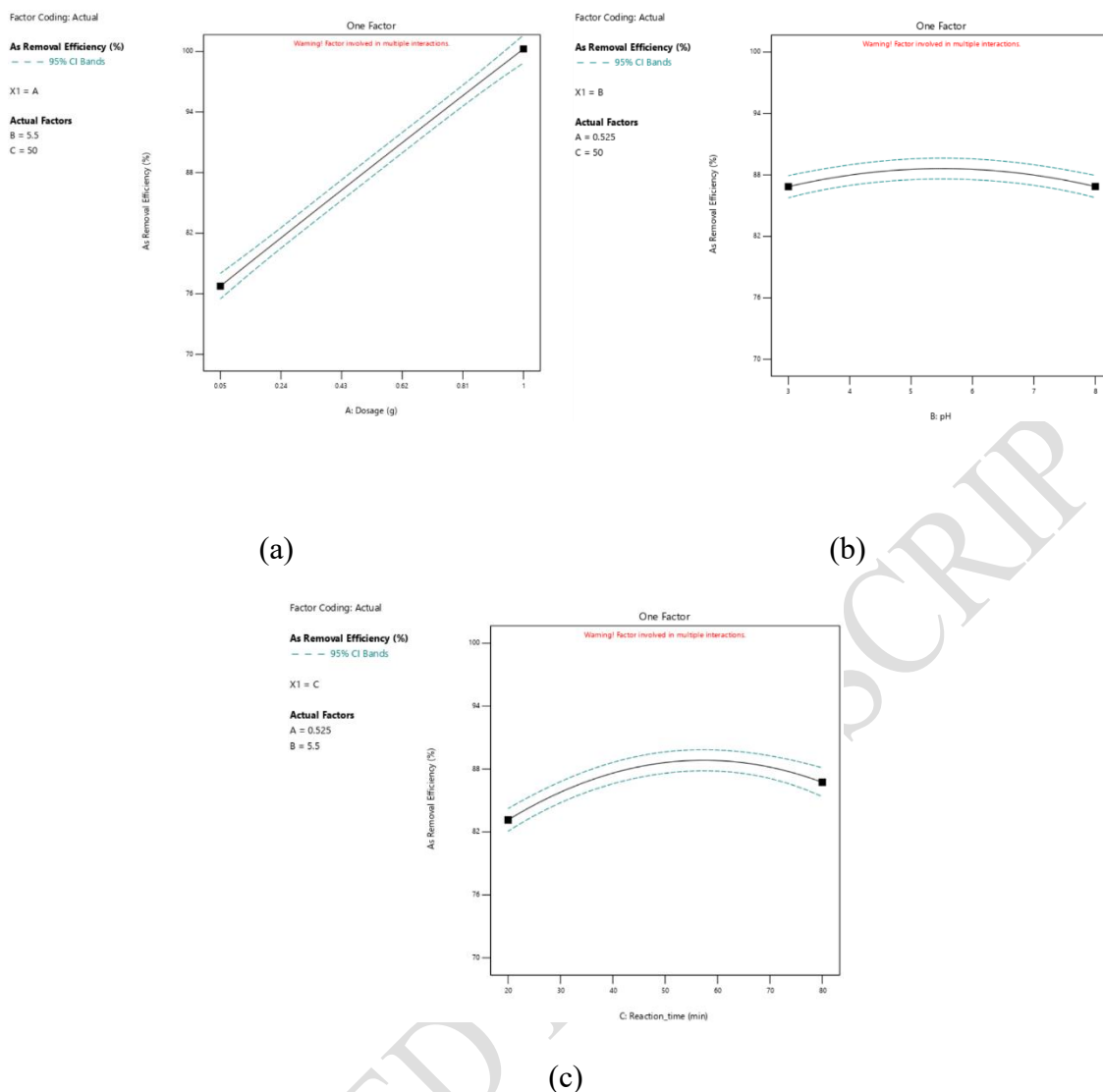


Figure 2. Comparison of actual experimental with model-predicted percent of the adsorption process.

Figure 2 illustrates the scatter plot comparing the experimentally observed arsenic removal efficiencies with the values predicted by the response surface methodology (RSM) model for the TiO₂-impregnated laterite adsorption system. The data points exhibit a strong alignment along the 45-degree reference line, indicating a high degree of agreement between the actual and predicted results. This strong correlation suggests that the developed RSM model reliably captures the behavior of the system across a range of experimental conditions. The distribution of color-coded points, representing removal efficiencies ranging from 65.19% to 98.15%, further demonstrates the model's ability to account for performance variability under different operational settings. Overall, the close fit between observed and predicted values affirms the model's accuracy, robustness, and effectiveness as a predictive tool for optimizing arsenic adsorption parameters.

3.2. Effect of operating parameters on arsenic removal using TiO₂-Impregnated Laterite

Percent arsenic removal in response to variations in operating parameters is shown in Figure 3.



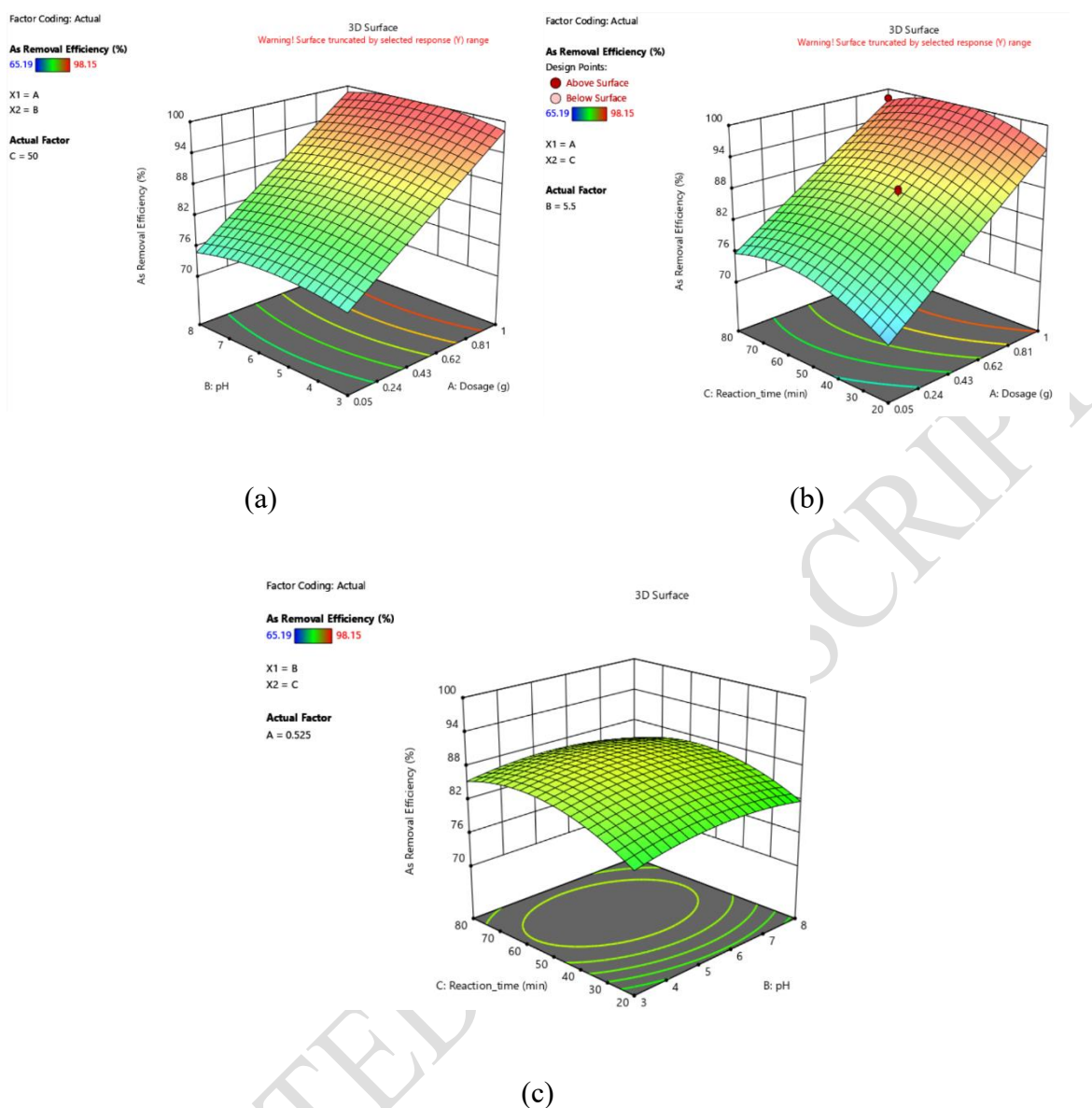
243 **Figure 3.** Effect of (a) Dosage (b) pH (c) Reaction time on arsenic removal using TiO₂-Impregnated
 244 Laterite.

245 Figure 3 depicts the individual effects of (a) adsorbent dosage, (b) solution pH, and (c) reaction time
 246 on the efficiency of arsenic removal using TiO₂-impregnated laterite, based on actual experimental
 247 levels. Among these variables, dosage (Figure 3a) was the most influential, showing a nearly linear
 248 increase in removal efficiency as the adsorbent mass rose from 0.01 g to 1.0 g. This strong dependence
 249 indicates that greater dosages enhance the available surface area and density of reactive hydroxyl
 250 groups, thereby providing more active sites for both arsenate adsorption and arsenite oxidation. The
 251 presence of TiO₂ likely accelerates this process by generating surface hydroxyl radicals under light
 252 exposure, which can oxidize As(III) to As(V), subsequently adsorbed via inner-sphere complexation

253 onto Fe–O and Ti–O sites. The effect of solution pH (Figure 3b) was less pronounced, following a
254 mild parabolic trend with maximum efficiency near pH 5.5. Mechanistically, this behavior can be
255 explained by the interplay between the surface charge of the TiO₂–laterite composite and the
256 speciation of arsenic oxyanions. Around pH 5–6, the surface is positively charged due to protonation
257 of surface hydroxyl groups, favoring electrostatic attraction with negatively charged H₂AsO₄[–] species.
258 At higher pH values, deprotonation of surface hydroxyls leads to electrostatic repulsion, while at very
259 low pH, competition from excess protons may suppress arsenate adsorption. Reaction time (Figure
260 3c) exhibited a curved response, with efficiency increasing until about 50 minutes before leveling off,
261 suggesting that adsorption–oxidation equilibrium had been reached. The initial rapid uptake reflects
262 fast external surface adsorption and photocatalytic oxidation of As(III), followed by a slower
263 diffusion-controlled stage where arsenic species migrate into mesopores or interact with less
264 accessible active sites. Taken together, the results point to a synergistic adsorption–oxidation
265 mechanism: (i) As(III) is oxidized to As(V) through photocatalysis on TiO₂, (ii) both As(III) and
266 As(V) form surface complexes with Fe–O and Ti–O groups via ligand exchange, and (iii) electrostatic
267 interactions modulate removal efficiency depending on solution pH. Among the tested parameters,
268 adsorbent dosage exerts the strongest control, followed by reaction time and pH, highlighting the
269 crucial role of active site density and surface chemistry in governing arsenic remediation using TiO₂-
270 impregnated laterite.

271 3.3. Optimum points for arsenic removal

272 The 3D surface plots of the two parameter interaction effects of Dosage, pH, Reaction time on percent
273 arsenic removal using TiO₂-Impregnated Laterite were shown in Figure 4.



274 **Figure 4.** 3D surface plots of the two parameter interaction effects of Dosage, pH, Reaction time on
 275 percent arsenic removal using TiO₂-Impregnated Laterite: (a) Dosage and pH, (b) Dosage and
 276 Reaction time, (c) pH and Reaction time.

277 Figure 4 displays the three-dimensional surface plots that illustrate the interactive effects of adsorbent
 278 dosage, pH, and reaction time on arsenic removal efficiency using TiO₂-impregnated laterite. In
 279 Figure 4a, removal efficiency increases with dosage up to approximately 0.8 g, particularly under
 280 lower pH conditions, indicating that acidic environments enhance the oxidative adsorption process.
 281 However, beyond pH 6, a slight reduction in efficiency is observed, likely due to diminished
 282 electrostatic attraction or surface charge effects at higher pH levels. Figure 4b reveals a synergistic

283 interaction between dosage and reaction time, with removal efficiency rising progressively as both
 284 parameters increase, reaching a maximum at the highest dosage tested. This trend highlights the
 285 combined importance of adequate adsorbent quantity and sufficient contact time for optimal arsenic
 286 removal. In Figure 4c, the interaction between pH and reaction time shows that maximum removal
 287 occurs at intermediate pH values (around 5–6) and extended contact durations (60–70 minutes),
 288 suggesting that favorable chemical conditions must align with appropriate reaction kinetics.
 289 Collectively, these surface plots underscore the complex, non-linear interactions among process
 290 variables and emphasize the need for integrated parameter optimization to achieve high arsenic
 291 removal efficiency.

292 **Table 3.** The optimum condition for arsenic removal using TiO₂-Impregnated Laterite

Values of optimum conditions	Dosage (g)	0.99
	pH	5.3
	Reaction time (min)	71
Actual and predicted values of PCT removal	Actual	97.65%
	Predicted	98.82%
	Difference	1.17

293 The optimization results for arsenic removal using TiO₂-impregnated laterite, presented in Table 3,
 294 demonstrate the high effectiveness of the process under the identified optimal conditions. The optimal
 295 parameters were determined to be an adsorbent dosage of 0.99 g, a solution pH of 5.3, and a reaction
 296 time of 71 minutes. Under these conditions, the experimentally observed arsenic removal efficiency
 297 was 97.65%, closely aligning with the model-predicted value of 98.82%, yielding a minimal deviation
 298 of only 1.17%. This close agreement between predicted and actual outcomes affirms the precision
 299 and reliability of the response surface methodology (RSM) model applied in this study. The findings

300 further underscore the strong adsorption performance of TiO₂-impregnated laterite, particularly in
301 slightly acidic conditions, which likely enhance surface reactivity and improve the availability of
302 active binding sites. Overall, these results validate the predictive capability of the model and reinforce
303 the potential of TiO₂-impregnated laterite as an effective, low-cost adsorbent for arsenic removal in
304 aqueous treatment applications.

305 CONCLUSION

306 This study confirmed the potential of TiO₂-impregnated laterite as an efficient and low-cost adsorbent
307 for the removal of arsenic from aqueous solutions. Using a Box–Behnken Design within the Response
308 Surface Methodology framework, the effects of three key operational parameters—adsorbent dosage,
309 pH, and reaction time—were systematically investigated and optimized. The statistical performance
310 evaluation using ANOVA and quadratic modeling highlighted the significant influence of dosage and
311 reaction time, with a well-fitted model ($R^2 = 0.996$), confirming the predictive strength of the
312 methodology. The findings indicated that both adsorbent dosage and reaction time significantly
313 influenced arsenic removal efficiency, whereas pH had a comparatively minor effect within the
314 studied range. Optimal conditions for maximum arsenic removal (98.82%) were identified at a dosage
315 of 0.99 g (~1.0 g), pH 5.3, and a reaction time of 71 minutes, demonstrating the promise of TiO₂-
316 modified laterite for real-world water treatment applications. This obtained removal efficiency of
317 TiO₂-impregnated laterite is higher than that of KMnO₄-modified laterite (93.2%) and comparable to
318 commercial adsorbents such as activated alumina (~95%), indicating superior or equivalent
319 performance. Given the abundance and low cost of laterite, combined with the stability of TiO₂, the
320 proposed material is well-suited for decentralized arsenic remediation systems, especially in rural or
321 resource-constrained regions.

322 Despite the promising findings, several limitations warrant consideration. The experiments were
323 performed under controlled laboratory conditions using synthetic arsenic-contaminated water, which
324 may not fully represent the complexity of natural systems where multiple competing ions and organic

325 matter coexist. Additionally, the long-term stability and reusability of the TiO₂-impregnated laterite
326 were not assessed, leaving uncertainties about its durability and regeneration potential under repeated
327 use. The investigation was also confined to a relatively narrow pH range, limiting the ability to predict
328 performance in highly acidic or alkaline environments often encountered in field applications.
329 Furthermore, adsorption isotherms and kinetic studies were not included, and these will be addressed
330 in future work to provide deeper mechanistic insights into the removal process.

331 Future studies will focus on field-scale evaluations under diverse environmental conditions,
332 particularly in arsenic-impacted areas. Further investigations should address the impact of co-existing
333 contaminants, assess regeneration performance, and conduct life-cycle analyses to determine overall
334 sustainability. Comprehensive material characterization is also recommended to elucidate surface
335 modification effects and adsorption mechanisms. Additionally, the integration of TiO₂-impregnated
336 laterite into hybrid treatment systems—such as those combining electrocoagulation or membrane
337 technologies—could be explored to enhance removal efficiency and operational robustness.

338 **AUTHOR CONTRIBUTIONS**

339 L.P.T (PhD) and V.T.K.O (Master) conducted all the experiments and simulation and wrote the
340 manuscript. L.P.T (PhD) revised the manuscript.

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