

1 **Investigation of antibiotic clarithromycin adsorption potential on microplastics**

2
3 **Zainab Ikram Sedeeq Sedeeq¹, Fatma Beduk^{1,*}**

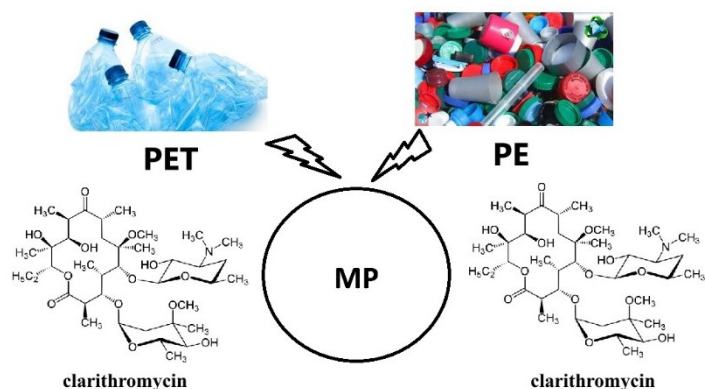
4 Necmettin Erbakan University, Engineering Faculty, Department of Environmental Engineering,
5 Koycegiz Campus, 42060, Konya, Turkey, zainabsedeeq8@gmail.com, fabeduk@erbakan.edu.tr

6
7 ***Corresponding Author:** Prof. Dr. Fatma Beduk

8 E-mail: fabeduk@erbakan.edu.tr; tel: +90 530 5256105

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ACCEPTED MANUSCRIPT

10 GRAPHICAL ABSTRACT



12

13 ABSTRACT

14 In this study, it was aimed to investigate the potential of microplastics (MPs) to adsorb antibiotic
15 clarithromycin (CLAR) in the water media. For this purpose, two of the most common used plastics;
16 polyethylene terephthalate (PET) and polyethylene (PE) were selected. Batch adsorption experiments
17 were performed under various conditions, i.e., pH, and ionic strength of the solution, type and dimension
18 of MPs. Liquid chromatography equipped with mass spectrophotometry (HPLC-MS) was used for the
19 analysis of CLAR. Fourier Transform Infrared Spectrometry (FT-IR) analysis of adsorbents was
20 performed before and after CLAR adsorption.

21 Results of the experimental studies showed that the adsorption reached the highest value at pH 6-7.
22 Equilibrium adsorption time was 240 min. The adsorption occurred in accordance with pseudo-second-
23 order kinetics. The experimental q_e values for CLAR adsorption of <2 mm PET-MPs; <5 mm PET-MPs;
24 <2 mm PE-MPs and <5 mm PE-MPs were 0.33 mg/g, 0.26 mg/g, 2 mg/g, and 0.2 mg/g, respectively. It
25 was determined that adsorption with <2 mm PE-MPs fits the Langmuir isotherm model ($R^2=0.95$), while
26 adsorption with <2 mm PET-MPs ($R^2=0.74$) and <5 mm PET-MPs ($R^2=0.83$) fit the Freundlich isotherm
27 model. The findings revealed that CLAR was adsorbed by all tested PET-MPs and PE-MPs, that poses
28 an accumulation and transportation risk in the aquatic environment.

29 **Keywords:** adsorption, antibiotics, clarithromycin, isotherm, kinetic, microplastic.

31 1. Introduction

32 Plastics have become one of the most important environmental pollutants due to their widespread use
33 (Ahmad *et al.* 2020). Plastics have been widely used in industry, commerce, and construction, due to
34 their easy molding, high mechanical and chemical resistance, and low cost. Plastics have different
35 surface properties, various crystal degrees, and physicochemical structures depending on their polymeric
36 properties (Fu *et al.* 2021). While only a small proportion of plastics are recycled, the remaining amount
37 is stored in solid waste landfills, incinerated or spread out into the environment (Pacheco *et al.* 2012).
38 Polyethylene terephthalate (PET), polyethylene (PE), polypropylene (PP), and polystyrene (PS) are the
39 most common polymer constituents of plastics in water sources (Li *et al.* 2020). Plastics turn into
40 microplastics (MPs) with sizes lower than 5 mm, as a result of various physicochemical and biological
41 decomposition processes in nature (Cole *et al.* 2011).

42 Plastic pollution in the marine environment is one of the threats that most affects the ecosystem.
43 Ingestion of plastics by marine fish species causes ecologically negative consequences. Young fish,
44 mammals, sea turtles, sharks, and reptiles are often exposed to plastics in the sea, and these objects can
45 cause their death. Seabirds are also very prone to swallow plastic objects (Lionetto and Esposito
46 Corcione 2021). When MPs are exposed to long-term environmental weather conditions, their surface
47 properties change (high specific surface area, porosity, amorphous structure, strong hydrophobicity, and
48 multi-pore structure etc.) and therefore they become prone to adsorb various toxic and harmful chemicals
49 in the environment (Zhang *et al.* 2018). Plastics adsorb heavy metals, and various types of synthetic
50 organic pollutants, including pharmaceuticals in aquatic environments, thus act as carriers of these
51 pollutants (Nguyen *et al.* 2021). Plastics themselves are also sources of toxic chemicals, such as
52 bisphenol A, phthalate, triclosan, and polybrominated diphenyl ether, that can be dissolved from their
53 structure (Arienzo *et al.* 2021).

54 The use of antibiotics is increasing day by day, and their concentrations in the aquatic environment are
55 also increasing in parallel (Aydin *et al.* 2019; Baumann *et al.* 2015). Approximately 60% of antibiotics

56 used in human and veterinary medicine are released into the environment as parent compounds.
57 Antibiotic residues remaining in the environment cause contamination of fresh water and food (Liu *et al.*
58 *et al.* 2022). They affect non-target organisms in the receiving environment and e.g. antibiotics develop
59 antibiotic resistance genes (ARGs) in bacteria (Imwene *et al.* 2022).

60 Macrolide antibiotics are widely used in infectious diseases caused by bacterial pathogens (Zhang *et al.*
61 2022). It has been found that macrolide antibiotics can be poorly degraded during conventional treatment
62 processes (Baumann *et al.* 2015). Macrolide antibiotics are used in combination with other medications
63 to treat bacterial infections, and stomach ulcers. One of the most commonly consumed type of macrolide
64 antibiotics is CLAR. CLAR was in the Watch List for EU, concerning water policy by Decision
65 2018/840. Therefore, CLAR was selected as model antibiotic in this study.

66 Adsorption studies of organic pollutants on different types of MPs have been carried out; Nguyen *et al.*
67 (2021) examined the adsorption of Tetracyclines (TC), an antibiotic frequently found in aquatic
68 environments, on high density polyethylene (HDPE) particles with an average size of 45 μm . TC
69 adsorption on the HDPE surface was consistent with pseudo-second-order kinetics. The Langmuir
70 adsorption isotherm described TC adsorption well ($r^2 > 0.99$). It was determined that chemical adsorption
71 and hydrogen bond formation were responsible for the interaction between TC and HDPE surface.
72 Maximum TC adsorption occurred at pH 7.0. It was evaluated that the overall adsorption energy was 1.0
73 kJ-mol, which means that TC adsorption on the PE surface occurred thermodynamically. The presence
74 of foreign ions increased TC adsorption due to compression of the electrical double layer and complex
75 formation (such as Mg^{2+} and Ca^{2+}). The presence of dissolved organic matter also affected the TC
76 adsorption to increase by a small amount.

77 Chen *et al.* (2021) determined TC adsorption potential of PE particles by using laboratory experiments
78 and molecular dynamics simulation. As a result of the analysis of adsorption kinetics and adsorption
79 thermodynamics investigated by FT-IR and X-ray photoelectron spectroscopy (XPS), it was stated that
80 the adsorption behavior of TC occurred only on PE surface and the adsorption process could be explained
81 mainly by the intermolecular van der Waals force and the filling mechanism of micropores.

82 Atugoda *et al.* (2020) conducted a research study about adsorption of CIPRO on PE-MPs. In the study,
83 the effects of pH, ionic strength and natural organic matter on adsorption efficiency were evaluated. The
84 maximum adsorption of CIPRO onto PE-MPs was observed around pH 6.5-7.5. As a result of
85 experiments investigating the effect of ionic strength, it was determined that 0.1 M NaNO₃ caused a 17%
86 reduction in CIPRO adsorption. Addition of humic acid (HA) to the medium reduced the adsorption
87 potential by 89%. This was explained by CIPRO's higher affinity for complexation with HA. It was
88 determined that CIPRO has a physical sorption on PE-MPs. In this case, it was evaluated that small
89 environmental changes could cause desorption of CIPRO from MPs.

90 Li *et al.* (2018) determined the adsorption potential of 5 antibiotics [sulfadiazine (SDZ), Amoxicillin
91 (AMX), TC, CIPRO and Trimethoprim (TMP)] on 5 types of MPs [PE, PS, PP, polyamide (PA),
92 polyvinyl chloride (PVC)] in freshwater and seawater systems. SEM and X-ray diffractometer (XRD)
93 analysis were used for the characterization of MPs. As a result of the study, it was determined that PA
94 had the strongest adsorption capacity for antibiotics. Adsorption showed a positive correlation with the
95 porous structure of the adsorbent, hydrogen bonds and octanol-water partition coefficients (Log K_{ow}).
96 Compared with the freshwater system, the adsorption capacity in seawater was significantly reduced.
97 The results showed that PA particles, commonly observed in waters, could serve as antibiotic carriers in
98 the aquatic environment.

99 The presence of MPs in aquatic environment, their contribution to the transport of pollutants and their
100 effects on aquatic organisms have been studied in recent years. However, a very limited number of
101 studies have been conducted on the adsorption of antibiotics on different types of MPs. In this study, it
102 was aimed to investigate the antibiotic CLAR adsorption potential of the most common type of MPs;
103 PET and PE in the water media.

104 **2. Materials and methods**

105 *2.1. Materials and Chemicals*

106 Certified reference materials of antibiotic Clarithromycin (CLAR) (PHR1038) was provided from
107 Merck. Methanol CH₃OH (Merck, Germany) was used to dissolve the antibiotic. 5 mM ammonium

108 formate NH_4HCO_2 ($\geq 99.0\%$ for HPLC) and 0.1% formic acid were used as mobile phase for HPLC. 0.1
109 M sodium hydroxide (NaOH) and 0.1 M hydrochloric acid (HCl) were used to adjust pH (Merck,
110 Germany). Sodium chloride (NaCl) (Merck, Germany) was used to determine the effect of ionic strength.
111 PET used as adsorbent was obtained from 500 mL water bottles commercially available in the market.
112 PET was washed with pure water and dried before use. PET was grinded in a grinder and those that
113 passed through a 5 mm sieve were used as <5 mm PET-MPs (named as 5 mm PET-MPs), and those that
114 passed through a 2 mm sieve were used as <2 mm PET-MPs (named as 2 mm PET-MPs). PE used as
115 adsorbent was obtained from a recycling facility. PE pellets were first washed with pure water and dried.
116 Those that passed through a 5 mm sieve were used in their current pellet form (named as 5 mm PE-
117 MPs), and those that passed through a 2 mm sieve were used as <2 mm PE-MPs (named as 2 mm PE-
118 MPs).

119 2.2. Characterization of MPs

120 Surface chemical characterizations of PET-MPs and PE-MPs before and after CLAR adsorption were
121 determined by FT-IR spectroscopy. Measurements were made in the range of $400\text{--}4000\text{ cm}^{-1}$, with 16
122 repeated scans and a resolution of 4 cm^{-1} . FT-IR spectroscopy is basically based on the absorption of
123 infrared light by the substance being examined.

124 Surface physical characterizations of PET-MPs and PE-MPs were determined by SEM. The surface
125 morphology of the samples were imaged at different magnifications at 20 kV., Hitachi – SU 1510. Since
126 the PET-MPs and PE-MPs used in this study were not conductive, they were coated with a very thin
127 (approximately 3 \AA /second) conductive material under 20 kV vacuum, so as to be examined.

128 Surface area and porosity of the MPs were measured using the Brunauer, Emmett and Teller (BET)
129 method in a liquid nitrogen environment at 77 K, based on nitrogen (N_2) gas adsorption technique.
130 Thanks to adsorption and desorption capacities, BET surface area and pore size distribution could be
131 determined. BET analyzes of PET-MPs and PE-MPs used in this study were carried out at $30\text{ }^\circ\text{C}$ for 24
132 hours.

133 2.3. Adsorption Experiments

134 3 g/L suspensions were prepared by adding 2 mm and 5 mm PET-MPs, and 2 mm and 5 mm PE-MPs
 135 to 50 mL distilled water in 100 mL glass vials. After spiking the initial concentration of 6 mg/L CLAR
 136 to the solution, pH at which optimum CLAR adsorption occurs was found, by adjusting the pH of the
 137 solution to a range of 4-8, using 0.1 M HCl or NaOH. Batch adsorption experiments were carried out in
 138 a controlled environment at 25 °C with a shaking speed of 220 rpm with a horizontal shaker (Shin Saeng,
 139 Korea), for 4 h. Withdrawn samples were filtered through PTFE membrane syringe filters, with pore
 140 size of 0.45 μ (Sartorius, SRP25), to remove MPs. Filtrate samples were analyzed for CLAR, by the
 141 HPLC-MS (Agilent Technologies). The adsorption kinetics were determined with an initial CLAR
 142 concentration of 6 mg/L, and MPs dosage of 3 g/L, at the optimum pH6-7, determined in the previous
 143 experimental step. Samples were withdrawn at the time intervals of 15, 30, 45, 60, 90, 180, 240, etc.
 144 min., filtered through 0.45 μ PTFE filters, and subjected to CLAR analysis. The adsorption isotherms
 145 were determined with CLAR concentration ranging between 2-30 mg/L. MPs dosage was kept as 3 g/L
 146 and the pH was adjusted to 6-7. Vials were kept on horizontal shaker for 240 min., which was equilibrium
 147 time, determined by the kinetics experiments. So as to determine the effect of environmental conditions
 148 on adsorption, the effect of ionic strength (0.01; 0.1; 1 M NaCl) were examined under optimum
 149 experimental conditions. All experiments were conducted in duplicate and results were given as mean.
 150 Adsorbed amount of antibiotics and percentage of the removal were calculated by using Eq.(1) and
 151 Eq.(2), respectively.

152 $q_e = \frac{C_o - C_e}{m} \times V$ Eq. (1)

153 $\% \text{ Removal} = \frac{C_o - C_e}{C_o} \times 100$ Eq. (2)

154

155 Where; q_e is the adsorbed amount of antibiotic at equilibrium (mg/g), C_o is the initial concentration of
 156 antibiotic (mg/L), C_e is the equilibrium concentration of antibiotic (mg/L), m is the amount of adsorbent
 157 (g), V is the solution volume (L).

158 2.4. Sorption Models

159 Adsorption kinetic models have been used to investigate the adsorption mechanisms of pollutants on
160 adsorbents (Fu *et al.* 2021). The analysis of adsorption kinetics helps to estimate the equilibrium time
161 and determine the adsorption rate of a solute by an adsorbent (Zhang *et al.* 2020). Adsorption rate is an
162 important parameter for the evaluation of the adsorption efficiency. The most commonly used adsorption
163 kinetic models are: pseudo-first-order kinetic model and pseudo-second-order kinetic model (Fu *et al.*
164 2021). The formulas of pseudo-first-order and pseudo-second-order kinetic models are given in Eq.(3)
165 and Eq.(4), respectively (Ho and McKay 1999).

$$166 \ln (q_e - q_t) = \ln q_e - k_1 t \dots\dots\dots \text{Eq. (3)}$$

$$167 q = \frac{k_2 q_e^2 t}{1 + k_2 q_e t} \dots\dots\dots \text{Eq. (4)}$$

168 Here:

169 q_e : The amount of compound adsorbed at equilibrium (mg/g)

170 q_t : The amount of compound adsorbed at time t (mg/g)

171 k_1 : Pseudo-first-order rate constant (1/min)

172 k_2 : Pseudo-second-order rate constant (1/min)

173 t : Contact time (min)

174 Adsorption isotherms are generally used to estimate the amount of adsorbate that can be adsorbed on a
175 solid surface and to determine whether the adsorption mechanism is linear single-layer or multilayer
176 adsorption (Fu *et al.* 2021). Langmuir and Freundlich adsorption isotherm models have been widely
177 used to determine the adsorption isotherms of antibiotics (Li *et al.* 2018). The Langmuir isotherm was
178 primarily used to describe the adsorption between gases and solid surfaces and to determine the
179 adsorption capacity of the adsorbent. This isotherm assumes that adsorption occurs in monolayer
180 homogeneous regions on the adsorbent. According to this model, adsorption and desorption occur in
181 equilibrium (Langmuir 1918). The Freundlich isotherm assumes that adsorption occurs in multilayer
182 heterogeneous regions on the adsorbent. According to this model, the heat of adsorption and affinity are

183 not distributed uniformly on the heterogeneous surface and the adsorption is reversible (Freundlich
184 1906).

185 The linear form of the Langmuir and Freundlich adsorption isotherm models are given in Eq. (5), and
186 Eq. (6), respectively.

187 Langmuir isotherm model:

$$188 \frac{C_e}{q_e} = \frac{1}{(q_e k_L)} + \frac{C_e}{q_e} \dots \dots \dots \text{Eq. (5)}$$

189 Freundlich isotherm model:

$$190 \ln q_e = \ln k_f + \frac{1}{n \ln C_e} \dots \dots \dots \text{Eq. (6)}$$

191 Here:

192 C_e : Compound concentration at equilibrium (mg/L)

193 q_e : Adsorbed amount of compound at equilibrium (mg/g)

194 k_L : Langmuir adsorption constant (L/mg)

195 k_f : Freundlich partition ratio (mg/g)

196 n : Freundlich adsorption constant; surface heterogeneity factor

197 2.5. Analytical Method

198 Liquid chromatography equipped with a mass spectrophotometer was used for quantitative analyzes of
199 target compounds (HPLC-MS, Agilent Technologies). The optimum column temperature program and
200 carrier liquid of the system were determined by using CLAR standard solution at a concentration of 10
201 mg/L. Chromatographic separation was performed with an Agilent Poroshell 120 EC-C18 (100 mm x 3
202 mm, particle size 2.7 μm) column. The calibration curve was prepared using seven standard solutions in
203 the linear range. It was aimed to obtain linear results in the concentration range studied. Each sample
204 was analyzed in duplicate.

205 Antibiotics were studied in positive mode and the most suitable carrier phase A was water containing
206 0.1% formic acid and 5 mM ammonium formate, and carrier phase B was methanol. The most suitable
207 carrier phase flow rate was determined to be 0.6 mL/min. The initial carrier phase ratio was 90% (A):
208 10% (B) and was kept at this ratio for 1 min. Then, carrier phase B was increased linearly to 30% in 3
209 minutes, to 70% in 8 min., to 95% in 2 min. and kept at this rate for 2 min. The initial carrier phase
210 conditions were returned and the study was carried out under these conditions for 4 min. before the next
211 injection. The column temperature was 35 °C and the injection volume was 2 µL. The protonated product
212 ion [M+H]⁺ was detected by injecting each compound prepared at a concentration of 10 ng/µL into the
213 standard HPLC-MS system in scan mode.

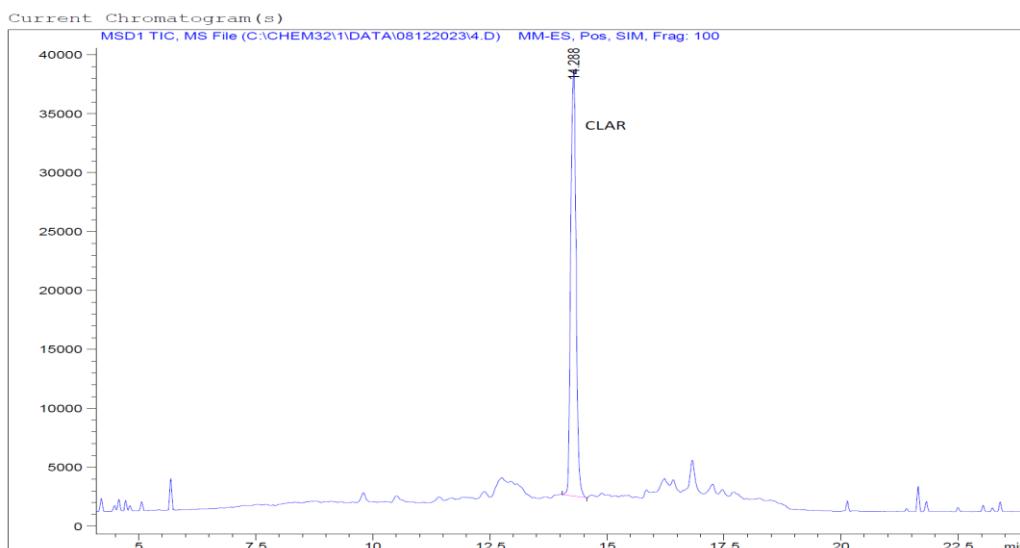
214 Table 1 shows the retention times (RT) and mass to charge ratio (m/z) values for antibiotic under
215 optimum HPLC-MS conditions. Figure 1 shows the standard chromatogram of antibiotic CLAR under
216 optimum HPLC-MS conditions. LOD and LOQ values for the CLAR were determined to be 3.8×10^{-6}
217 ng/L, and 1.27×10^{-5} ng/L. It was seen that R² values varied between 0.9928-0.9998. Relative standard
218 deviation (RSD) of repeatability values ranged between 1.52% and 9.12% (n=6).

219

220 **Table 1.** Retention time and m/z values for antibiotic CLAR under optimum HPLC-MS conditions

Antibiotic	m/z	RT (min)
CLAR	748, 590 [M+H] ⁺	14.288

221



222

223 **Figure 1.** Standard chromatogram for antibiotic CLAR under optimum HPLC-MS conditions (10 ng/ μ L)

224

225 3. Results and Discussion

226 3.1. Characterization of PET-MPs and PE-MPs

227 3.1.1. Morphology and surface area of PET-MPs and PE-MPs

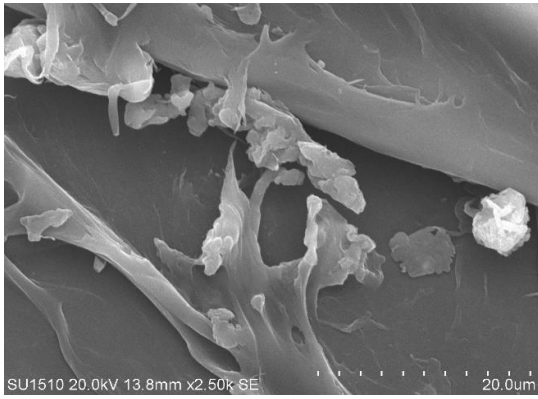
228 Surface morphology images of 2 mm and 5 mm PET-MPs and 2 mm and 5 mm PE-MPs samples with
 229 SEM at 20 kV at different magnifications are given in Figure 2 and Figure 3, respectively. Multiple
 230 irregular folds on particle surfaces create more voids and pore spaces, therefore exhibit higher numbers
 231 of adsorption sites. PET-MPs and PE-MPs samples showed low crystallinity. This allows antibiotic
 232 molecules to be adsorbed into the loosely arranged polymer structure by Van der Waals forces (Nguyen
 233 et al. 2021; Atugoda et al. 2020; Fu et al. 2021). As a result of multi-point BET analysis, the surface area
 234 of 2 mm PET-MPs was 0.002 m²/g, while it was 0.235 m²/g for 2 mm PE-MPs. The surface area of 5
 235 mm PET or PE-MPs could not be determined by multi-point BET analysis method. As a result of the
 236 analysis performed with the density function theory (DFT method), the surface areas of 5 mm PET-MPs
 237 and 5 mm PE-MPs were determined as 0.145 m²/g and 0.126 m²/g, respectively.

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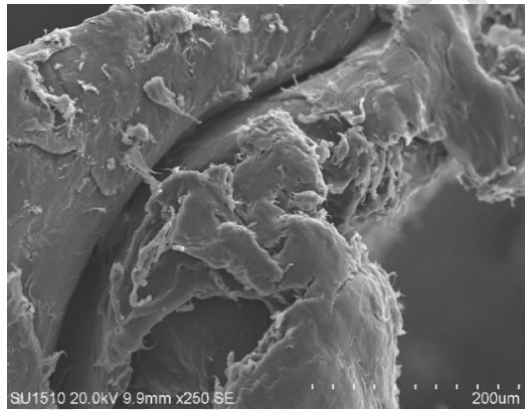
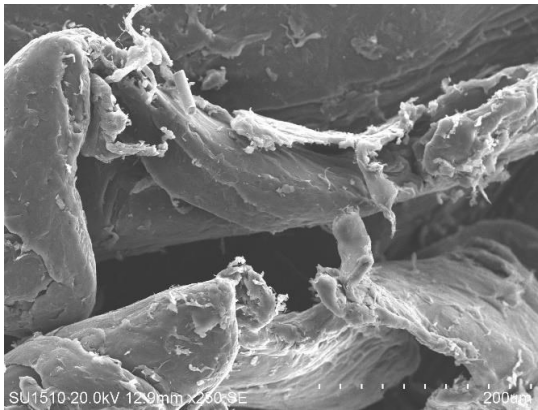
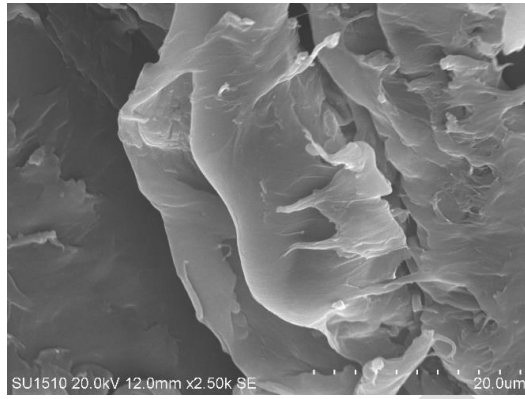
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mm PET-MPs



mm PET-MPs



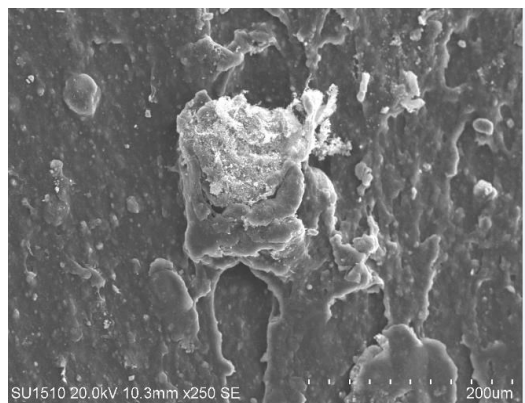
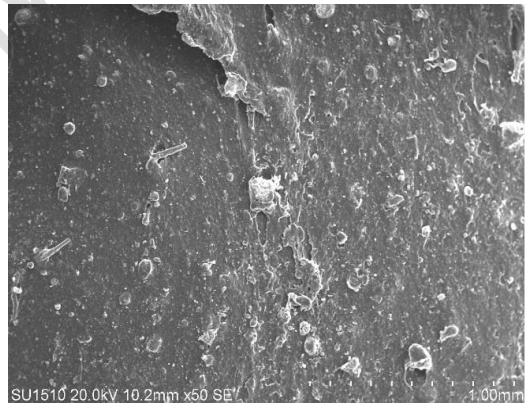
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Figure 2. SEM images of 2 mm PET-MPs and 5 mm PET-MPs

mm PE-MPs



mm PE-MPs



242

Figure 3. SEM images of 2 mm PE-MPs and 5 mm PE-MPs

243 3.1.2. FT-IR analysis of PET-MPs and PE-MPs

244 FT-IR spectra of PET-MPs and PE-MPs before and after CLAR adsorption are given in Figure 4. The
245 most frequently detected peaks were in the range of 700-3800 cm^{-1} . The region between 400-1500
246 (fingerprint region) represents specific compounds and the region between 1500-4000 (functional group
247 region) represents the existing chemical bond types (Dovbeshko *et al.* 2000; Movasaghi *et al.* 2008).
248 Significant FT-IR peaks and the identified functional groups of PET-MPs and PE-MPs before and after
249 CLAR adsorption are given in Table 2. The point with the highest vibration in the FT-IR spectra and the
250 highest peak was defined as the adsorption frequency. CLAR adsorption of 2 mm PET-MPs; 5 mm PET-
251 MPs, 2 mm PE-MPs, and 5 mm PE-MPs occurred at 1725 cm^{-1} , 1000 cm^{-1} , 2900 cm^{-1} , and 2900 cm^{-1}
252 frequencies, respectively. Carboxyl and vinyl ether compounds were identified in PET samples, and
253 alkane compounds were identified in PE samples. C=O and C-H stretching and C-O ribose bond were
254 detected. FT-IR analysis of MPs revealed that the spectra of the analyzed particles matched the
255 corresponding spectra for PET and PE in the instrument database. Therefore, MP samples were
256 characterized to confirm the specifications provided by the manufacturer.

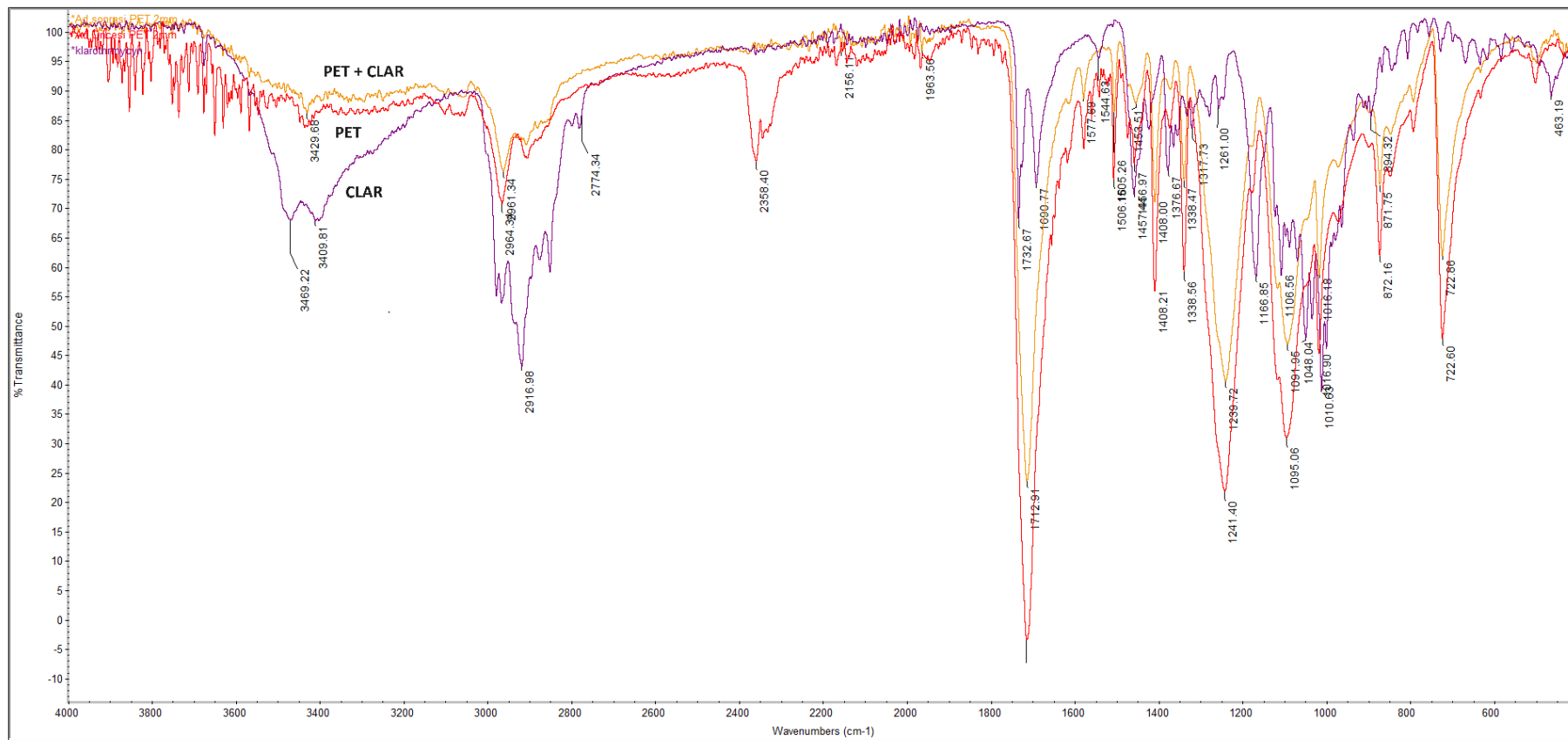
257 **Table 2.** Significant FT-IR peaks and identified functional groups of PET-MPs and PE-MPs before and
258 after CLAR adsorption

MPs	Before Adsorption (cm^{-1})	After Adsorption (cm^{-1})	CLAR (cm^{-1})	Adsorption Frequency (cm^{-1})	Functional group	Compounds
2 mm PET	1718.85	1712.91	1732.67	1725	(C=O stretching)	Carboxyl
5 mm PET	1015.91	1011.82	1010.63	1000	(C-O Ribose bond)	Vinyl Ether
2 mm PE	2915.56	2915.87	2916.98	2900	(C-H stretching)	Alkane
5 mm PE	2916.12	2918.18	2916.98	2900	(C-H stretching)	Alkane

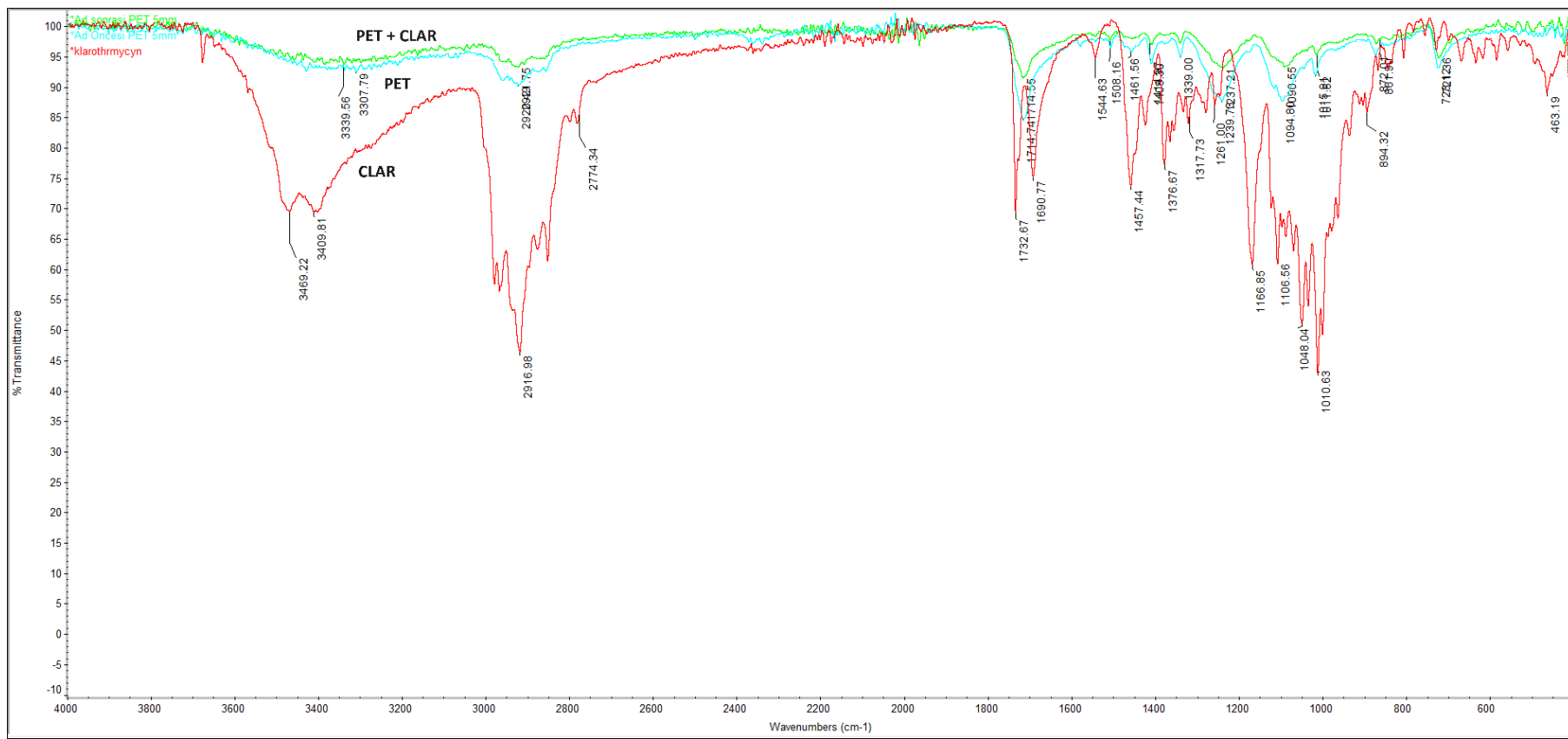
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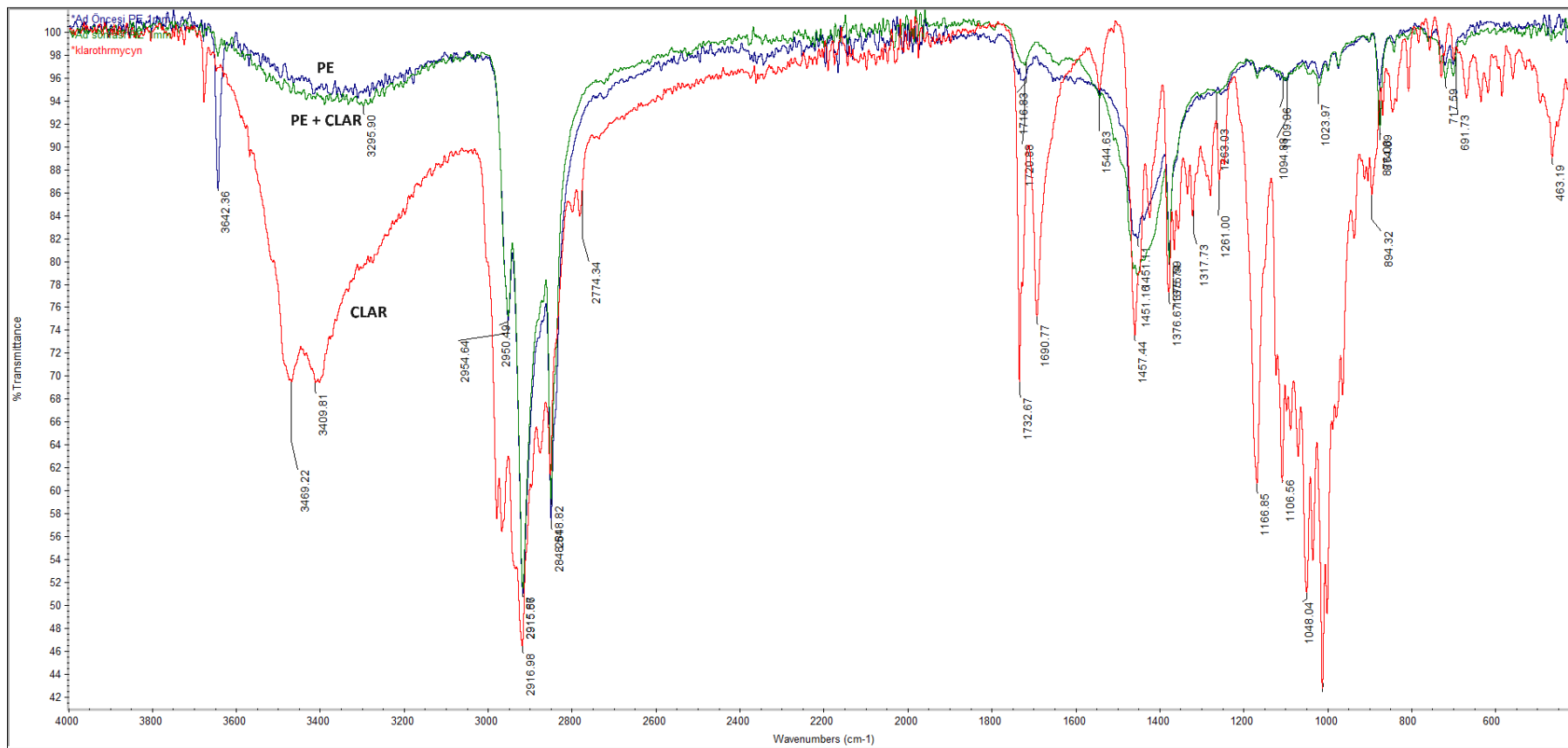


(a)



(b)

ACCEPTED



(c)

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(d)

Figure 4. FT-IR spectra of PET-MPs and PE-MPs before and after CLAR adsorption (a: 2 mm PET-MP + CLAR; b: 5 mm PET-MP + CLAR; c: 2 mm PE-MP + CLAR; d: 5 mm PE-MP + CLAR)

3.2. Effect of pH on CLAR Adsorption

Antibiotics are ionizable compounds. The ionization constant (pKa) of various antibiotics often varies significantly due to their specific functional groups. Antibiotics can exist as cations, zwitter ions, or anions depending on solution pH. Therefore, under a certain pH condition, the speciation of ionic chemicals can affect their sorption degree on MPs, since electrostatic interaction occurs at a certain pH (Li *et al.* 2018; Fu *et al.* 2021; Atugoda *et al.* 2020). The CLAR adsorption capacity of PET-MPs and PE-MPs was tested in the solution pH range of 2-11. It was determined that the CLAR was decomposed at pH 2 and pH 11. Therefore, the results obtained in the pH4-9 range were evaluated (Figure 5). In this pH range, cationic form of CLAR (pKa = 8,99 at 25 °C) lead to electrostatic interaction between CLAR and plastics. The surfaces of MPs are negatively charged. Therefore, ions in the medium can electrostatically bind to the binding sites and disrupt the charge balance of the surface (Moura *et al.* 2022). Adsorption capacity was increased under acid-normal conditions and maximum adsorption was achieved between pH6-7 similar to reported by Chen *et al.* (2021) for adsorption of tetracyclins (TC) on PE-MPs. When pH exceeded 7 and decreased below 6, the adsorption capacity of MPs decreased. The removal rates were determined as 7% for 2 mm PET-MPs, and 85% for 2 mm PE-MPs at pH6-7. If the pH of the adsorption medium exceeds the zero charge point (pH_{pzc}) of MPs, their surfaces will be negatively charged and electrostatically attract positively charged organic pollutants. However, when the pH of the adsorption medium exceeds the acid dissociation constant (pKa) of organic pollutants, the pollutants will be deprotonated and enter an anionic form, which will cause electrostatic repulsion and prevent their adsorption by MPs. Therefore, electrostatic interaction is closely related to the electrification of MPs, the shape of organic pollutants, and the amount of charge involved (Fu *et al.* 2021). In the study conducted by Nguyen *et al.* (2021), the effect of pH on TC adsorption of PE particles was investigated. It was noted that the surface of PE particles was negatively charged at pH > pH_{pzc} (~1.8) and as a result, the TC adsorption capacity was found to increase with pH, reaching a maximum value of 6.4 mg/g at pH 7.0, then decreasing with further increase in pH. The results show that TC was predominantly positively and neutrally charged at pH < 3.3 and 3.3 < pH < 8, respectively.

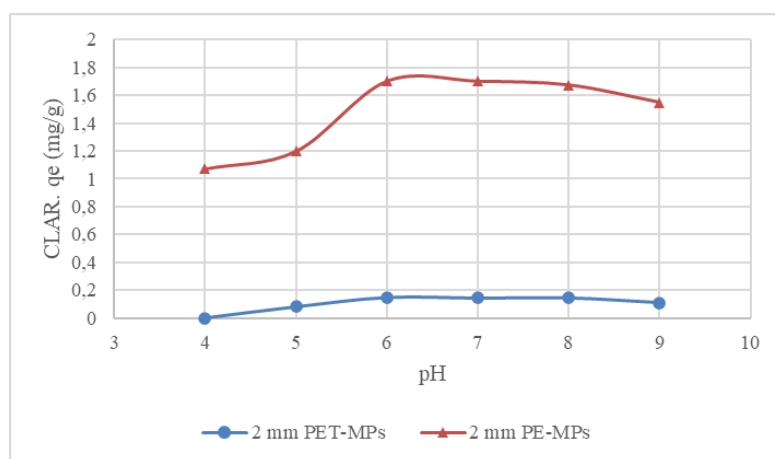


Figure 5. Effect of pH on the adsorption of CLAR on PET-MPs and PE-MPs (Experimental conditions; adsorbent: 3 g/L, 2 mm PET-MPs, and 2 mm PE-MPs, t: 4 hours, C_0 : 6 mg/L CLAR, 50 mL solution, pH adjustment with 0.1 M HCl, 0.1 M NaOH, 220 rpm, 25 °C, n=2)

3.3. Adsorption Kinetics

Findings of kinetic studies allowed to obtain information about adsorption rate of CLAR on MPs. Figure 6 indicates the sorption percent of CLAR as a function of contact time. Results show that equilibrium time was achieved in 240 min. When 65% adsorption rate was observed in just 15 min with 2 mm PE-MPs, adsorption rate went up to nearly 90% in 240 min. Lower adsorption rates were observed for both 2 mm PET-MPs and 5 mm PET-MPs, which were nearly 17% and 13%, respectively. Q_e values determined at equilibrium time for PET-MPs-2 mm, PET-MPs-5 mm, PE-MPs-2 mm, and PE-MPs-5 mm were 0.33 mg/g, 0.26 mg/g, 2 mg/g, and 0.2 mg/g, respectively. Lower adsorption value observed for PE-MPs-5 mm was attributed to smoother surface morphology observed by SEM images (Figure 3). Adsorption of CLAR on PE-MPs was also examined by Atugoda et al. (2020). 3 mg/g CLAR adsorption on PE-MPs in zero ionic strength and pH 7 was reported.

When the compatibility of the adsorption temporal change data with the pseudo-first-order order and pseudo-second-order kinetic models was evaluated, it was found that the adsorption was compatible with the pseudo-second-order kinetic model for all tested MPs (Figure 7). In the graphs drawn using t against t/q_t data, r^2 values varied between 0.98-0.99. The rate constants (k_1 and k_2) and theoretical equilibrium sorption capacities for CLAR ($q_{e, \text{calculated}}$) were calculated by use of the slopes and intercepts of the linear plots of the pseudo first-order and pseudo-second-order kinetic models. It was found that the

experimentally determined q_e values ($q_{e_{\text{experimental}}}$) were significantly overlapping with the q_e values calculated with the pseudo-second-order kinetic model (Table 3). However, the calculated q_e and the experimental q_e did not match in the results obtained with PE-MPs-5 mm, which could be explained by the very low levels of adsorption.

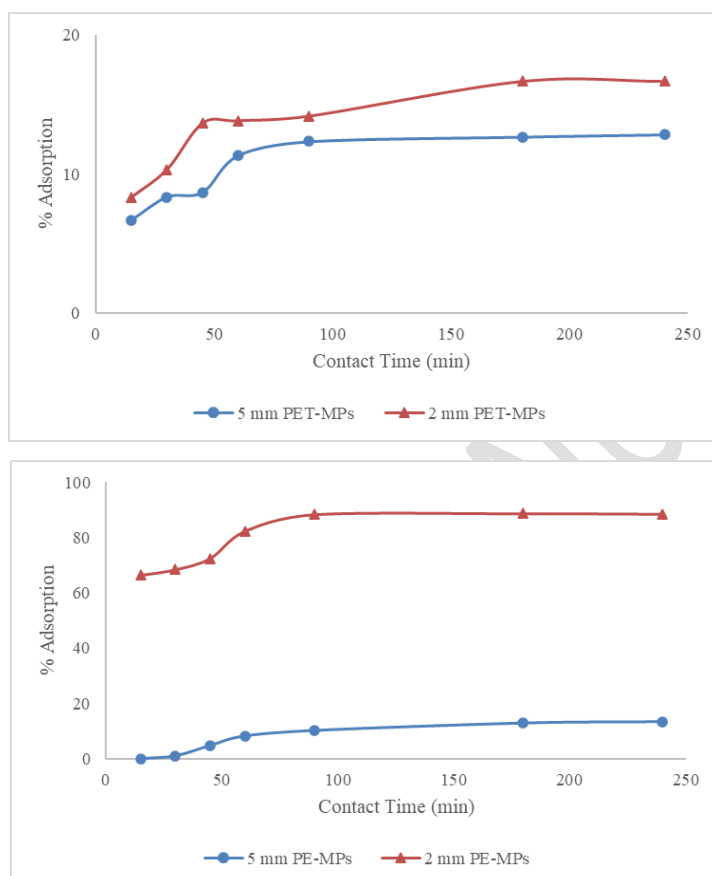


Figure 6. Effect of contact time on adsorption of CLAR by PET-MPs and PE-MPs (Experimental conditions; adsorbent: 3 g/L, t : 15, 30, 45, 60, 90, 180, 240 min, C_0 : 6 mg/L CLAR, 50 mL solution, pH 6.0-7.0, 220 rpm, 25 °C, $n=2$)

Table 3. Sorption rate constants and equilibrium sorption capacities for pseudo-first-order and pseudo-second-order kinetic models

	2 mm PET-MPs	5 mm PET-MPs	2 mm PE-MPs	5 mm PE-MPs
$q_{\text{experimental}}$ (mg/g)	0.33	0.26	2.0	0.2
<i>Pseudo-first-order kinetic constants</i>				
k_1 (1/min)	0.0072	0.01	0.0031	0.02
$q_{\text{calculated}}$ (mg/g)	5.5	6.3	1.5	2.0
R^2	0.79	0.92	0.74	0.20
<i>Pseudo-second-order kinetic constants</i>				
k_2 (g/mg.min)	0.002	0.001	0.59	1.97×10^{-8}
$q_{\text{calculated}}$ (mg/g)	0.36	0.27	2.11	0.0004
R^2	0.99	0.99	0.99	0.98

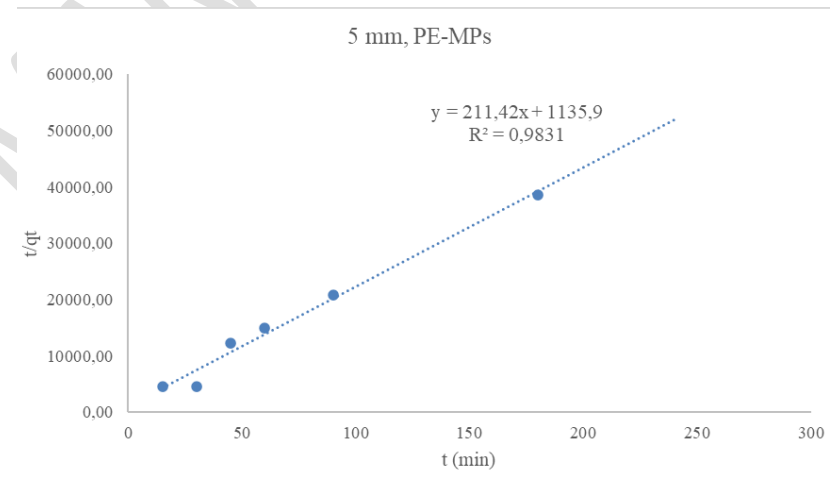
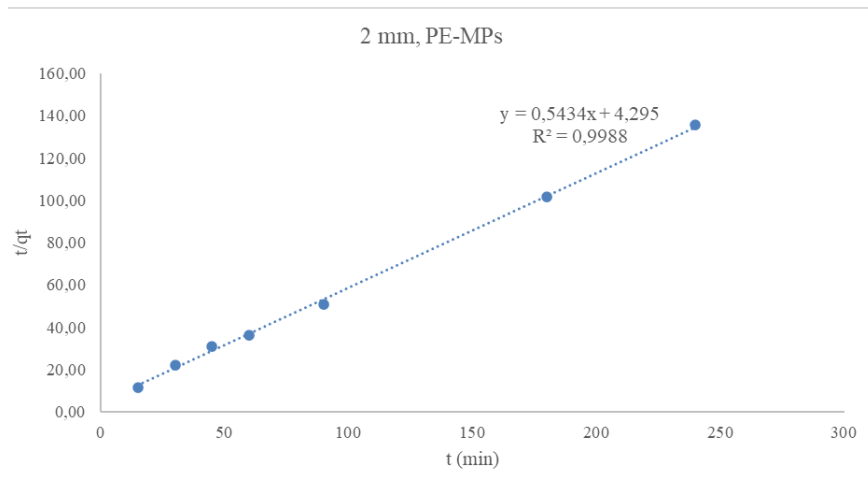
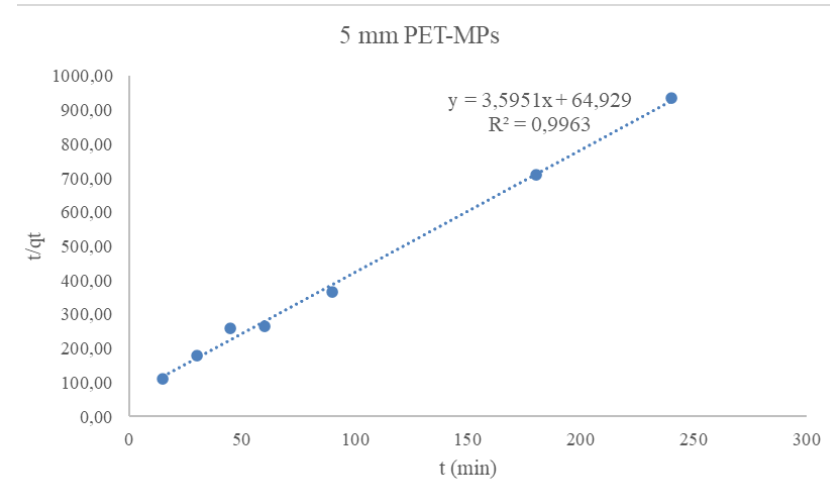
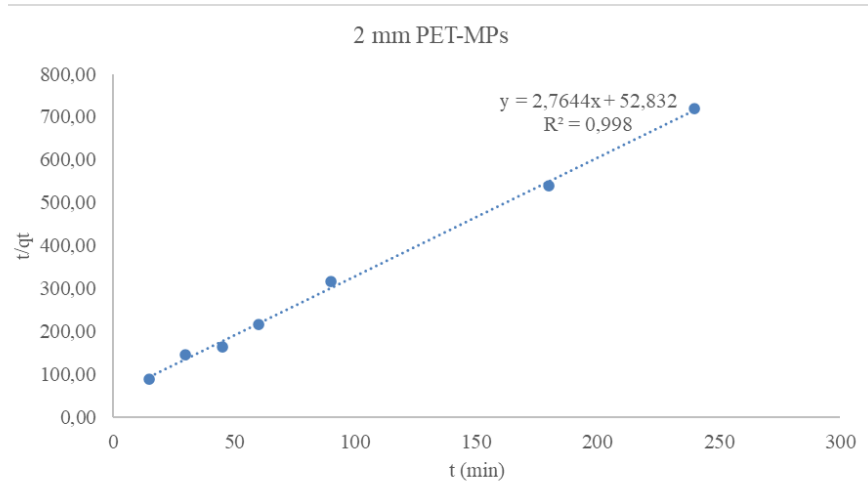


Figure 7. Pseudo-second-order kinetic model of CLAR adsorption by PET-MPs and PE-MPs (Experimental conditions; adsorbent: 3 g/L, t: 15, 30, 45, 60, 90, 180, 240 min, C₀: 6 mg/L CLAR, 50 mL solution, pH 6.0-7.0, 220 rpm, 25 °C, n=2)

1 3.4. Adsorption Isotherms

2 The experimental results were analyzed by using Langmuir and Freundlich isotherm models, so as to
3 evaluate the event that governs the adsorption between the adsorbent and adsorbate in the solution. For
4 this purpose, the adsorption capacities of PET-MPs and PE-MPs in the solution with a C_0 concentration
5 of 2-20 mg/L CLAR were determined at equilibrium time. Langmuir and Freundlich isotherm
6 parameters are given in Table 4. It was determined that 2 mm PE-MPs complies with the Langmuir
7 isotherm model ($r^2=0.94$), while 2 mm PET-MPs ($r^2=0.73$) and 5 mm PET-MPs ($r^2=0.83$) comply with
8 the Freundlich isotherm model. 5 mm PE-MPs does not comply with either Langmuir, or Freundlich
9 isotherm models. Linear regression graphs of PET-MPs and PE-MPs for the Langmuir and Freundlich
10 isotherm models are given in Figure 8 and Figure 9, respectively. CLAR adsorption with 2 mm PE-MPs
11 complies with the Langmuir isotherm model assumes that adsorption occurs in monolayer homogeneous
12 regions on the adsorbent. According to this model, adsorption and desorption occur in equilibrium. The
13 conformity of CLAR adsorption with 2 mm PET-MPs and 5 mm PET-MPs to the Freundlich isotherm
14 model reveals that the adsorption occurs in multilayer heterogeneous regions on the adsorbent.
15 According to this model, the adsorption heat and affinity are not uniformly distributed on the
16 heterogeneous surface and the adsorption is reversible.

17 When the studies in the literature are examined, it is generally determined that the adsorption of
18 pharmaceuticals on plastics obeys the Langmuir and Freundlich isotherms. The adsorption of TC
19 antibiotic on HDPE with a size of 45 μm was investigated by Nguyen *et al.* (2021). The conformity of
20 the adsorption to the linear, Langmuir and Freundlich isotherms was evaluated. The obtained results
21 showed that the adsorption was more suitable for the Langmuir isotherm model ($r^2=0.99$).

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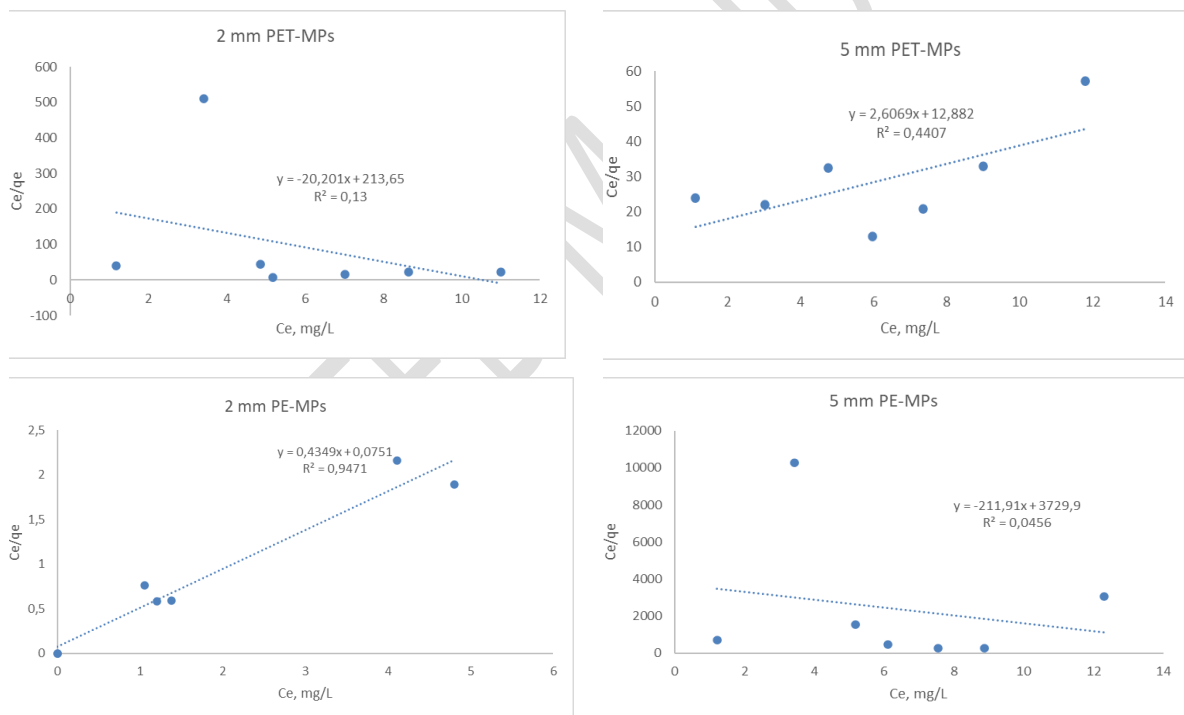
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29 **Table 4.** Langmuir and Freundlich isotherm parameters

	2 mm PET-MPs	5 mm PET-MPs	2 mm PE-MPs	5 mm PE-MPs
Langmuir Isotherm				
Model				
q_{max} (mg/g)	0.049	0.383	2.299	0.004
k_L	4316	33.582	30.618	790403
R^2	0.13	0.44	0.94	0.04
Freundlich				
Isotherm Model				
k_F (mg/g)	35.53	22.95	1.78	2598.4
n	0.76	1.00	6.14	0.58
R^2	0.73	0.83	0.25	0.49

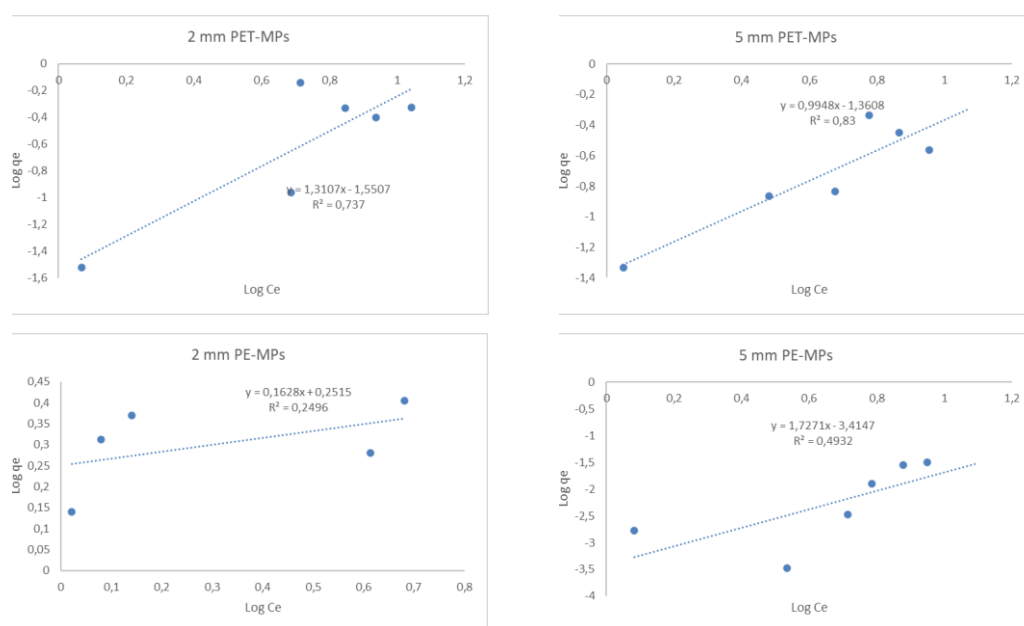
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32 **Figure 8.** Langmuir isotherm graphs of CLAR adsorption with PET-MPs and PE-MPs (Experimental
 33 conditions; adsorbent: 3 g/L, t: 240 min, C_0 : 2-20 mg/L CLAR, 50 mL solution, pH 6.0-7.0, 220 rpm, 25
 34 °C, n=2)

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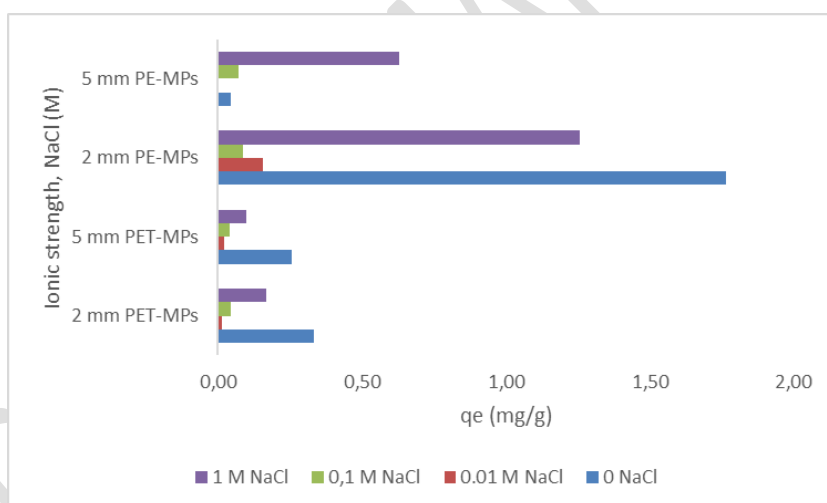
36 **Figure 9.** Freundlich isotherm graphs of CLAR adsorption with PET-MPs and PE-MPs (Experimental
 37 conditions; adsorbent: 3 g/L, t: 240 min, C_0 : 2-20 mg/L CLAR, 50 mL solution, pH 6.0-7.0, 220 rpm, 25
 38 °C, n=2)

39 3.5. Effect of Ionic Strength on CLAR Adsorption

40 In general, the ionic strength of the solution is quite low in adsorption experiments of pharmaceuticals,
 41 carried out with distilled water. However, salinity and hence ionic strength vary greatly in natural waters.
 42 Freshwater sources have significantly less dissolved salt than sea or ocean waters. Therefore, the
 43 pharmaceuticals adsorption capacity of MPs may differ significantly depending on their entry point into
 44 the environment. MPs have different entry points into the natural environment; usually discharged into
 45 the rivers or lakes via wastewater treatment plants and in some cases, directly into the seas and oceans
 46 (Klavins *et al.* 2022).

47 In this study, the effect of ionic strength in the range of 0-1 M NaCl on CLAR adsorption was evaluated.
 48 When the ionic strength of the solution was adjusted to contain 0.01 M NaCl, the adsorption capacity of
 49 all MPs decreased significantly (Figure 10). When salinity increases, the adsorption capacity decreases
 50 because Na^+ ions electrostatically bind to the negatively charged PET-MPs and PE-MPs, disrupting the
 51 charge balance of the surface and reducing the binding sites of the antibiotic (Atugoda *et al.* 2020). Guo
 52 *et al.* (2019) found that the amount of sulfamethoxazole (SMT) adsorption onto MPs decreased with
 53 increasing salinity, revealing the importance of electrostatic reaction in the sorption process. Besides,

54 high Na^+ concentrations increase the density and viscosity of the solution and prevent the movement of
55 analyte from the solution to the surface of MPs (Zhang *et al.* 2020). However, when the ionic strength
56 of the solution in this study reached up to 1 M NaCl the adsorption capacity of all MPs increased
57 compared to other ionic strength experiments, which can be explained by “salting out” effect. The
58 presence of salt ions reduces the solubility of CLAR, increases its hydrophobic interactions with MPs,
59 and thus induces the “salting out” effect. Ma *et al.* (2019) reported that, when the NaCl content increased
60 from 8.75% to 35%, the adsorption capacity of PVC-S (small PVC particles) for TCS increased by
61 43.8%, while the adsorption capacity of PVC-L (large PVC particles) for TCS reached to 73.4%. This
62 was primarily explained by the “salting out” effect that occurred during adsorption, which reduced the
63 solubility of TCS in solution and increased the adsorption of TCS onto PVC. At high salinity, PFOS was
64 found to be easily adsorbed on PE and PS, and the sorption of PFOS on MPs in seawater was also
65 explained by this effect (Joo *et al.* 2021).



66

67 **Figure 10.** Effect of ionic strength on CLAR adsorption (Experimental conditions; adsorbent: 3 g/L PE-
68 MPs and PET-MPs, pH6.0-7.0, t: 4 hours, C_0 : 10 mg/L CLAR, 50 mL solution, ionic strength: 0.01 M
69 NaCl, 0.1 M NaCl, 1 M NaCl, 220 rpm, 25 °C, n=2)

70 4. Conclusions

71 This study has shown that the risk posed by microplastics in aquatic environments is not only due to
72 their chemical content, but also that microplastics have the potential to accumulate antibiotics in water
73 by adsorbing them onto their surfaces. It has been determined that the adsorption of antibiotics onto

74 microplastics depends on solution pH and ionic strength. The sorption behavior of MPs was also
75 influenced by their type and size. Adsorption of antibiotics on MPs has the potential of vectorial
76 translocation of these chemicals and provides a surface for the formation of antibiotic-resistant genes.
77 In this context, the entry of both plastics and antibiotics into aquatic environments should be prevented.

78

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161 **Figure Captions**

162 **Figure 1.** Standard chromatogram for antibiotic CLAR under optimum HPLC-MS conditions (10
163 ng/ μ L)

164 **Figure 2.** SEM images of 2 mm PET-MPs and 5 mm PET-MPs

165 **Figure 3.** SEM images of 2 mm PE-MPs and 5 mm PE-MPs

166 **Figure 4.** FT-IR spectra of PET-MPs and PE-MPs before and after CLAR adsorption (a: 2 mm PET-
167 MP + CLAR; b: 5 mm PET-MP + CLAR; c: 2 mm PE-MP + CLAR; d: 5 mm PE-MP + CLAR)

168 **Figure 5.** Effect of pH on the adsorption of CLAR on PET-MPs and PE-MPs (Experimental
169 conditions; adsorbent: 3 g/L, 2 mm PET-MPs, and 2 mm PE-MPs, t: 4 hours, C_0 : 6 mg/L CLAR, 50
170 mL solution, pH adjustment with 0.1 M HCl, 0.1 M NaOH, 220 rpm, 25 °C, n=2)

171 **Figure 6.** Effect of contact time on adsorption of CLAR by PET-MPs and PE-MPs (Experimental
172 conditions; adsorbent: 3 g/L, t: 15, 30, 45, 60, 90, 180, 240 min, C_0 : 6 mg/L CLAR, 50 mL solution,
173 pH 6.0-7.0, 220 rpm, 25 °C, n=2)

174 **Figure 7.** Pseudo-second-order kinetic model of CLAR adsorption by PET-MPs and PE-MPs
175 (Experimental conditions; adsorbent: 3 g/L, t: 15, 30, 45, 60, 90, 180, 240 min, C_0 : 6 mg/L CLAR,
176 50 mL solution, pH 6.0-7.0, 220 rpm, 25 °C, n=2)

177 **Figure 8.** Langmuir isotherm graphs of CLAR adsorption with PET-MPs and PE-MPs (Experimental
178 conditions; adsorbent: 3 g/L, t: 240 min, C_0 : 2-20 mg/L CLAR, 50 mL solution, pH 6.0-7.0, 220 rpm,
179 25 °C, n=2)

180 **Figure 9.** Freundlich isotherm graphs of CLAR adsorption with PET-MPs and PE-MPs
181 (Experimental conditions; adsorbent: 3 g/L, t: 240 min, C_0 : 2-20 mg/L CLAR, 50 mL solution, pH
182 6.0-7.0, 220 rpm, 25 °C, n=2)

183 **Figure 10.** Effect of ionic strength on CLAR adsorption (Experimental conditions; adsorbent: 3 g/L
184 PE-MPs and PET-MPs, pH6.0-7.0, t: 4 hours, C_0 : 10 mg/L CLAR, 50 mL solution, ionic strength:
185 0.01 M NaCl, 0.1 M NaCl, 1 M NaCl, 220 rpm, 25 °C, n=2)

186

187 **Table Captions**

188 **Table 1.** Retention time and m/z values for antibiotic CLAR under optimum HPLC-MS conditions

189 **Table 2.** Significant FT-IR peaks and identified functional groups of PET-MPs and PE-MPs before and
190 after CLAR adsorption

191 **Table 3.** Sorption rate constants and equilibrium sorption capacities for pseudo-first-order and pseudo-
192 second-order kinetic models

193 **Table 4.** Langmuir and Freundlich isotherm parameters

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218 Competing Interests

219 We wish to confirm that there are no known conflicts of interest related to the work submitted for
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221 Author Contributions

222 Two of the authors contributed to the study conception and design. Material preparation, data collection
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238 Ethical Approval

239 Experimental studies performed in this research study do not involve human or animal participants,
240 neither their organs/tissues etc. No ethical approval is required

241 Consent to Participate

242 Experimental studies performed in this research study do not involve human or animal participants,
243 neither their organs/tissues etc. No consent to participate is required.

244 Consent to Publish

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246 The Data Availability Statement (DAS)

247 Data is available on request from corresponding author.

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