Synthesis and adsorption capacity of biochar derived from Tamarindus indica shell for the removal of heavy metal

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GRAPHICAL ABSTRACT

Abstract

Tamarindus indica shell biochar is employed as an alternate adsorbent precursor for the removal of heavy metal ions from aqueous solutions. It investigated the Tamarindus indica shell biochar's capacity to absorb chromium (Cr), copper (Cu), and Lead (Pb). This study showed the extensive explored how biosorption experimental limitations counting primary metal attentiveness, adsorbent dosage, temperature, and contact time affect the process. The
complete analysis of the Tamarindus indica shell's adsorption capability with respect to chromium, copper, and nickel removal was conducted using a batch adsorption procedure. Determining the amount of heavy metal removal in the aqueous solution proceeded by Gas Chromatography (GC). The experimental data analyzed using the Yoon Nelson and Thomson models to regulate the equilibrium isotherms. The optimal parameters for the overall adsorption model were determined by using ANOVA. Investigate the adsorbent's surface area to determine the presence of heavy metal presents using SEM, XRD, and FTIR techniques. Each researched heavy metal's adsorption capability is listed below: Cr = 6.07 mg/L, Cu = 5.53 mg/L and Pb = 5.497 mg/L with a removal percentage of 64%, 92% and 78%, respectively. The results showed that biochar generated from Tamarindus indica shells is an effective adsorbent for removing copper from aqueous solutions but not a viable biosorbent for removing chromium. Also, the regenerated column's adsorption capability was examined. The outcomes of the research demonstrated that bio-char, which produced from Tamarindus indica shell can be employed as an efficient and reasonably priced adsorbent to remove heavy metal ions from aqueous solutions.

Keywords: Heavy metal, Biochar, Adsorption, ANOVA analysis, Kinetic study, regeneration

1. Introduction

Toxic metals called as heavy metals are discrete metals and metal composites that have harmful effect in people's health. Because heavy metals can impair human health even at low concentrations in the environment, their presence in water streams, air, soil, and food has become problematic [1]. One of the issues that people have is heavy metal pollution in the water, heavy metal can be toxic to the life. It poses a risk to the ecosystem, including to the health of people, animals, and plants. In order to manage the degree of water pollution, The Environmental Protection Agency (EPA) and the World Health Organization (WHO) have established the maximum permissible discharge level into ecosystems [2]. Because to population increase, rapid industrial and agricultural development, and a high concentration of harmful heavy metals in water sources, there is a threat to human health and natural systems. Exposure to heavy metals like lead (Pb), chromium (Cr), and copper (Cu) can cause heavy metal poisoning [3]. When heavy metals bind to specific cell components, organs cannot function properly. The effects of heavy metal poisoning can be irreversible and life-threatening. Most heavy metals are absorbed, stored, and even accumulate in the human body, causing persistent problems [4]. Hence, before releasing waste aqueous solution into the environment, these heavy metals from industrial influents must be removed. A critical issue is
the removal of such hazardous metal ions from aqueous solutions [5]. A variety of methods have been used to remove heavy metal ions from aqueous solutions, including chemical precipitation, ion-exchange, adsorption, membrane filtration, electrochemical treatment methods, and so on [6]. One of the most significant physico-chemical treatment methods for removing heavy metals from aqueous solutions is adsorption. The natural availability of biomaterials in the environment and their inexpensive cost makes using biochar, which is made from them, quite popular [7]. Several attempts have been undertaken to adsorb heavy metals from aqueous solutions using the least expensive and uncommon adsorbents, such as aquatic plants, plant wastes, agricultural and industrial by-products. The primary goal of this research is to use the adsorption technique to remove heavy metals like chromium (Cr), copper (Cu), and lead (Pb) [8]. Heavy metals were removed using biochar made from Tamarindus indica shells as an adsorbent. Although there have been many applications for biochar, they have not gotten significant consideration. Assessment of bio-char as low-cost adsorbent for aqueous treatment should be painstaking [9]. As a result, bio-char, a byproduct of the shell of Tamarindus indica, was used as a substitute adsorbent precursor in this work for the adsorption-based removal of heavy metal ions from aqueous solutions. After the adsorption procedure, the level of heavy metals in an aqueous solution is assessed using Gas chromatography (GC) [10]. For the purpose of separating and analysing chemicals that can be vaporized without decomposing, it is an analytical chemistry technique. The experimental data was analyzed using the Yoon Nelson and Thomson models to establish the equilibrium isotherms [11]. The ANOVA analysis examined statistically significant variations between the means and the treatment variance. SEM, XRD, and FTIR techniques should be used to examine the adsorbent's surface area to detect the presence of heavy metals [12]. The thorough analysis demonstrates the Tamarindus indica shell-derived biochar's adsorption potential.

2. Materials and Methods

2.1. Biochar preparation

The biochar was made using a common leftover stalk of Tamarindus indica shell that was discovered as a pertinent feedstock. The stalks were collected from farmland [13]. Deionized water was used to wash the Tamarindus indica shell numerous times until the soil was
removed. Using a multi-purpose swing grinder, a powdered sample (1mm) was created after 3–4 days of air drying [14]. Following that, each trial was carefully packed into a ceramic pot and sealed with a lid to produce an oxygen-limited environment for the heating process. Heating administered in a muffle furnace at a degree of 50°C min⁻¹ until a desired ultimate temperature of 400°C was reached, which was then sustained for 3 h [15]. The biochar product was powdered after it had naturally cooled enough that the entire sample could pass a 150-mesh sieve while still being reserved on a 100-mesh sieve [16]. Fresh biochar trials of element size 60-100 mm were consequently attained.

2.2. Preparation of synthetic aqueous solution

To create stock solutions containing 1000 mg/L of metal ions, analytical grade CuSO₄·5H₂O, CrCl₃·6H₂O, and Pb metal were dissolved in distilled water. All the chemicals utilized were of the highest analytical quality [17]. The studies used distilled water exclusively. Prepared by dissolving 2.5 g of CuSO₄·5H₂O, 4.2 g of CrCl₃·6H₂O, and 1.5 g of Pb (metal) in 1000 mL of distilled water, stock solutions of 1000 mg/L for copper, chromium, and lead ions [18].

2.3. Adsorption study

Inner diameter of 3 cm and 50 cm length glass column used for adsorption study. Particle sizes of the biochar, which is made from the shell of the tamarind indica plant, range from 0.5 to 1.5 mm [19]. The column was filled with adsorbent, and the bottom was covered with glass wool. From literature survey the optimum height of 10 cm column used for this study [20]. The laboring flow rates ranged from 2.0 mL/min. At predefined intervals, the residual heavy metal content in the effluent samples was assessed. Column investigations ended when the column neared fatigue [21]. For practical reasons, the column studies are conducted at room temperature.

2.4. Gas chromatography (GC)

The water used for GC met the requirements of ISO Grade 78-2:1982, and the heavy metal copper, chromium and lead stock standard solutions were obtained [22]. Heavy metal solution from several sources was used for the method validation and calibration trials as well as an independent source for quality control [23]. The gradient pump in the GC system had a
flow rate of 0.50 mL/min., an auto sampler with a 10 µL injection loop, a column thermostat set at 27°C, an eluent generator supplying 40 ml/L, and a conductivity detector [24]. The suppression column was a LCGC, and the column was a silicon-based column, both in 4mm format. Each sample ran for a total of 20 minutes [25]. The working range, performance, and calibration data for a concentration decade looking at standard solutions of heavy metal concentrations were evaluated statistically.

2.5. Kinetic study

2.5.1 Yoon Nelson Model for adsorption study

Due to the Yoon-Nelson Model's lack of a need for in-depth adsorbate understanding, it is easier [26]. According to this model, the likelihood of each adsorbate molecule adhering to the adsorbent decreases at a rate that is proportional to both the likelihood of adsorbate adsorption and the likelihood of adsorbate breakthrough on the adsorbent [27]. It is a model for a single component system, the linearized equation of model expressed as Eq:

\[ \ln \left( \frac{C_t}{C_0 - C_t} \right) = k_{yt} t - \tau k_{yt} \]

The rate constant is \( k_{yt} \) (min\(^{-1}\)), and (min) is the shortest period necessary for 50% adsorbate breakthrough. Yoon Nelson linear plots are used as a model. The intercept and slope of the linear plot of the \( \ln \left( \frac{C_t}{C_0 - C_t} \right) \) vs. \( t \) graph can be used to determine the parameters \( k_{yt} \).

2.5.2. Thomson Model for adsorption study

By means of Thomson model, the association among internal then external progressions of adsorption found [28]. The Thomson model described as

\[ \ln \left( \frac{C_0}{C_t} - 1 \right) = k_{TH} q_e W - k_{TH} C_0 t \]

2.6. ANOVA analysis

An experiencing cumulative inconsistency originating from exclusive statistics established is separated from methodical elements and random factors using a statistical inquiry approach called analysis of variance (ANOVA) [29]. It establishes how a dependent variable in a regression analysis is impacted by an independent unknown. A one-way ANOVA is used in this study to analyze the connection between the dependent and independent variables. To assess the impact of persuasive parameters on response, the ANOVA method has frequently been used [30]. This is frequently done through cross authentication, testing, and estimation.
The underpinning for scheming taxing is completed exclusively of testing model [31]. Yet, this is frequently not practicable in corporeal science because there are frequently not enough examples [32]. Then, A more effective method is used, which repeatedly removes items from the data collection to do caricature forecast testing.

\[
F = \frac{MST}{MSE}
\]

Where:

F = ANOVA coefficient
MST = Mean sum of squares due to treatment
MSE = Mean sum of squares due to error

Experimental data should be analyzed using a second-order polynomial model to increase the unpredictability in the progression of coagulation and flocculation. A design expert also established the analysis of the change.

2.7. Characterization study

2.7.1. SEM analysis

The material and particle size distribution were graphically described using scanning electron microscope (SEM) equipment. The Shimadzu SD analyzer performed the SEM test [33]. Using a PerkinElmer Z SD3500 analyzer, a thermogravimetric analysis was done to calculate the sample mass as a function of temperature and constant heating rate.

2.7.2. XRD study

Using the X-ray diffraction (XRD) method and an ARL EQUINOX 9900 XRD with V X-ray diffractometer outfitted with monochromatized Cu K radiation (1.4258), the crystal structure and phase purity were determined [34]. Energy dispersive X-ray spectroscopy was performed using a Phoneix instrument X-Max energy dispersive X-ray spectrometer. Cu₂O SPs' morphology was evaluated using a field emission scanning electron microscope. [35]. On an XPS spectrometer, X-ray photoelectron spectroscopy (XPS) was conducted.

2.7.3. FTIR Analysis

Fourier transform infrared spectroscopy was used to identify the surface species (FT-IR). A Shimadzu-450 spectrometer was used to capture the FT-IR spectra in Cu pellets. Copper was added to the samples after which they were dehydrated at 150 °C and exposed to ultraviolet
bright [36]. The capsules were tested instantly after processing under natural illumination in the mid-infrared spectrum.

2.8. Regeneration of adsorbent

By electrically heating the adsorbent to 280°C in both an inert and an environment with air, thermal regeneration was accomplished [37]. The adsorbent was heated to between 300°C and 500°C in a muffle furnace during the hot water extraction process, twice washed with DI water and an HCl solution, and then dried for an additional two hours in a hot air oven [38]. The effectiveness of the regenerated adsorbent's regeneration was determined by measuring the heavy metal removal capacity.

3. Result and Discussion

3.1. Adsorption study

3.1.1. Chromium Adsorption (Cr):

Batch adsorption research was conducted to ascertain the amount of chromium removed. The chromium (Cr) concentration range of 4.2 g/L was employed for the adsorption research as a reference value [39]. 10 cm was chosen as the ideal height for the experimental investigation. The Tamarindus indica shell-derived biochar was placed in a class column with 0.5 mL/min exit ranges. The initial treatment efficiency started at 15 minutes in the 3.8 g/L level. After increasing it for the next 15 minutes, the column's removal efficiency reached 1.5 g/L after 105 minutes [40]. As shown in Table.1 and Figure.1, the column reached saturation under these circumstances after 120 minutes.

<table>
<thead>
<tr>
<th>Time (Min)</th>
<th>Chromium Concentration g/L</th>
</tr>
</thead>
<tbody>
<tr>
<td>15</td>
<td>3.8</td>
</tr>
<tr>
<td>30</td>
<td>3.3</td>
</tr>
<tr>
<td>45</td>
<td>2.9</td>
</tr>
<tr>
<td>60</td>
<td>2.5</td>
</tr>
<tr>
<td>75</td>
<td>2.4</td>
</tr>
<tr>
<td>90</td>
<td>1.7</td>
</tr>
<tr>
<td>105</td>
<td>1.5</td>
</tr>
<tr>
<td>120</td>
<td>1.5</td>
</tr>
</tbody>
</table>
3.1.2. Copper Adsorption (Cu):

Batch adsorption research was conducted to ascertain the amount of copper removed. The copper (Cu) concentration of 2.5 g/L or less was selected as the reference level for the adsorption experiment [41]. It was determined that 10 cm was the ideal height for the experimental investigation. After being filled with biochar made from Tamarindus indica shells and having exit ranges of 0.46 mL/min, the column reached saturation after 105 minutes, as shown in Table.2 and Figure.2.

<table>
<thead>
<tr>
<th>Time (Min)</th>
<th>Copper Concentration g/L</th>
</tr>
</thead>
<tbody>
<tr>
<td>15</td>
<td>2.4</td>
</tr>
<tr>
<td>30</td>
<td>2.0</td>
</tr>
<tr>
<td>45</td>
<td>1.6</td>
</tr>
<tr>
<td>60</td>
<td>1.2</td>
</tr>
<tr>
<td>75</td>
<td>0.75</td>
</tr>
<tr>
<td>90</td>
<td>0.20</td>
</tr>
<tr>
<td>105</td>
<td>0.20</td>
</tr>
</tbody>
</table>
3.1.3. Lead Adsorption (Pb):

To ascertain the Lead elimination by adsorption investigation, a batch adsorption study was conducted. Lead (Pb) concentrations between 1.5 g/L were selected as a starting point for the adsorption experiment [42]. During the experimental investigation, a height of 10 cm was determined to be ideal. The Tamarindus indica shell-derived biochar was placed in a class column with exit ranges of 0.45 mL/min. The initial treatment efficiency started at 15 minutes in the 1.4 g/L level. In the following 15 minutes, the removal efficiency increased, and after 75 minutes, the column's removal efficiency was 0.33 g/L [43]. Under this condition, the column became saturated after 90 minutes, as shown in Table.3 and Figure.3.

Table.3 Lead removal

<table>
<thead>
<tr>
<th>Time (Min)</th>
<th>Lead Concentration g/L</th>
</tr>
</thead>
<tbody>
<tr>
<td>15</td>
<td>1.4</td>
</tr>
<tr>
<td>30</td>
<td>1.1</td>
</tr>
<tr>
<td>45</td>
<td>0.98</td>
</tr>
<tr>
<td>60</td>
<td>0.72</td>
</tr>
<tr>
<td>75</td>
<td>0.33</td>
</tr>
<tr>
<td>90</td>
<td>0.33</td>
</tr>
</tbody>
</table>
3.1.4. **Heavy metal adsorption**

The heavy metals (Cr, Ca, and Pb) used in this extensive adsorption investigation were taken in the range of 4.2 g/L, 2.5 g/L, and 1.5 g/L. In accordance with the literature, the ideal column height was determined to be 10 cm. Gas chromatography (GC) was used to analyze the amount of heavy metal elimination every 15 minutes [44]. Initial treatment efficiency in the analysis of chromium adsorption started at 15 minutes in the 3.8 g/L level. After being increased for the following 15 minutes, the column's removal efficiency reached 1.5 g/L in 105 minutes, and in 120 minutes the column reached saturation. Chromium was removed from the biochar made from Tamarindus indica shells at a 64% removal rate [45]. The initial treatment efficiency started at 15 minutes in the 2.4 g/L level in the subsequent experiment about copper removal at a concentration of 2.5 g/L. In the following 15 minutes, the removal efficiency rose, and after 90 minutes, the column's removal efficiency was 0.20 g/L with a 92% removal rate. The third lead elimination study went forward with a concentration of 1.5 g/L. In the following 15 minutes, the removal efficiency rose, and after 75 minutes, the column's removal efficiency was 0.33 g/L with a 78% removal rate [46]. This thorough study demonstrated that the biochar made from Tamarindus indica shells, with an adsorption column height of 10 cm, was effective at removing copper with a 92% removal rate.

3.2. **Gas Chromatographic study**

The samples were taken after the adsorption research and put in vials that were maintained in the fridge in order to analyze the chromatogram. A 10 µl sample was taken from the intake
region and passed through the mobile phase and stationary phase. [47]. The perfect heavy metal level determined by using graph of GC result. In order to assess graphical representation, Class VP Software and GC was hired to establish the quantity of heavy metals [48]. The peak's height and area in the graphical representation were used to determine the sample's heavy metal concentration.

![Graphs of heavy metals](image)

**Figure.4 Heavy metal (Cr, Cu & Pb) analysis by Gas Chromatography (GC)**

### 3.3. Yoon Nelson model for adsorption study

According to results, heavy metal removal exhibited a stronger adsorption break through with a copper $R^2$ value larger than 0.9835, lead $R^2$ value 0.9101, and chromium $R^2$ value 0.8754 [49]. In the row of heavy metals, the rate constants were 4.51; 5.20; and 4.93. Heavy metals have Ky(min$^{-1}$) values of 0.474, 0.624, and 0.551. This meant that the kinetic values of heavy metal removal were mostly responsible for the experimental outcomes.

**Table.4 Heavy metal removal by Yoon – Nelson model**

<table>
<thead>
<tr>
<th>Materials</th>
<th>Ky(min$^{-1}$)</th>
<th>$\tau$(hr)</th>
<th>$R^2$</th>
</tr>
</thead>
<tbody>
<tr>
<td>Chromium</td>
<td>0.474</td>
<td>4.51</td>
<td>0.8754</td>
</tr>
<tr>
<td>Copper</td>
<td>0.624</td>
<td>5.20</td>
<td>0.9835</td>
</tr>
<tr>
<td>Lead</td>
<td>0.551</td>
<td>4.93</td>
<td>0.9101</td>
</tr>
</tbody>
</table>
3.4. Thomson model for adsorption study

The elimination of heavy metals through adsorption was analyzed using the Thomson model. The projected break through curve and the measured adsorption process agreed. The mass (m), concentration time (t), and copper metal's regression coefficient (R2) of 0.9817 all affect the value of \( k_t \) [50]. As seen by the lowest \( k_t \) value at highest Co, the adsorption kinetics supported at the highest adsorbate concentration. The initial \( k_t \) values increased to 0.9104 for copper, 0.7159 for chromium, and 0.8273 for lead from lower levels. According to Table 4 and Figure 5, Copper, Chrome, and Lead equilibrium uptake capacities (qo), which were 73.50, 27.35, and 41.72 respectively, were somewhat increased. [51]. The decline in qo demonstrated that there is an inverse correlation between bed height, contact time, and adsorption capacity.

<table>
<thead>
<tr>
<th>Heavy metal</th>
<th>( k_t \times 10^{-3} ) (mL/(min.mg))</th>
<th>qo (mg/g)</th>
<th>( R^2 )</th>
</tr>
</thead>
<tbody>
<tr>
<td>Chromium (Cr)</td>
<td>0.7159</td>
<td>27.35</td>
<td>0.9642</td>
</tr>
<tr>
<td>Copper (Ca)</td>
<td>0.9104</td>
<td>73.50</td>
<td>0.9817</td>
</tr>
<tr>
<td>Lead (Pb)</td>
<td>0.8273</td>
<td>41.72</td>
<td>0.9635</td>
</tr>
</tbody>
</table>
3.5. ANOVA for Quadratic model

The Model F-value of 725.64 suggests that the model is significant. Just 0.2% of the time may noise be the cause of an F-value this high. In cases when the P-value is fewer than 0.0600, archetypal relations are considered important [52]. If the value is more than 0.0001, then the model relations are not substantial. If there are many extraneous terms, model reduction might improve this model. The F-value of 0.6532 for dearth of suitability shows that the absence of appropriateness is not significantly different from the pure error [53]. The unintentional likelihood of noise causing a significant Lack of Fit F-value is 92.56%.

**Table.6 ANOVA for Quadratic model**

<table>
<thead>
<tr>
<th>Source</th>
<th>Sum of Squares</th>
<th>df</th>
<th>Mean Square</th>
<th>F-value</th>
<th>p-value</th>
<th>Remarks</th>
</tr>
</thead>
<tbody>
<tr>
<td>Model</td>
<td>481.62</td>
<td>19</td>
<td>48.27</td>
<td>725.64</td>
<td>&lt; 0.0001</td>
<td>Significant</td>
</tr>
<tr>
<td>A-Initial</td>
<td>297.41</td>
<td>1</td>
<td>256.74</td>
<td>5471.77</td>
<td>&lt; 0.0001</td>
<td></td>
</tr>
<tr>
<td>Concentration</td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>B-PH Solution</td>
<td>197.52</td>
<td>1</td>
<td>104.56</td>
<td>1755.15</td>
<td>&lt; 0.0001</td>
<td></td>
</tr>
<tr>
<td>C-Contact Time</td>
<td>44.56</td>
<td>1</td>
<td>27.45</td>
<td>384.78</td>
<td>&lt; 0.0001</td>
<td></td>
</tr>
<tr>
<td>D-Adsorbent Dosage</td>
<td>84.31</td>
<td>1</td>
<td>88.12</td>
<td>1378.16</td>
<td>&lt; 0.0001</td>
<td></td>
</tr>
<tr>
<td>AB</td>
<td>0.9415</td>
<td>1</td>
<td>0.8417</td>
<td>9.84</td>
<td>0.0032</td>
<td></td>
</tr>
<tr>
<td>AC</td>
<td>3.21</td>
<td>1</td>
<td>3.56</td>
<td>38.73</td>
<td>&lt; 0.0001</td>
<td></td>
</tr>
<tr>
<td>AD</td>
<td>3.74</td>
<td>1</td>
<td>3.20</td>
<td>41.97</td>
<td>&lt; 0.0001</td>
<td></td>
</tr>
<tr>
<td>BC</td>
<td>4.59</td>
<td>1</td>
<td>4.12</td>
<td>50.85</td>
<td>&lt; 0.0001</td>
<td></td>
</tr>
<tr>
<td>BD</td>
<td>0.2411</td>
<td>1</td>
<td>0.1048</td>
<td>1.75</td>
<td>0.2124</td>
<td></td>
</tr>
<tr>
<td>CD</td>
<td>2.73</td>
<td>1</td>
<td>2.77</td>
<td>34.11</td>
<td>&lt; 0.0001</td>
<td></td>
</tr>
</tbody>
</table>
3.6. Characterization of Biochar adsorbent

3.6.1. SEM analysis of Biochar adsorbent

Figure 7 shows the SEM images of the adsorbent; the wolfram deposit and diatomite-based ceramic have a shape that is nearly spherical and a rough, porous surface. From the inside to the exterior of ceramicite, there are numerous pores [54]. Thus, the surface and internal structure of ceramsite is likely to experience Cu²⁺ ion adsorption in solution. The porous structural nature received a dump of the ca²⁺ adsorbent that was already present in the surface area. The Pb component was supported by the adsorbent's surface-level structure [55]. Optimizing the circumstances for getting heavy metal particle dispersions to apply to a fibrous carrier was the challenge. As crosslinking bridges, heavy metals were used to create adsorbent nanoparticles [56]. The molar ratio is the primary determinant of the process parameters for a given constant concentration of heavy metal in mixtures, and the properties of the particles indicate the presence of heavy metal in the adsorbent.

![Figure 7 SEM analysis of Biochar adsorbent](image-url)
3.6.2. XRD analysis of Biochar adsorbent

The typical XRD pattern of the Cu, Cr, and Pb sample is displayed in Figure 8. All the deflection crests of the heavy metal sample were in upright contract with the cubic phase of the heavy metal, which had a framed relentless of 5.7145 nm. [57]. The replications of hydroplanes of cubic heavy metals were thought to be responsible for the peaks at 3 values of 33.75°, 28.52°, 30.13°, 56.84°, and 64.82°. There were also found to be other impurities, like metal Cu, Cr, and Pb [58]. The heavy metals sample's good crystallinity was shown by the strong and precise diffraction peaks. The EDS analysis revealed that the copper to oxygen atom ratio was nearly 3:2, which supported the hypothesis that the synthesized sample included the heavy metal.

![XRD analysis of Biochar adsorbent](image)

3.6.3. FTIR analysis of Biochar adsorbent

Figure 9 showed the FTIR spectra of the heavy metal adsorbent. The modest absorption peaks at 5841 and 3574/cm, respectively, represent the stretching and bending vibrations of the OH-bond, demonstrating the simultaneous existence of coordinated water and a few adsorbed water [59]. The peak at 1682 cm for the adsorbent in Figure 9 might be attributed to C-H flexural vibration, whereas the bands at 1678 cm and 1578 cm are attributed to O-H deformation vibration and C=C stretching vibration, respectively. The carboxyl groups' (-C=O-) and C-H bending vibrations, respectively, are responsible for the large absorption peaks at 1547 cm and 745 cm, respectively [60]. The wide band seen between 1384 and 1012 cm is caused by vibrations that stretch the C-O bond and bend the O-H bond (in plane).
3.7. Column regeneration study

In order to evaluate the adsorbent's reusability, the cleaned column was utilized once more for the ensuing adsorption cycle, which was followed by four further adsorption cycles. To test for reusability, the adsorbent was repackaged and used fresh once more [61]. corresponding to three study cycles. The effectiveness of heavy metal removal decreased after the first four cycles.

4. Conclusion

In this study, a low-cost alternative adsorbent for the removal of the ions Chromium (Cr), Copper (Cu), and Lead (Pb) from aqueous solution was examined. The bio-char was made from the shell of the Tamarindus indica plant. For the elimination of chromium (Cr), copper (Cu), and lead (Pb), the ideal adsorption conditions were identified as a function of pH, adsorbent dosage, initial metal ion concentration, and solution contact duration. According to the study, the following is a list of heavy metals' adsorption capacities: With elimination percentages of 64%, 92%, and 78%, respectively, Cr, Cu, and Pb are at 6.07 mg/L, 5.53 mg/L, and 5.497 mg/L, respectively. The findings demonstrated that biochar made from Tamarindus indica shells is not a viable biosorbent for chromium elimination but performs well as an adsorbent to extract copper from liquid samples. Kinetic analysis the adsorption capability of biochar material against heavy metal was well calculated with $R^2 = 0.9817$, according to the Yoon Nelson and Thomson models. The surface alteration caused by heavy metal adsorption in the adsorbent is seen in the SEM, XRD, and FTIR characteristics. The regenerative capability of the adsorbent in contradiction of heavy metal adsorption studied.
According to this thorough study's findings, Tamarindus indica shell bio-char seems to be a reliable, affordable, and for exclusion of heavy metals from liquid samples, use a replacement sorbent pioneer.

Conflict of Interest
The authors declare no conflict of interest.

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