

1 **Factorial Design and Optimization of Date Stone as A Natural Coagulant for**
2 **Organic and Heavy Metals Removal from Industrial Wastewater**

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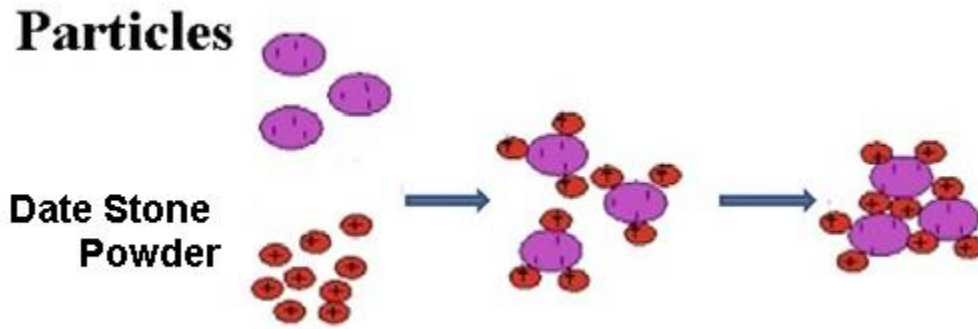
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25 **GRAPHICAL ABSTRACT**



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27

28 **Abstract**

29 Several chemical coagulants previously utilize for wastewater treatment with significant
 30 performance in removing heavy metals and other parameters. However, their cost effective and
 31 the residual of toxic chemical precipitates that pose problems to human health and the
 32 environment. Therefore, using plant-based natural coagulants is considered as an alternative
 33 technique which is non-toxic, biodegradable and environmentally friendly. This research aims to
 34 explore the performance of date stones as a natural coagulant in iron and steel plant wastewater
 35 treatment and to optimize the operating parameters to assess the feasibility of using date stones in
 36 the wastewater treatment sector. Response Surface Methodology (RSM), a statistical experimental
 37 design, was used to improve the COD, TSS, NH₃-N, and heavy metals removal efficiency using
 38 1.4 g/200 mL date stones as control parameters, as well as pH and settling time. At pH 8, the most
 39 significant removal efficiency for COD, NH₃-N, Fe, Mn, Al, Cu, and Ni was 61, 63, 93, 93, 96.5,
 40 51, and 86 %, respectively. The quadratic models for the parameters chosen were found to be
 41 significant with low probability (<0.001), except for NH₃-N (0.004), Fe (0.0042), and Ni (0.0025).
 42 The study's results revealed the potential of utilizing date stones as a natural coagulant for the
 43 treatment of iron and steel industrial wastewater.

44

45 **Keywords:** Industrial Wastewater, Natural coagulant, Date Stone, Treatment, Removal
 46 Efficiency, Heavy Metals, Factorial Design and Optimization.

47 **1. Introduction**

48 In recent times, water consumption has increased due to industrialization, urbanization, and
49 population growth (Ali & Tien Seng, 2018), and, accordingly, wastewater from the various
50 activities of industrialization and urbanization is also increasing, making access to clean and safe
51 water a critical issue (Abujazar, Fatihah, Kabeel, Sharil, & Abu Amr, 2018). Inappropriate
52 mistreatment or untreated wastewater containing contaminants such as suspended solids,
53 pathogens, nutrients, and heavy metals are hurtful and hazardous to the environment and lead to
54 numerous pollution problems (M. Y. D. Alazaiza et al., 2022; Mukherjee, Mandal, Ganguly, &
55 Chatterjee, 2016). Furthermore, leading to waterborne diseases, which affect human health and are
56 responsible for about 80% of the world's diseases (Lundqvist, Mandava, Lungu-Mitea, Lai, &
57 Ahrens, 2019; Ugwu, Umuokoro, Echiegu, Ugwuishiwu, & Enweremadu, 2017); therefore, the
58 best way to combat freshwater scarcity and waterborne diseases is to treat and reuse wastewater
59 (Abujazar, Fatihah, Lotfy, Kabeel, & Sharil, 2018).

60 The production of effluents in different industrial processes has posed several
61 environmental risks as a result of rapid industrialization (Mahmood et al., 2019). Water and soil
62 contamination can result from indiscriminate dumping of these effluents. Besides, the effects on
63 abiotic components such as soil and water substantially impact living organisms' health (Chhonkar,
64 Datta, Joshi, & Pathak, 2000). Huge quantities of industrial effluents are produced daily all over
65 the world. Industrial wastewater is rich in chemical dyes, sodium salts of organic acids, and lignin
66 and has a significant concentration of COD, oils, detergents, fats, and suspended solids
67 (Muralimohan, Palanisamy, & Vimaladevi, 2014; Tobajas, Alicia M. Polo, Mohedano, &
68 Rodriguez, 2014).

69 Sometimes, wastewater contains heavy metals. These wastewaters containing heavy metals
70 mainly come from anthropogenic sources such as farms or mining that do not use environmentally
71 friendly techniques or from natural disasters such as earthquakes, storms, and volcanoes that
72 introduce toxic substances into the wastewater (Ahmed, Aktar, Zaman, Jahan, & Bari, 2020; Helen
73 Kalavathy & Miranda, 2010; Nath, Mishra, & Pande, 2019). Heavy metals such as arsenic (As),
74 lead (Pb), copper (Cu), cadmium (Cd), nickel, zinc (Zn), and chromium (Cr) are highly toxic. Even
75 at low concentrations, they are considered the most critical harmful wastes in freshwater reservoirs
76 because they are harmful, non-biodegradable, and inherently long-lived (Azimi, Azari,

77 Rezakazemi, & Ansarpour, 2017; Nath et al., 2019; Vikashni, Matakite, Kanayathu, & and
78 Subramanium, 2012). As much as chemical usage continues on its current trend, removing these
79 poisons from the environment will be challenging (Abujazar, Karaağaç, Abu Amr, Alazaiza, &
80 Bashir, 2022).

81 Consequently, effort must be made to eliminate environmental toxic substances from
82 bodies of water. Each industrial wastewater treatment procedure produces treatment outcomes, but
83 the results vary. However, most of these systems employed in the detoxification process have
84 several serious drawbacks operating and maintenance expenses, collateral harm, and complicated
85 treatment processes (M. Alazaiza et al., 2022; Ali & Tien Seng, 2018). The production of
86 secondary waste characterizes conventional treatment processes after the treatment process, such
87 as toxic sludge, which endangers human health and the environment.

88 The shortcomings of the industrial wastewater treatment process include that it has limited
89 capabilities in the treatment process, is capable of leakage, is affected by the weather, and is not
90 treated thoroughly. Concerted efforts have been made in the field of research and development to
91 utilize new plant species and components that can be used as natural coagulants, such as date
92 kernel powder, which is convenient, easy to operate, simple in design, economically inexpensive,
93 and does not produce secondary results. Several studies recently reported the effectiveness of
94 different types of natural coagulants for wastewater treatment. Rifi et al., (2022) utilized *Moringa*
95 *oleifera* as a natural coagulant for treating the agricultural wastewater produced from olive oil
96 industry. The study reported significant removal for turbidity and COD from agricultural
97 wastewater. Iber, Okomoda, Rozaimah, & Kasan, (2021) reviewed the performance of chitosan as
98 a natural coagulant for aquaculture wastewater treatment. Besharati Fard et al., (2021) utilized
99 *Lallemantia mucilage* as a natural coagulant for the treatment of saline oily wastewater.
100 Satisfactory removal for COD was reported in this study. However, the performance of natural
101 coagulants for heavy metals removal from industrial wastewater was not well documented.

102 The effectiveness of date stones as a natural coagulant for organic removal from industrial
103 wastewater and their performance for heavy metals removal from industrial wastewater are
104 evaluated and discussed in this paper. The proper experimental settings and the statistical
105 relationship between variables and response for employing date stones as a natural plant-based
106 coagulant for industrial wastewater treatment are investigated.

107 **2. Materials and Methods**

108 Raw industrial wastewater was obtained from Karabuk iron and steel factory, Karabuk, Turkey.
109 The wastewater samples were collected from the discharge point of the factory and later on
110 transported to the laboratory in a cool box within one hour of the collection; if not used
111 immediately, the samples were kept at 25°C in the dark until.

112 **2.1 Preparation of Date Stone Powder**

113 Date stones Figure 1 were obtained from a household Gaza strip, Palestine, and transferred to
114 Karabuk University, Turkey. To remove sticking pieces, the date stone was cleaned with distilled
115 water. The stones were dried under atmospheric temperature first and then inside an oven for about
116 eight (8) hours at 50°C. to make the date stones easy to crush. The crushing of the date stones was
117 carried out for size reduction using a (Retsch RS 200) grinder to obtain powder form for the
118 experiments.

119



120

121 **Figure 1.** Date stone and powder.

122

123 **2.2 Analytical Study**

124 The characterization parameters and strategies utilized are shown in Table 1. During the tests, the
125 pH of the samples was adjusted with a 1 N H₂SO₄/NaOH solution (Hanson, 2015).

126 **Table 1.** Characterization parameters and methods.

Parameters	Method
pH	pH meter
Color (Pt-Co)	SM 2120 C
TSS (mg/L)	SM 2540 D
COD (mg/L)	ASTM D1252-A
Ammonia-nitrogen NH ₃ -N (mg/L)	TS EN ISO 11732
Manganese "Mn" (mg/L)	TS EN ISO 11885
Iron "Fe" (mg/L)	TS EN ISO 11885
Zinc "Zn" (mg/L)	TS EN ISO 11885
Aluminum "Al" (mg/L)	TS EN ISO 11885
Nickel "Ni" (mg/L)	TS EN ISO 11885

127

128 **2.3 Experimental Procedure**

129 The coagulation-flocculation process was simulated using Orbital shaker (Type: PSU-10i,
 130 no:010144-1404-0228, Latvia), and three 500 mL beakers were used to test the effect of the
 131 coagulant dose. Each beaker held 200 mL of sample. The timing and speed for rapid and slow
 132 mixing were set using the shaker apparatus's automated controller. In this investigation, the
 133 coagulation-flocculation technique included 5 minutes of rapid mixing at 200 rpm, 15 minutes of
 134 slow mixing at 90 rpm, and 60 minutes of settling for farther testing for removal efficiency of
 135 COD, TSS, ammonia-nitrogen NH₃-N, and heavy metals (Manganese "Mn," Iron "Fe", Zinc "Zn",
 136 Aluminum "Al" and Nickel "Ni", Throughout this step of the test, the starting pH (8) of the sample
 137 was kept uncorrected. Coagulation was tested on the removal efficiency of COD, and NH₃-N.

138 The optimal date stone powder dosage found in the prior experiment was next examined
 139 to see how pH (ranging from 5-10) affected efficient removal for the desired parameters. Before
 140 adding the coagulant, the pH was adjusted using 1M of HCl solution and 1M of NaOH solution.
 141 To reduce the potential of solids settling, industrial wastewater samples were vigorously shaken
 142 prior to coagulation; efficiency removal is computed as follows:

$$143 \text{ Removal efficiency(\%)} = \left[1 - \left(\frac{C_f}{C_i} \right) \right] * 100 \quad (1)$$

144 where C_i and C_f correspond to the initial and final values of each parameter
 145 The characterization of the iron and steel industry wastewater used for these experiments is listed
 146 in Table 2.

147
 148

149 **Table 2.** Characteristic of industrial (iron and steel factory) wastewater.

Industrial parameters	wastewater	Units	results
pH		--	8
Color		Pt-Co	865.6
TSS		mg/L	110
COD		mg/L	840.24
Ammonia-nitrogen NH ₃ -N		mg/L	42.8
Manganese "Mn"		mg/L	6.27
Iron "Fe"		mg/L	5.30
Zinc "Zn"		mg/L	5.44
Aluminum "Al"		mg/L	0.38
Nickel "Ni"		mg/L	0.15

150 **2.4 Factorial design and optimization**

151 The Design Expert Software (version 6.0.7) was used for statistical trial design and data analysis
 152 based on CCD and response surface RSM. The RSM is a mathematical and statistical approach
 153 that is often used for experimental designs to discover the optimal process parameter levels
 154 (Ghafari, Aziz, & Bashir, 2010; Yi, Su, Qi, Su, & Wan, 2010), the following equation (2) describes
 155 the correlation and interaction between the input parameters process and their response.

156
$$Y = f(X_1, X_2, X_3, \dots, X_k) \pm \varepsilon \quad (2)$$

157 Where $x_1, x_2, x_3, \dots, x_k$ are the input variables that might influence the result and \mathcal{E} is the
 158 random error.

159 Depending on the number of design parameters, the Design Expert program presented
 160 numerous designs. The Design Expert Software showed a variety of designs based on several
 161 design factors. The designs' ability to estimate higher-order words differs. The majority of designs
 162 are only appropriate for the quadratic model. The equation represents the second-order model (3).

$$Y = \beta_0 + \sum_{j=1}^k \beta_j X_j + \sum_{j=1}^k \beta_{jj} X_j^2 + \sum_{i < j=2}^k \sum_{i=1}^k \beta_{ij} X_i X_j + e_i \quad (3)$$

where Y represents the response, X_i and X_j represent the variables, the regression coefficient, k is the number of components evaluated and optimized in the experiment, and e represents the random error.

For graphical analyses of the data to determine the interaction between the process factors and the responses, analysis of variance (ANOVA) was performed to optimize the three treatment techniques. The coefficient of determination (R^2) value was used to describe the quality of the fit polynomial model, and its statistical significance was validated using the F-test in the same application. The P-value (probability) with a 95% confidence level was used to evaluate model terms.

CCD and RSM were used in this section to optimize and assess the relationship between the two independent factors: (1) dosage of a date stone, (2) and pH, as shown in Table 3.

Table 3. Independent variables of the CCD design.

Level of Value	A:Date stone (g)	B: pH
-1	0.6	7.5
0	1	5.38
+1	1.4	9

Chemical oxygen demand (COD), ammonia-nitrogen ($\text{NH}_3\text{-N}$), manganese (Mn), iron (Fe), Copper (Cu), aluminum (Al), and nickel (Ni) removal efficiencies of effluent wastewater were examined and regarded as dependent variables (response). The process's performance was assessed by measuring the removal efficiencies for the parameters mentioned above. Each independent variable was adjusted across three levels between -1 and +1 at the given ranges (Tizaoui, Bouselmi, Mansouri, & Ghrabi, 2007). The total number of experiments achieved for the two factors was 13 ($=2k+2k^5$), where k is the number of factors ($k=2$). **Table 4** shows the specifics of the coagulation exponential design matrix.

184 **Table 4. Summary for the experimental matrix of the amount of date stone powder and**
 185 **pH number for each experiment.**

Run	Type	Factor 1(date stone dosage)/ 200 mL	Factor 2 (PH)
SD1	Center	1.00 g	7.50
SD2	Axial	1.57 g	7.50
SD3	fact	0.60 g	9.00
SD4	Axial	1.00 g	5.38
SD5	Axial	1.00 g	9.62
SD6	Center	1.00 g	7.50
SD7	fact	1.40 g	9.00
SD8	Axial	0.43 g	7.50
SD9	Fact	1.40 g	6.00
SD10	Fact	0.60 g	6.00

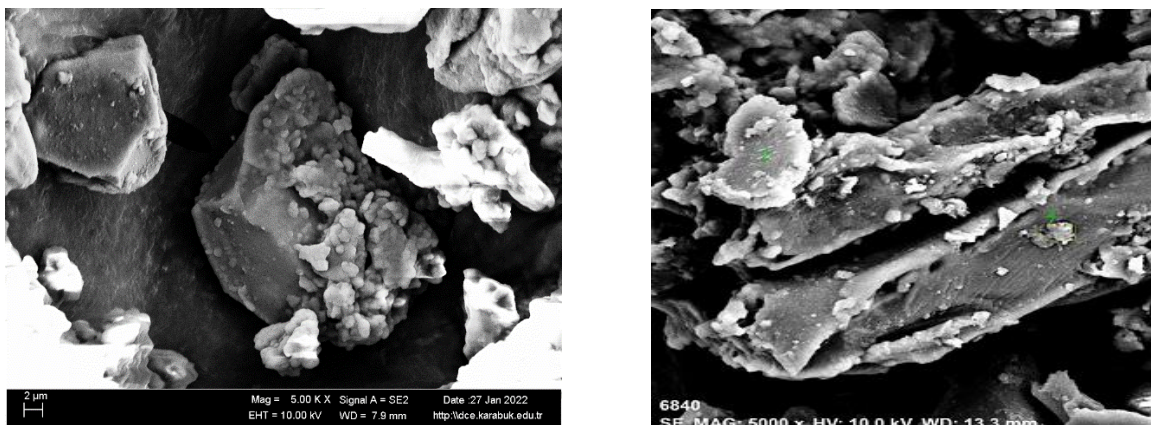
186 **3. Results and Discussion**

187 **3.1 Characterization of Date Stone Powder Imaging using Scanning Electron Microscopy**
 188 **(SEM)**

189 The morphological surface structure of date stone powder was studied before and after the
 190 coagulation procedure. Date stone powder has a condensed crystalline brick-shaped structure, as
 191 shown in Figure 2 (a). The structure functioned as an attachment point for suspended particles and
 192 cations (Salehizadeh & Shojaosadati, 2001). Figure 2 (b) shows how the coagulant aggregated the
 193 particles, resulting in the creation of bigger flocs that sank readily. As a result, SEM pictures of
 194 date stone powder revealed that bridging may be to blame for date stone powder's outstanding
 195 coagulation capabilities (He, Li, Chen, & Lun, 2002; Salehizadeh & Shojaosadati, 2001).

196 a)

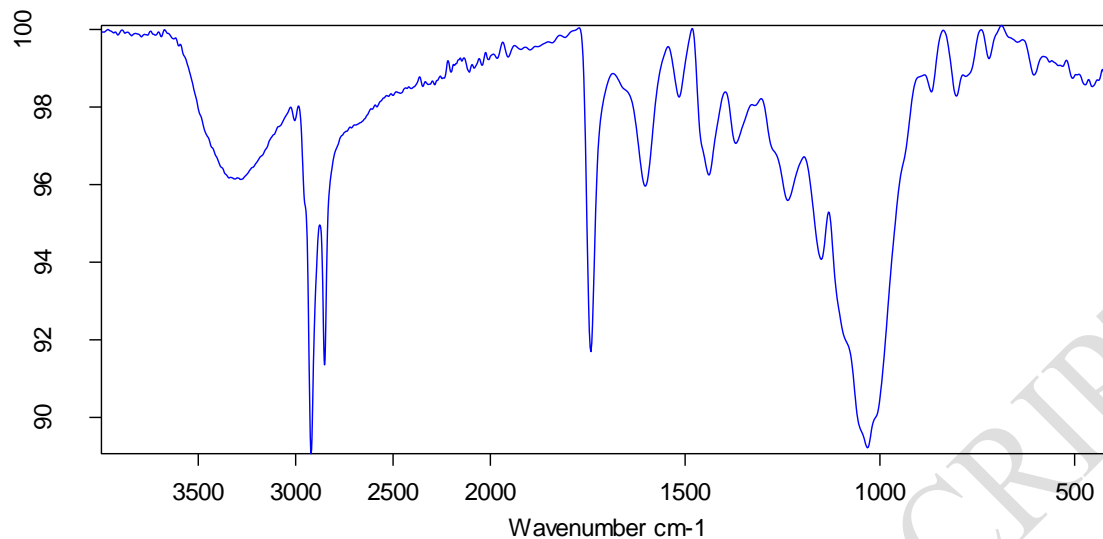
b)



197 **Figure 2.** Scanning electron microscopy image (2 μm) of date stone powder (a) before (b) after
198 the coagulation procedure.

199 3.2 Fourier Transformed Infrared (FTIR) Analysis

200 The corresponding Infrared (IR) spectrum using Fourier Transform Infrared (FTIR) Spectroscopy
201 was generated to investigate further the existence of the powdered date stone's main possible
202 functional groups. As shown in Figure 3, FTIR analysis was adequately done to simplify and
203 highlight its main functional groups. To ease the analysis of the IR spectrum obtained for date
204 stone powder, the bands' range- where its functional groups could possibly highlight within the
205 range of wavelength peaks. The observed peaks in the $300\text{-}2500\text{ cm}^{-1}$ range might indicate the
206 existence of solid amine salts (N-H) that are involved in the bridging mechanism used by particles
207 during the coagulation-flocculation and may contribute to the increase of ammonia and organic
208 removal from wastewater. The peak between $1750\text{-}1650\text{ cm}^{-1}$ shows the C-N link, whereas the
209 ones from $(1650\text{-}1550)\text{ cm}^{-1}$ either confirm a primary amine N-H or the aromatic C=C. The peak
210 between a green region of $1300\text{-}1250)\text{ cm}^{-1}$ 1 indicates an aromatic ester C-O bond, while the one
211 between $1200\text{-}1000\text{ cm}^{-1}$ shows the N-H aliphatic amine.



212

213 **Figure 3.** Fourier transformed infrared (FTIR) spectroscopy curve for date stone powder.

214 **Table 5.** Summary of an experimental matrix for coagulation of wastewater using date stone
 215 powder.

Run	Type	Factors		Responses						
		A: Date stone dosage (g)	B: pH	COD Removal %	NH ₃ -N Removal %	Fe Removal %	Mn Removal %	Ai Removal %	Cu Removal %	Ni Removal %
1	Center	5.00	7.50	35.8	28.0	92.0	92.5	92.8	63.2	90.7
2	Axial	7.85	7.50	6.4	64.0	95.9	92.3	87.1	63.2	88.0
3	Fact	3.00	9.00	65.3	65.7	96.7	93.8	93.7	47.4	87.0
4	Axial	5.00	5.38	44.2	58.2	94.3	83.4	74.8	34.2	81.0
5	Axial	5.00	9.62	41.2	24.3	94.0	94.7	93.9	60.5	86.0
6	Center	5.00	7.50	41.2	34.1	92.0	91.7	82.5	60.5	90.0
7	Fact	7.00	9.00	9.1	64.7	96.0	88.9	78.3	60.5	80.7
8	Center	5.00	7.50	35.8	28.0	92.0	92.5	92.8	63.2	90.7
9	Center	5.00	7.50	35.8	28.0	92.0	92.5	92.8	63.2	90.7

10	Axial	2.15	7.50	67.9	93.0	90.0	90.2	89.1	42.1	89.3
11	Fact	7.00	6.00	14.5	97.7	96.7	87.9	91.3	65.8	85.0
12	Fact	3.00	6.00	70.6	77.8	89.0	82.6	70.7	31.6	83.0
13	Center	5.00	7.50	35.8	28.0	92.0	92.5	92.8	63.2	90.7

216 The process of adding date stone powder to the wastewater solution was carried out in
217 different quantities with a change in the experimental conditions, and the results of the removal
218 efficiencies ranged between 6.4% and 70.6% for **COD**, 24.3% to 97.7% for **NH₃-N**, 89.0 % to
219 96.7% for **Fe**, 82.6% to 94.7% for **Mn**, 70.7% to 93.9% for **Al**, ranges from 31.6% to 65.8%, for
220 **Cu**, and 80.7% to 90.7%, for **Ni**. The results indicate that the efficiency of date stone powder in
221 the processing process is extensive in removing **Fe** and **NH₃-N**, while the treatment rate was weak
222 in **Al** and **Cu**; this is due to the cohesion of the molecules of these elements with each other, which
223 gave a lower treatment efficiency. As shown in Table 5.

224 3.3 Analysis of variance

225 Table 6 depicts the modules' analysis of variance and the statistical relationship between the
226 variables and responses. The findings in the table below reveal that all simulations were weighty
227 at the 5% confidence level based on the value of **P. (Prob)**. The values of the R² for COD, NH₃-
228 N, Fe, Mn, Al, CU and Ni, were: 0.9790, 0.8764, 0.8784, 0.9412, 0.9216, 0.8105 and 0.8956,
229 respectively, which is more than 0.80 in order to fit the model well, and R² value close to 1
230 indicates a worthy acceptance between the expected and calculated outcomes results.

231

232

233 **Table 6.** Analysis of Variance (ANOVA) for parameters removal.

COD removal %	Source	Sum of Squares	DF	Mean Square	F Value	Prob > F	
	Model	5046.96	5	1009.39	65.31	< 0.0001	significant
A	4961.86	1	4961.86	321.03	< 0.0001		
B	27.68	1	27.68	1.79	0.2227		
A2	0.088	1	0.088	5.724E-003	0.9418		

	B2	56.94	1	56.94	3.68	0.0964	
	AB	0.000	1	0.000	0.000	1.0000	
	Residual	108.19	7	15.46			
	Lack of Fit	85.36	3	28.45	4.99	0.0774	not significant
	Pure Error	22.83	4	5.71			
	Cor Total	5155.15	12				
	Std. Dev. 3.93	R ² : 0.9790, Mean:38.75					
NH ₃ -N Removal %		Sum of		Mean	F		
	Source	Squares	DF	Square	Value	Prob > F	
	Model	7298.16	5	1459.63	9.93	0.0044	significant
	A	60.76	1	60.76	0.41	0.5408	
	B	1081.24	1	1081.24	7.35	0.0301	
	A2	5759.35	1	5759.35	39.17	0.0004	
	B2	715.29	1	715.29	4.86	0.0632	
	AB	108.10	1	108.10	0.74	0.4196	
	Residual	1029.36	7	147.05			
	Lack of Fit	999.84	3	333.28	45.16	0.0015	significant
	Pure Error	29.52	4	7.38			
	Cor Total	8327.52	12				
	Std. Dev. 12.13,	R ² : 0.8764, Mean: 53.20					
Fe removal %		Sum of		Mean	F		
	Source	Squares	DF	Square	Value	Prob > F	
	Model	66.30	5	13.26	10.11	0.0042	significant
	A	29.18	1	29.18	22.25	0.0022	
	B	5.50	1	5.50	4.20	0.0797	
	A2	3.66	1	3.66	2.79	0.1388	
	B2	12.24	1	12.24	9.33	0.0184	
	AB	17.23	1	17.23	13.14	0.0085	
	Residual	9.18	7	1.31			
	Lack of Fit	9.18	3	3.06			
	Pure Error	0.000	4	0.000			
	Cor Total	75.48	12				
	Std. Dev. 1.15	R ² :0.8784, Mean:93.26					
Mn removal		Sum of		Mean	F		
	Source	Squares	DF	Square	Value	Prob > F	
	Model	159.82	5	31.96	22.43	0.0004	significant

A	1.37	1	1.37	0.96	0.3593	
B	98.60	1	98.60	69.18	< 0.0001	
A2	6.92	1	6.92	4.86	0.0634	
B2	30.17	1	30.17	21.17	0.0025	
AB	25.95	1	25.95	18.21	0.0037	
Residual	9.98	7	1.43			
Lack of Fit	9.52	3	3.17	27.86	0.0039	significant
Pure Error	0.46	4	0.11			
Cor Total	169.80	12				
Std. Dev.	1.19					R ² : 0.9412, Mean: 90.41

Al removal %

Source	Sum of Squares	DF	Mean Square	F Value	Prob > F	
Model	616.14	5	123.23	5.99	0.0181	significant
A	0.65	1	0.65	0.032	0.8636	
B	170.78	1	170.78	8.30	0.0236	
A2	27.61	1	27.61	1.34	0.2848	
B2	104.53	1	104.53	5.08	0.0589	
AB	324.53	1	324.53	15.77	0.0054	
Residual	144.09	7	20.58			
Lack of Fit	59.31	3	19.77	0.93	0.5028	not significant
Pure Error	84.78	4	21.19			
Cor Total	760.22	12				
Std. Dev.	4.54,					R ² : 0.8105, Mean 87.16

Cu removal %

Source	Sum of Squares	DF	Mean Square	F Value	Prob > F	
Model	1608.41	5	321.68	16.47	0.0010	significant
A	743.85	1	743.85	38.08	0.0005	
B	284.92	1	284.92	14.58	0.0066	
A2	151.78	1	151.78	7.77	0.0270	
B2	370.98	1	370.98	18.99	0.0033	
AB	110.80	1	110.80	5.67	0.0488	
Residual	136.75	7	19.54			
Lack of Fit	131.21	3	43.74	31.58	0.0030	significant
Pure Error	5.54	4	1.39			
Cor Total	1745.15	12				
Std. Dev.	4.42					R ² : 0.9216, Mean 55.26

N i

Sum of Mean F

Source	Squares	DF	Square	Value	Prob > F	
Model	148.77	5	29.75	12.01	0.0025	significant
A	4.83	1	4.83	1.95	0.2052	
B	5.67	1	5.67	2.29	0.1740	
A2	15.13	1	15.13	6.11	0.0427	
B2	114.57	1	114.57	46.24	0.0003	
AB	17.36	1	17.36	7.01	0.0331	
Residual	17.35	7	2.48			
Lack of Fit	16.99	3	5.66	63.72	0.0008	significant
Pure Error	0.36	4	0.089			
Cor Total	166.12	12				
Std. Dev. 1.57	R ² : 0.8956, Mean87.13					

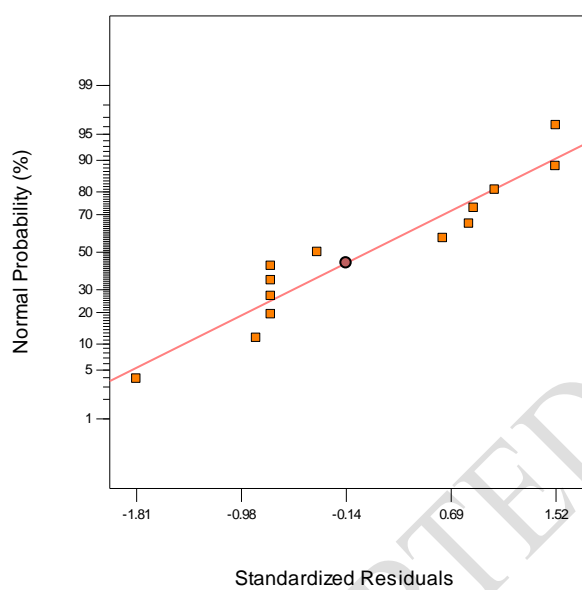
234 3.4 Treatment Effectiveness

235 The selected model is equivalent to the existing system using Design Expert 6.0.7 software by
 236 delivering typical protection graphs for diagnostics and standardized residuals. Probability graphs
 237 produced by Design Expert 6.0.7 software were used to evaluate the models. The standardized
 238 residuals probability plots for COD, NH₃-N, Fe, Mn, Al, Cu, and Ni are shown in Figure 4 (a-g).
 239 As a result, it may be stated that the reactions of some models to data are regularly distributed.

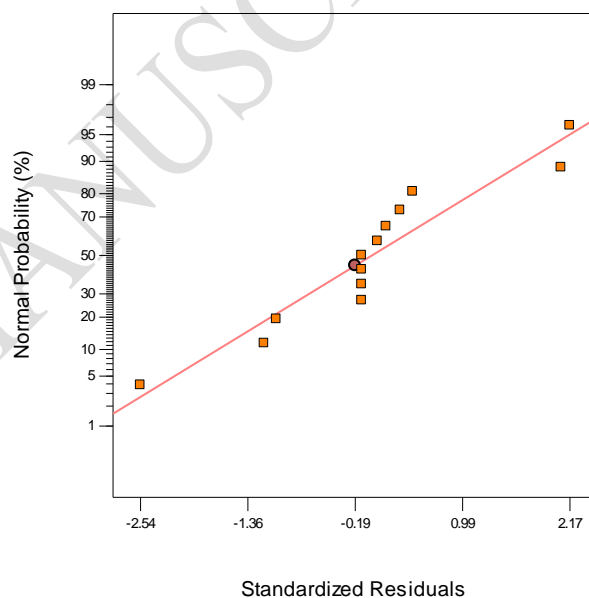
240 The Design Expert 6.0.7 program was used to investigate the interaction linkages between
 241 independent factors and the responses of specific models using 3D surface response and contour
 242 plots, as illustrated in **Error! Reference source not found.** (a-g). The largest percent of NH₃-N
 243 and COD removal is 82.2% and 66.5 %; respectively, when the dose of ground date stones is 1.4
 244 g, and the level is 9.0 as well as for Fe, Mn, Ai, Cu, and Ni, the removal percentage is 97.2% and
 245 94 .9%, 98.24%, 67.6%, and 90.8%, respectively. These response charts indicate that the amount
 246 of treatment needed is determined by the ratios of these elements in the wastewater and the
 247 experimental settings (pH level). The effectiveness of date stone powder's coagulation in removing
 248 COD and NH₃-N varied. Determining the ideal coagulant dose is crucial to ensure that the
 249 treatment process runs at its best while lowering material costs and sludge formation. The ability
 250 of date stone powder's natural polyphenols to adsorb metal ions and organic impurities improved
 251 the elimination of organic pollutants (Palma, Freer, & Baeza, 2003). The action of electric double
 252 layers produced by carboxylic, phenolic, and amino groups may be responsible for the

253 improvement in organic and ammonia elimination (Schofield, Mbugua, & Pell, 2001). The
254 efficiency of the targeted parameters' elimination decreased when date stone doses more than 7 g
255 were utilized. The wastewater's colloids and particles were better able to bridge one another thanks
256 to date stone's positively charged primary amino groups, which also enhanced the flocculation
257 process (Mangrich, Doumer, Mallmann, & Wolf, 2014). High molecular weight date stone
258 powder is not hydrolyzed in wastewater. A larger dose of date stone causes a significant volume
259 of powder to precipitate quickly, which may lessen the efficiency of flocculation (Kim, Silva, Kim,
260 & Jung, 2010).

A)

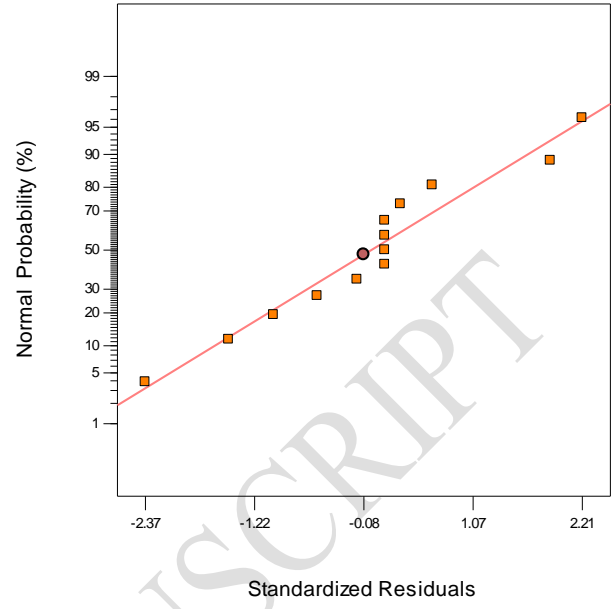
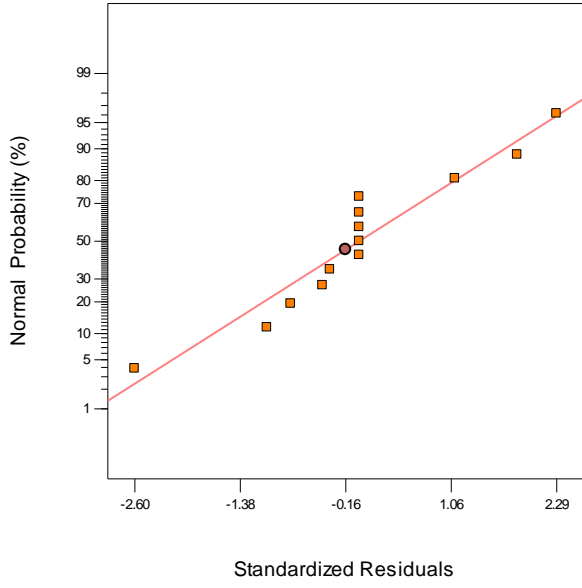


b)

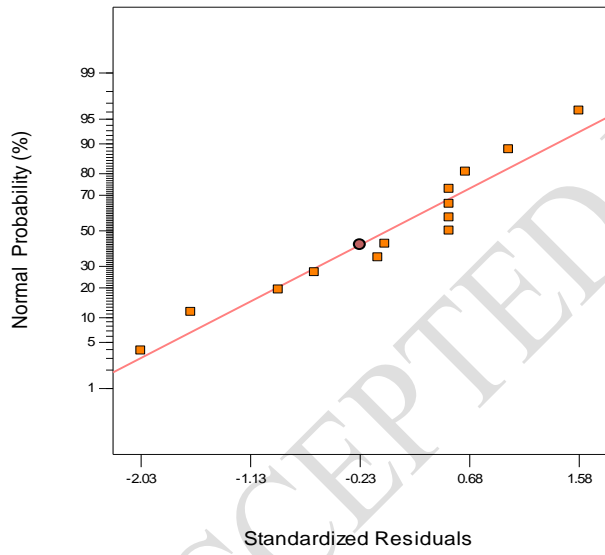


c)

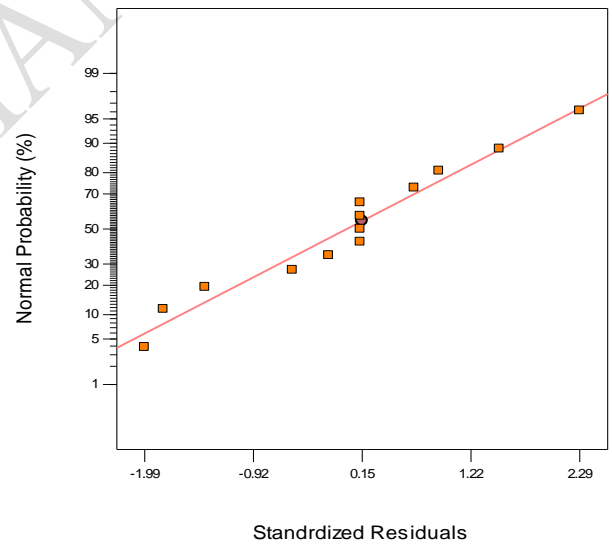
d)



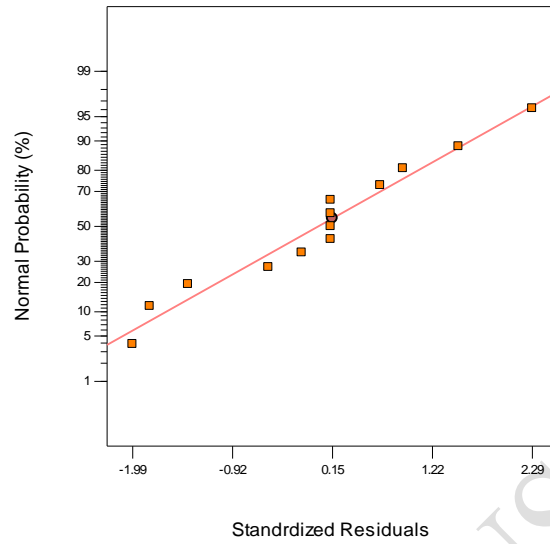
e)



f)



g)



261 **Figure 4.** Normal probability plots for a (COD), b (NH₃-N), c(Fe),d (Mn), e (Ai), f(Cu) and g(Ni)
262 removals.

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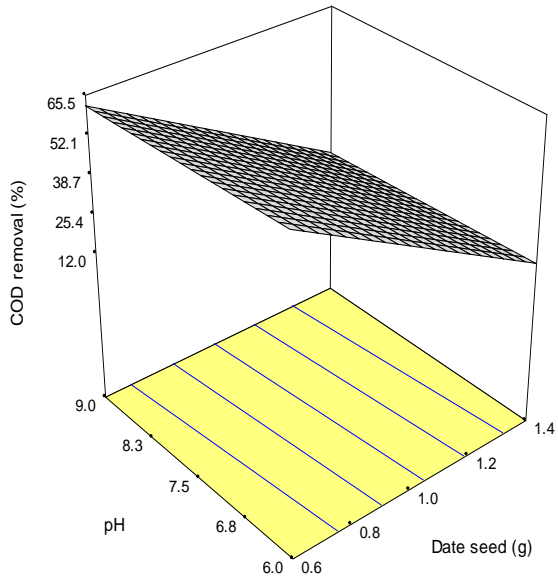
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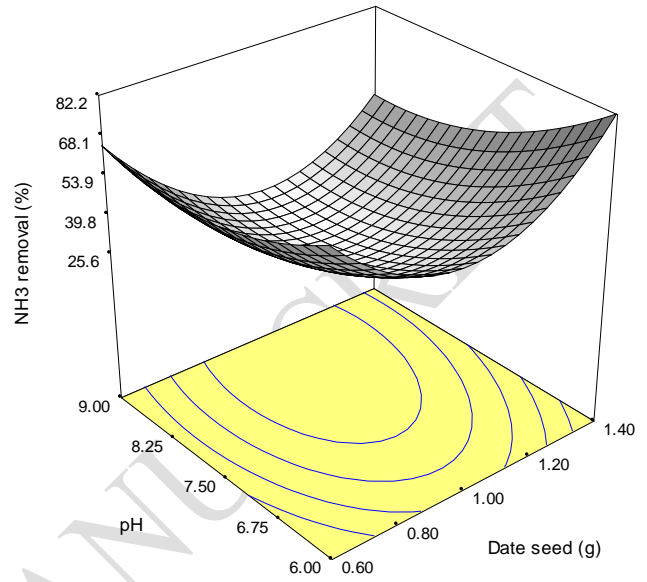
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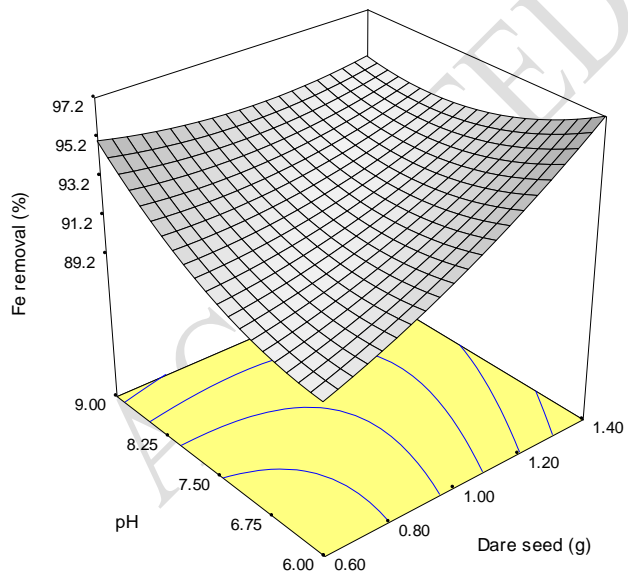
a)



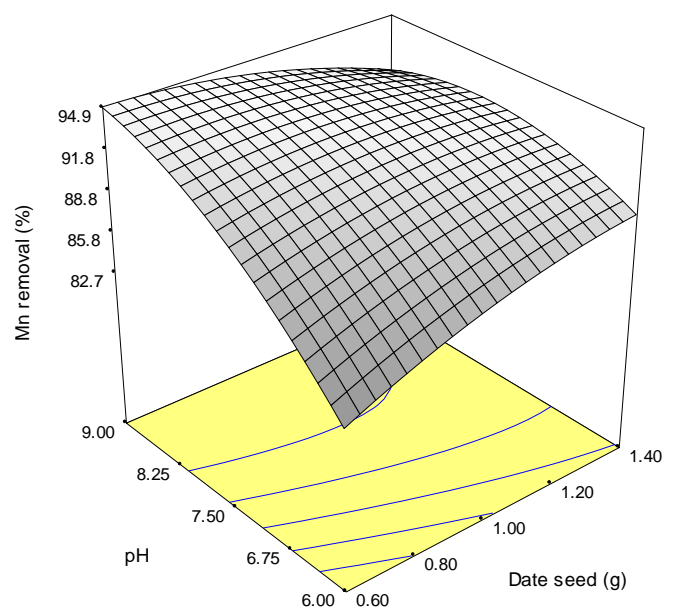
b)



c)

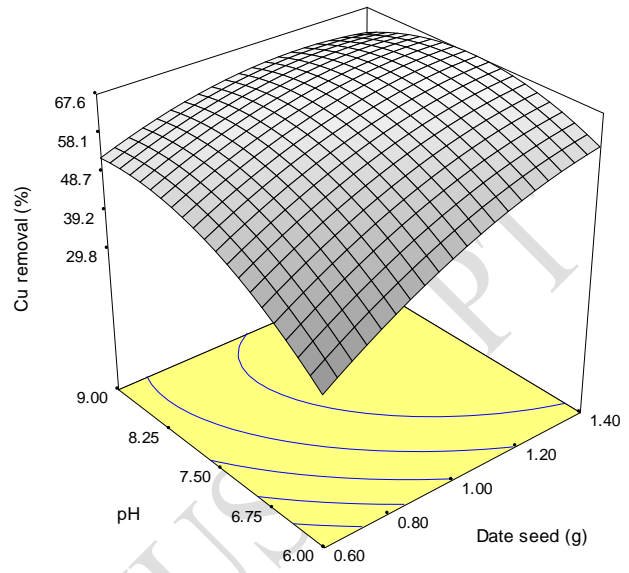
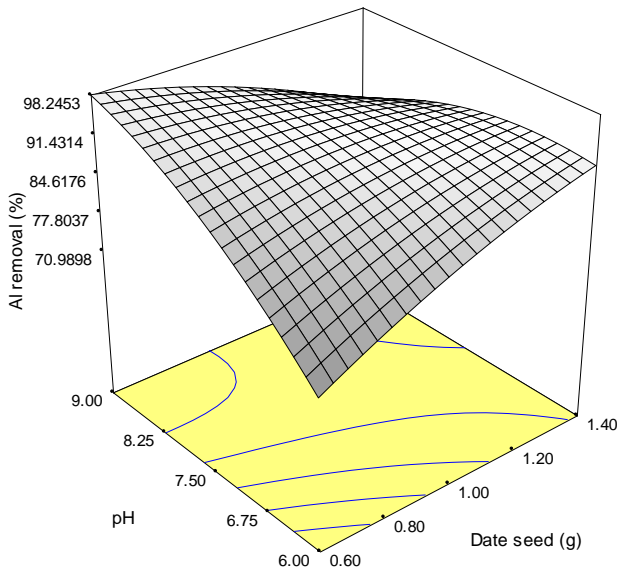


d)

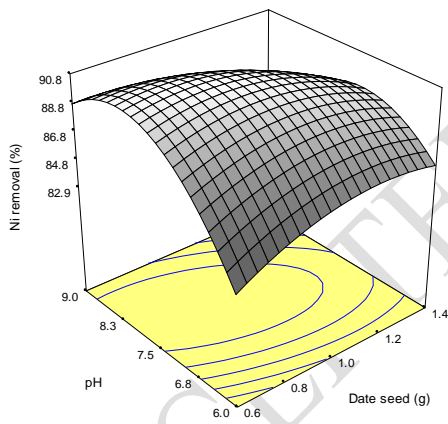


e)

f)



gg)



279 3.5 Optimization Operational Conditions

Figure 5. Response surface Plots for a(COD), b(NH₃-N), c(Fe), d(Mn),e (Ai), f(Cu) and g(Ni) removals.

280 Work was done to determine the optimal value for treating the presence of COD and NH₃-N, Fe,
 281 Mn, Ai, Cu, Ni in wastewater using the Design Expert 6.0.7 program. Accordingly, the
 282 experimental conditions were determined for each case (pH concentration and dose of crushed
 283 date stones), and the answers were determined as the best limits in achieving the highest treatment
 284 value. The software combines individual desirability into a single value, which it then strives to

285 optimize based on the response objective. As a consequence, the ideal operating conditions and
286 efficiency removals were identified, as indicated in Table 6.

287 Table 7 shows, it is expected to remove 61%, 65%, 95%, 94%, 98%, 52%, 88% of COD
288 and NH₃-N, Fe, Mn, Al, Cu, Ni, respectively. Based on optimized operating conditions (date stone
289 0.6g, pH 9). an experiment was conducted in the laboratory to ensure the correctness of the optimal
290 results. Moreover, it was found that the experiment's results correspond to the value of the expected
291 response.

292 **Table 7.** Optimal response results from model prediction and laboratory.

	Date stone (g)	pH	COD removal (%)	NH ₃ -N removal	Fe removal (%)	Mn removal (%)	Al removal (%)	Cu removal (%)	Ni removal (%)	Desirability
Prediced	0.6	9	61.8	65	95	94	98	52	88	0.923
Lab. Experiment			61	63	93	93	96.5	51	86	

293 4. Conclusion

294 In this study, the percentage of COD, NH₃-N, Fe, Mn, Al, Cu and Ni removal by date stone powder
295 showed significant promise as a plant-based natural coagulant in iron and steel factory treatment.
296 The experiment proved the date stone's significant coagulation characteristics. The following are
297 the particular findings of the studies. The FTIR analysis verified the presence of several functional
298 groups that are involved in the coagulation process. At 1.4 g/200 mL, the date stone powder
299 removed a high percentage of COD, NH₃-N, Fe, Mn, Al, Cu and Ni from effluent at pH 8, with
300 percentages 61, 63, 93, 93, 96.5, 51 and 86 %, respectively.

301 Due to the organic structure of date stones powder, the pH of industrial effluent remained
302 unchanged after its addition. Consequently, no pH adjustment was necessary throughout the
303 treatment process when date stone powder was used as a coagulant.

304

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313 **Declaration of interests**

314

315 The authors declare that they have no known competing financial interests or personal
316 relationships that could have appeared to influence the work reported in this paper.

317

318 The authors declare the following financial interests/personal relationships which may be considered
319 as potential competing interests:

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