

Removal of methylene blue using activated carbon prepared from date stones activated with NaOH

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Abstract

Synthetic dyes have a hurtful effect on human health and the environment. In this work, activated carbon was produced from date stones for use in elimination of methylene blue charged in aqueous solutions. Before that, the adsorbent was characterized by BET method, SEM, X-ray and TGA. The results of the adsorption kinetics are describe better with the pseudo-second order model ($R^2 = 0.998$). Frenlich adsorption isotherm model describe better the experimental data than the Langmuir model. The capacity for methylene blue removal was found to be 163.67 mg/g. Batch experiments studies show that the activated carbon produced as of date stones can be used effectively in the treatment of cationic dyes in aqueous solutions.

Keywords: Adsorption, kinetic, isotherm, activated carbon, methylene blue.

1. Introduction

The existence of organic micro pollutants and inorganic substances in the waters has much interesting attention of the international scientific community, favoring new research, oriented to class and to measure the toxicological potentialities of an extremely great number of organic chemicals and inorganic substances. Industrial discharges are the main sources of water contamination, may cause serious environmental consequences for ecosystems to all taxonomic groups (algae, bacteria, fish, birds, mammals) (Couture *et al.*, 1989; Gupta and Saini, 2005; Ian *et al.*, 2006; Saha *et al.*, 2012; Schreurs *et al.*, 2004).

Synthetic dyes are used in many industrial sectors such as dyeing of textile, paper, leather, food, cosmetics industries and pharmaceutical products (Bartonova *et al.*, 2017; Robinson *et al.*, 2001; Umpuch and Sakaew, 2013; Yagub *et al.*, 2015). Textile industries cause pollution of water which are harmful to the environment, such as certain carcinogenic azo dyes,

they require physicochemical techniques to degrade them (Aksu *et al.*, 2005).

A various techniques (Physico-chemical and biological) have been developed and tested for water filled with dyes. These techniques include adsorption (Hamdaoui *et al.*, 2006), coagulation-flocculation (Verma *et al.*, 2012), ion exchange (Karcher *et al.*, 2002), membrane filtration (Avlonitis *et al.*, 2008), Fenton reagent (El Haddad *et al.*, 2014), photo-catalysis of hydrogen peroxide (Aleboye and Aleboye, 2015), peroxonation (Pekey, 2016), photolysis of hydrogen peroxide and ozonation (Alaton *et al.*, 2002); biological treatment (Chellaiah *et al.*, 2018).

Activated carbon is widely used for the treatment of wastewater due to its internal surface which makes them ideal for the removal of soluble substances from water (Iqbal and Ashiq, 2007).

The agricultural solid waste as an abundant and cheap material widely used as raw adsorbent or converted into activated carbon by a physical activation process such as pistachio shells (Attia *et al.*, 2003), almond shells (Maaloul *et al.*, 2017), rattan sawdust (Hameed *et al.*, 2007), cotton stalk (Deng *et al.*, 2009), orange peel (Foo and Hameed, 2012), hazelnut shell (Şayan, 2006), oil-palm shell (Lua and Jia, 2009), coffee residue (Boonamnuayvitaya *et al.*, 2004), mangosteen peel (Ahmad and Alrozi, 2010), eucalyptus wood (Mane and Babu, 2011), powdered peanut hull (Gong *et al.*, 2005), bagasse (Valix *et al.*, 2004), sunflower stalks (Şaibani *et al.*, 2008), Sugarcane (Ibrahim *et al.*, 2006), mango seed kernel (Vasanth and Kumaran, 2005), coconut coir dust (Macedo *et al.*, 2006), groundnut shells (Kannan and Sundaram, 2001), oil-palm (Cheng *et al.*, 2017), Apricot stones (Kobyas *et al.*, 2005), banana pith (Kadirvelu *et al.*, 2003), coir pith (Kavitha and Namasivayam, 2007), Peach stones (Amina *et al.*, 2008). Glucose, cellulose and hazelnut shells (Çaglar *et al.*, 2018).

Algeria is one of leading producers of dates with about 14% of world production, according to the statistics of FAO (2013), Algeria ranks the 4th in terms of date production, after Saudi Arabia, Egypt and Iran.

Deglet Nour, Ghars and Degla Beida are the main varieties of dates produced in Algeria. The agri-food industries generate an important amount of date stones that are usually considered as waste. This work aims to produce activated carbon as of date stones as a waste agriculture for use in the removal of dye from water, particularly for the removal of textile industry effluents.

2. Materials and methods

2.1. Preparation of adsorbent

Deglat Beida stones as an agricultural solid waste were obtained from Biskra, Algeria, the sample was washed repeatedly with tap water to remove soluble impurities, dried under a period of 24 hours at 60 °C, followed by mechanical grind to obtain a fine particles of diverse sizes. The particles was washed in distilled water to eliminate soluble organic matter and floating matter in the water, filtered using a Wattman membrane N°4 then dried at 60 °C, impregnated in solution of NaOH its concentration 0.5 M for 4 h. The sample was then washed in distilled water until the sample was neutralized, filtrated and dried in the oven at 60 °C for 24 h. The sample was heated in an electric oven with heating ramps 5 °C per min until 600 °C was maintained for one hour. The activated carbon (CNDB) obtained by this treatment were washed with distilled water, filtered and dried at 100 °C for 2 hours and then sieved using a sieve RETCH Model AS 200 to obtain a particle size between 315–500 µm.

2.2. Preparation of MB solution

A stock solution containing 500 mg/L of MB was prepared by dissolving required mass of methylene blue ($C_{16}H_{18}N_3S$, 98.5% purity, Fluka) in the distilled water. Adsorption tests solutions were used by dilution stock solution. pH of the solutions was adjusted by 0.1 M hydrochloric acid 37% purity, Chemistry-Plus or by addition of a 0.1 M solution of sodium hydroxide 98% purity, Fluka Chemika.

2.3. Characterization of the activated carbon

Nitrogen adsorption measurements were performed using QuadraSorb SI MP Station at 77 K to determine the Surface area of ACDB. A MEB FEG JEOL 6700F scanning electron microscope (SEM) was used to observe the surface morphologies of ACDB. Philips X' Pert X-ray diffraction was used to identify the nature of the crystalline and amorphous phases present in ACDB. Thermo gravimetric analysis (TGA) of NDB sample was carried out by TGA/SDTA 851^e Mettler-Toledo. Thermal analyzer, on weight of 7.6416 mg at a heating range from 25 to 950 °C under 10 °C/min and 40 ml/min, heating rate and an air flow rate respectively.

2.4. Batch adsorption studies

Adsorption tests of the cationic dye methylene blue MB solution on activated carbon ACDB were carried out in batch system by mixing 0.08 g of ACDB with 50 ml containing 500 mg/L of MB. For the measurement of pH solution a Hanna pH-meter model: 211, the solution was used and adjusted by 0.1 M of sodium hydroxide or

hydrochloric acid. The contact time parameter effect was studied at different time interval from 5 to 360 min at pH value of 6 and 25 °C and initial concentration of 500 mg/L of MB. The pH parameter effect on the quantity of cationic dye MB adsorbed was studied in range 2 to 10 at 25 °C. The effect of adsorbent dose on the adsorption of MB was studied for different masses from 0.01 to 0.1 g at pH 6 and a temperature of 25 °C. Adsorption isotherm experiments were performed into different initial concentrations of MB between 50 and 500 mg/L at pH 6 and 25 °C, were shaken for 24 h to reach equilibrium.

The concentration of MB in the solution was determined by UV-Visible Optizen 1412V Spectrophotometer at wave length of 664 nm.

The quantity of cationic dye MB adsorbed at equilibrium concentration was calculated by the following expression (Rong and Qi, 2010):

$$q_e = \frac{(C_0 - C_e)}{m} \times V \quad (1)$$

Where C_e and C_0 (mg/L) are the residual concentration of MB at equilibrium and the primarily concentration of adsorbate MB, respectively. V (L) is the solution volume, and m (g) is the mass of ACDB used.

3. Results and discussion

3.1. Characterization of adsorbent

From the Figure 1, the SEM observation shows the presence of very remarkable cavities due to the chemical treatment with NaOH and the pyrolysis at 600 °C which improves the porosity of the adsorbent (formed cavities) of ACDB. Figure 2, shows the N_2 adsorption-desorption isotherm of activated carbon ACDB, the plot demonstrates a typical isotherm type I (Storck *et al.*, 1998; Chen and Zeng, 2003) reveal microporous adsorbent according to the classification of IUPAC. The specific surface area of ACDB was found to be $S_{BET} = 248.38 \text{ m}^2/\text{g}$ measured by the method of BET at (p/p_0) range [0.05-0.3].

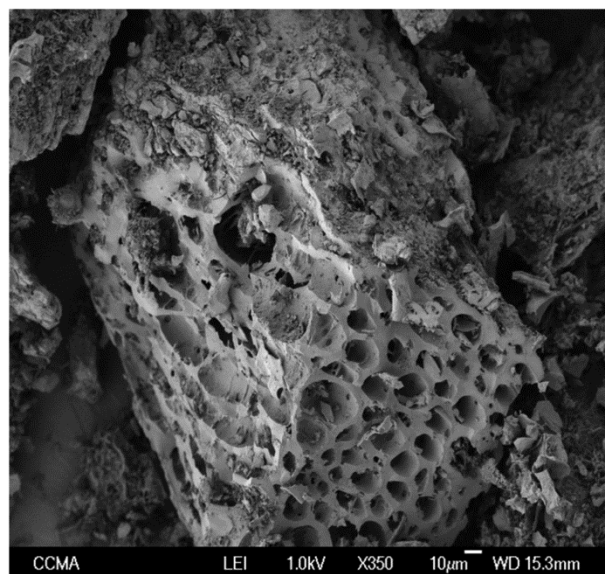


Figure 1. SEM image of ACDB

The X-ray diffraction results of the samples treated with sodium hydroxide and activated carbon before and after the adsorption of methylene blue NDB, NDB-MB, ACDB and ACDB-MB respectively, are shown in Figure 3, the diffraction spectrum of NDB and NDB-MB show the same spectrum and exhibit the same diffraction peaks at $2\theta = 16.7$ and $2\theta = 21$ which are attributed respectively to the cellulose (Hui *et al.*, 2015), peak intensity of the two diffraction peaks have no change after MB adsorption, which indicates that the adsorption is produced in the amorphous region, the disappearance of these peaks for the activated carbon before and after the adsorption of methylene blue ACDB and ACDB-MB respectively, was attributed to the degradation of cellulose, the spectrum before or after the adsorption on activated carbon has no change, which also reveals that the adsorption is produced in the amorphous region. Thermogravimetric analysis for the raw adsorbent treated with sodium hydroxide (NDB) is presented in Figure 4. The TGA/DTG curves show that CNDB thermal decomposition has three stages. Dehydration which ended at 150 °C, with a maximum mass loss of 5.9 (%). Then, the combustion of volatile matter and combustion phase until the peak temperature of 382 °C, with a very brutal mass loss of 58.57(%), followed by, the last stage corresponds to the combustion of char until 550 °C, with a mass loss of 27.48 (%) (Ge *et al.*, 2015; Munir *et al.*, 2009).

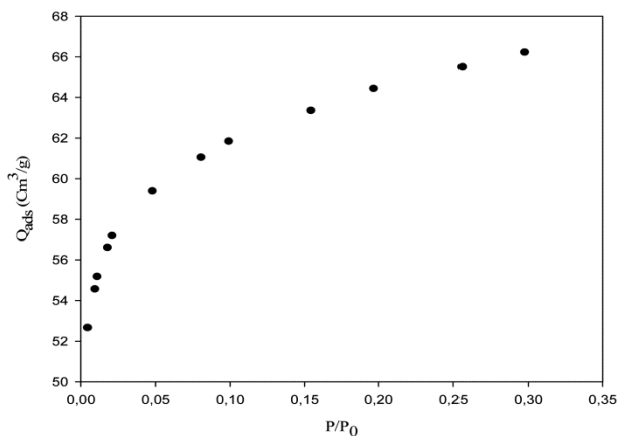


Figure 2. N₂ adsorption-desorption isotherms of ACDB at 77 K

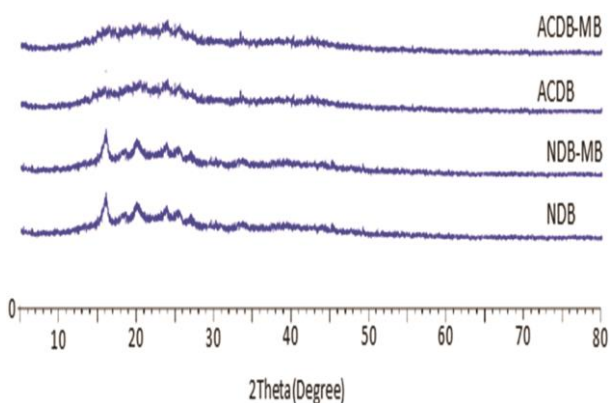


Figure 3. X-ray diffraction of ACDB

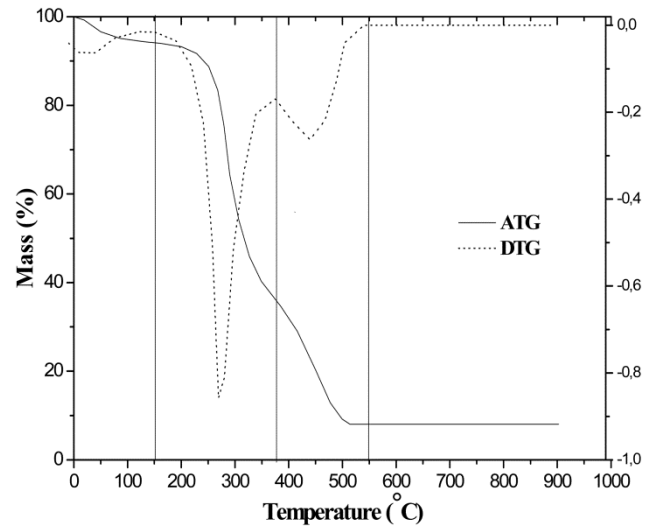


Figure 4. TGA/DTG curves of ACDB

3.2. Effect of pH on adsorption of MB

The initial pH value is a very important parameter to consider for controlling the adsorption removal process in aqueous solution, it can change, speciation of molecules surface, charge of the adsorbent and degree of ionization of the adsorbate (Aksu *et al.*, 2005; Miretzky and Munoz, 2011; Yao *et al.*, 2010). Figure 5, shows the effect of initial pH on the adsorption of methylene blue on ACDB. Increasing of initial pH values from 2 to 10 enhances the adsorption capacity of MB from 89.07 to 207.09 mg/g. At higher initial pH values, the surface of the adsorbent CNDB adopts the negatives charges sites which favorites the adsorption of MB cations by electrostatic attraction while at lower initial pH values the surface of the CADB adopts the positive charge which causes a decrease in MB adsorbed due to the electrostatic repulsion, similar results were obtained by other studies on MB adsorption by activated carbon (AL-Aoh *et al.*, 2013; Karagöz *et al.*, 2008; Postai *et al.*, 2016).

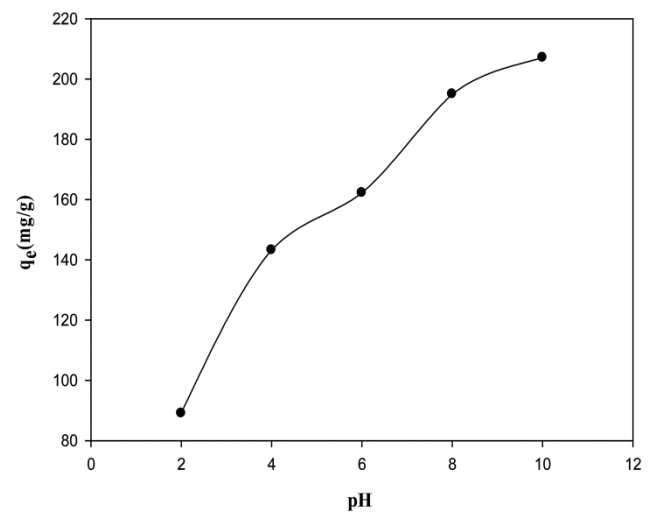


Figure 5. Effect of initial pH on the adsorption equilibrium of MB using ACDB

3.3. Effect of adsorbent dose

The effect of the adsorbent dose on the adsorption capacity and the adsorption efficiency of MB were studied on ACDB adsorbents. Figure 6, illustrates that the adsorption efficiency augmented with the increase of the adsorbent amount, while the amount adsorbed decreases with increasing mass. This may probably due to the augmented surface area and number of active sites available for the fixation of methylene blue. This is similar to the studies reported by (Jain *et al.*, 2015; Mehta *et al.*, 2016; Uddin *et al.*, 2009).

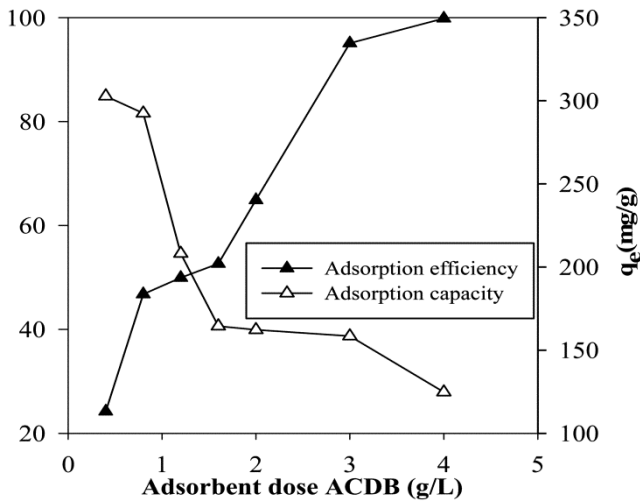


Figure 6. Effect of adsorbent dose on the adsorption of MB by ACDB

3.4. Adsorption kinetics

In order to determine the kinetic model for the removal of MB on ACDB, two models have been applied such as pseudo-first order model and pseudo-second order model, were represented respectively by the following equations (Uddin *et al.*, 2009; Sarici-Özdemir and Önal, 2014).

$$\ln(q_e - q_t) = \ln q_e - K_1 t \quad (2)$$

$$\frac{t}{q_t} = \frac{1}{K_2 q_e^2} + \frac{1}{q_e} t \quad (3)$$

Where, q_e and q_t (mg/g) are the quantity of MB adsorbed at equilibrium and adsorbed at instant t (min), respectively, k_1 (1/min) and k_2 (mg/g min) are the rate constants of both models.

Figure 7a and b show the comparison between the kinetic models, pseudo-first order model and pseudo-second order model for the adsorption of MB on the ACDB. The values of kinetic parameter of both kinetic models are included in the Table 1. The results appear that the model of pseudo-second order was the best for describing the kinetic of methylene blue compared to the other model pseudo-first order. The value of correlation coefficients R^2 was superior than 0.99 also the values of ($q_{e,cal}$) calculated from the model of pseudo-second order was approach to the experimental value (q_{exp}), indicating the applicability of this model to the adsorption of MB on ACDB.

Table 1. Kinetic parameters for MB (500 mg/L) adsorption on ACDB

q_{exp} (mg/g)	Pseudo-first order			Pseudo-second order		
	$q_{e,cal}$ (mg/g)	k_1 (1/min)	R^2	$q_{e,cal}$ (mg/g)	k_2 (mg/g min)	R^2
163.67	100.4	0.749	0.984	169.4	0.00047	0.998

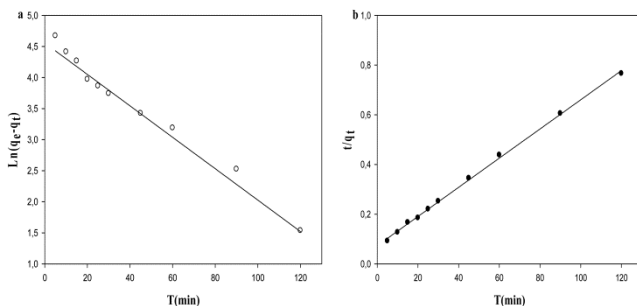


Figure 7. Pseudo-first order (a), pseudo-second order (b) for the adsorption of MB on ACDB

3.5. Adsorption isotherms

In order to comprehend the adsorption mechanism for different initial concentrations, and also to identify the isotherm represents the adsorption of MB on ACDB

(Figure 8). Two theoretical models were tested on the experimental results obtained by application of both Freundlich and Langmuir models. The isotherm equation linear form of models Freundlich and Langmuir are written respectively by the following equations (Yao *et al.*, 2010):

$$\ln q_e = \ln K_F + \frac{1}{n} \ln C_e \quad (4)$$

$$\frac{C_e}{q_e} = \frac{1}{q_m b} + \frac{1}{q_m} C_e \quad (5)$$

Where C_e represents the equilibrium concentration (mg/L), q_m is the maximum quantity of MB adsorbed (mg/g) and K_L is the thermodynamic constant of equilibrium (1/mg), K_F is the Freundlich constant (L/mg), and $(1/n)$ the heterogeneity factor.

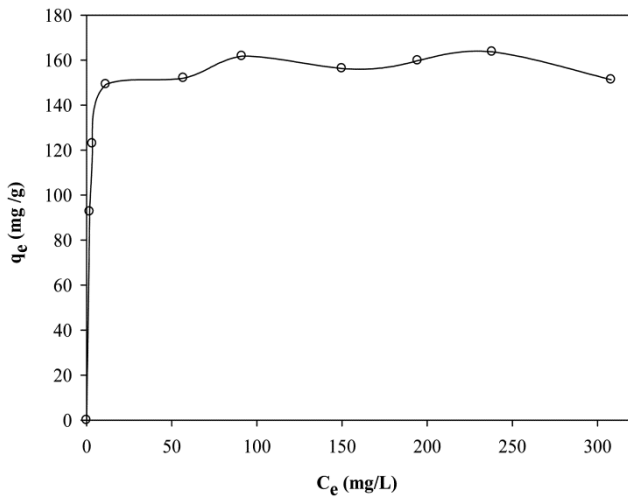


Figure 8. Adsorption isotherm of MB on ACDB

The essential characteristics of the Langmuir isotherm can be described by a separation factor R_L (Bulut *et al.*, 2008):

$$R_L = \frac{1}{1 + K_L C_0} \quad (6)$$

The value of R_L indicates the type of isotherm, favorable if ($0 < R_L < 1$), unfavorable if ($R_L > 1$), linear ($R_L = 1$) and irreversible if ($R_L = 0$) (Doğan *et al.*, 2008).

Table 2. Isotherm parameters for the adsorption of BM from aqueous solution by ACDB

Langmuir constants				Freundlich constants		
q_{max} (mg/g)	K_L (l/mg)	R_L	R^2	K_F (L/mg)	$1/n$	R^2
43.10	0.007	0.222	0.477	120.9	0.056	0.794

Figure 9a and b show the comparison of the linear forms of Langmuir and Freundlich isotherms for the adsorption of methylene blue ACDB. According to the Table 2, the maximum fixing capacity of methylene blue on ACDB is 163.67 mg/g, Figure 9b shows a better applicability of the Freundlich model which has the highest correlation factor compared to the Langmuir model, indicating the possibility of multilayer adsorption, it is also noted that the slope values ($1/n$) are less than 1, which represents that the adsorption is favorable with an L-type isotherm (Shavandi *et al.*, 2012). The adsorption capacity values of other works from the literature are illustrated in the Table 3.

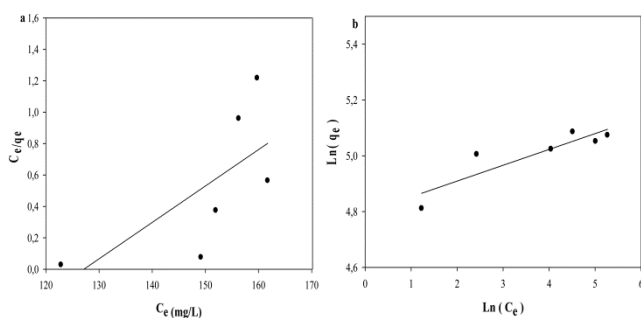


Figure 9. Linearizations according to Langmuir (a) and Freundlich (b)

Table 3. Comparison of adsorption capacities of various adsorbents for MB

Adsorbents	q_{exp} (mg/g)	References
Acrylic fibrous	20.6	Naeem <i>et al.</i> , 2016
Banana pith	04.6	Kadirvelu <i>et al.</i> , 2003
Sepiolite	57.3	Alkan <i>et al.</i> , 2008
Iron impregnated AC	30.61	Shah <i>et al.</i> , 2015
Rattan sawdust	294.1	Hameed <i>et al.</i> , 2007
Coir pith	05.8	Kavitha and Namasivayam, 2004
Pistachio shells	129.0	Attia <i>et al.</i> , 2003
Attapulgitte/bentonite	168.6	Liu <i>et al.</i> , 2014
Mango seed kernel	142.8	Vasanth <i>et al.</i> , 2005
Titanate nanotubes	133.3	Xiong <i>et al.</i> , 2010
Coconut coir dust	15.2	Macedo <i>et al.</i> , 2006
Groundnut shell	164.9	Kannan and Sundaram, 2001
Grinding palygorskite	111.7	Zhang <i>et al.</i> , 2015
Coconut leaves	149.3	Jawad <i>et al.</i> , 2016
AC Degla Beida stones	163.6	This work

4. Conclusion

This study estimated the adsorption performance of methylene blue MB dye from aqueous solution by activated carbon prepared from date stones ACDB and confirmed the possibility of valorizing the date stones as agricultural solid waste. The influence of the initial pH and adsorbent dose were studied, the results show that the adsorption capacity enhance with increase in the initial pH value of the aqueous solution and the adsorption efficiency increased with the increase of the adsorbent dose, maximum methylene blue removal was 163.67 mg/g. Experimental data was best approved with the kinetic model of pseudo second-order and best described by Freundlich model. This paper concludes that the activated carbon prepared from date stones ACDB can be used as low-cost adsorbent for the removal of methylene blue dye from aqueous solution.

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