

# Investigation of adsorptive properties of $\text{Ag}_2\text{CO}_3$ -polyaniline composite for environmental pollution control

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## Abstract

In this research, the  $\text{Ag}_2\text{CO}_3$ -PANI composite was synthesized with a simple precipitation method and then used as an effective adsorbent for adsorption of Methylene Blue cationic dyes from aqueous solution. Characterization of the adsorbent was carried out using UV-visible diffuse reflectance spectroscopy (UV-Vis DRS), X-ray diffraction (XRD), Fourier transform infrared spectroscopy (FT-IR) and scanning electron microscopy (SEM). The various parameters such as pH, contact time, sorbent dosage, initial dye concentration, and dye solution temperature were investigated. The optimum photo-catalytic activity of  $\text{Ag}_2\text{CO}_3$ -PANI at a weight content of 50% PANI for the degradation of MB was almost 86% that is much higher than the pure  $\text{Ag}_2\text{CO}_3$  and PANI. The results showed an efficient removal at pH 10.0, within 60 min, and by using  $1 \text{ g L}^{-1}$   $\text{Ag}_2\text{CO}_3$ -PANI composite at the temperature of  $32^\circ\text{C}$ . The kinetic and equilibrium data fit into pseudo-second-order kinetic ( $R^2 > 0.84$ ) and Freundlich isotherm ( $R^2 > 0.99$ ) models, respectively. Adsorption capacity ( $q_0$ ) calculated from Langmuir isotherm was found to be 55 mg/g. Thermodynamic studies indicated that the adsorption process was endothermic ( $\Delta H^\circ > 0$ ). The adsorption/desorption experiments were carried out attaining regenerations of up to 97% from MB, using distilled water and 0.1N HCl. The composite indicated high efficiency adsorptive properties and high reusability.

**Keywords:** Adsorption,  $\text{Ag}_2\text{CO}_3$ -PANI composite, adsorbent, methylene blue.

## 1. Background

Investigations show that more than 10,000 synthetic dyes are available annually at with over  $7 \times 10^5$  ton. Many dye pollutants exhibit a high degree of sustainability against biological degradation and remain stable for a long time. These compounds and their derived products are poisonous or carcinogenic agents; they can cause a genetic mutation. Also, these the contaminations prevent the growth of bacteria that can destroy the impurities and

causing an imbalance in the environment (Cheng *et al.*, 2014; Wang *et al.*, 2014a; Gupta *et al.*, 2015; Yao *et al.*, 2015). Many different methods, including biological treatment, coagulation/flocculation, membrane filtration, electrochemical methods, advanced oxidation processes and adsorption, have been used for the dye removal from water and wastewaters (Ai *et al.*, 2010; Mittal *et al.*, 2010; Ayad and El-Nasr, 2012; Saleh *et al.*, 2014; Yao *et al.*, 2015; Robati *et al.*, 2016). Among the various techniques for removal of dye, the adsorption method has been considered the most cost-effective method for environmental problems and it can remove classes of pollutants that are not easily degradable (Ahmaruzzaman and Gupta, 2011; Bao *et al.*, 2011; Gupta *et al.*, 2011; Gupta *et al.*, 2013; Xiong *et al.*, 2013; Yao and Liu, 2014). Photocatalytic degradation method has been applied for treatment of wastewater. This method has advantages such as low consumption of chemicals, no sludge production, relatively high mineralization, but by-products may be formed in this process (Crini, 2006; Yu *et al.*, 2014; Ghaedi *et al.*, 2015; Yu *et al.*, 2016; Saravanan *et al.*, 2013a; Saravanan *et al.*, 2016). Traditional semiconductors can only absorb the small amounts of photons in the visible region and need to irradiation of UV light for excitation, while sunlight irradiation is composed of 3-5% UV light and approximately 43% visible light. Moreover, the high recombination rate of the photo-excited electrons and holes are their drawback (Di-Paola *et al.*, 2012; McEvoy and Zhang, 2014; Wang *et al.*, 2010; Saravanan *et al.*, 2013b). Silver-containing compounds such as  $\text{Ag}_2\text{CO}_3$  possess distinct advantages as photocatalyst due to SPR effect of metallic silver nanoparticles that are produced in visible light (Ai *et al.*, 2013; Dai *et al.*, 2014; Wang *et al.*, 2014b; Xu *et al.*, 2011; Xu *et al.*, 2015; Dai *et al.*, 2012). The formation of silver semiconductor and other compounds can produce heterojunctions that greatly decrease the recombination of photogenerated electron and hole pairs (Shifu *et al.*, 2008; Liu *et al.*, 2015). The conjugated polymers can be excited upon visible-light and correct the wide bandgap semiconductors. Also, they are stable photosensitizers

(Wang *et al.*, 2010). Among the conjugated polymers, polyaniline (PANI) has been considered for non-toxicity, corrosion prevention, proper stability, special oxidation-reduction properties, simple synthesis and reasonable prices, high absorption coefficient in the visible region and the high mobility of the load carriers (Saleh and Gupta, 2011; Saleh *et al.*, 2012a; Behniafar *et al.*, 2016; Gu *et al.*, 2016). Meanwhile, supports such as activated carbons, clays, siliceous materials, zeolites and conjugated polymers were applied as adsorption of pollutants (Khani *et al.*, 2010; Padervand *et al.*, 2011; Gupta and Saleh, 2013; Saravanan *et al.*, 2013c; Saravanan *et al.*, 2013d; Gupta *et al.*, 2014a; Sohrabnezhad *et al.*, 2014; Devaraj *et al.*, 2016). PANI can be used as an appropriate adsorbent for removal of pollutants in separation and purification systems also as support for immobilization of photocatalyst. It can increase the adsorption of pollutants (Ai *et al.*, 2010; Di-Paola *et al.*, 2012; Bhaumik *et al.*, 2014; Rajendran *et al.*, 2016; Robati *et al.*, 2016; Saravanan *et al.*, 2015a; Xiong *et al.*, 2013). Herein,  $\text{Ag}_2\text{CO}_3$  and  $\text{Ag}_2\text{CO}_3$ -PANI were prepared *via* a simple precipitation method. The influences of important parameters such as support amount, pH effect, dye concentration, adsorbent dosage and contact time on the adsorption were investigated. Isotherm, kinetic and thermodynamic models were evaluated *via* the removal of MB as a model dye.

## 2. Materials and methods

### 2.1. Materials

Silver nitrate ( $\text{AgNO}_3$ ), sodium carbonate ( $\text{Na}_2\text{CO}_3$ ), aniline (An) monomer, ammonium persulfate ( $(\text{NH}_4)_2\text{S}_2\text{O}_8$ , APS), Hydrochloric acid and sodium hydroxide were used. Methylene blue (C.I. name: Basic Blue 9,  $\text{C}_{16}\text{H}_{18}\text{ClN}_3\text{S}\cdot 3\text{H}_2\text{O}$ ), was used as received.

### 2.2. Synthesis of $\text{Ag}_2\text{CO}_3$ , PANI, and $\text{Ag}_2\text{CO}_3$ -PANI

The synthesis of  $\text{Ag}_2\text{CO}_3$  was according to the literature (Asadollahi *et al.*, 2017). For polymerization of aniline, 100 mL of freshly distilled aniline monomer with a concentration of 0.2 M was taken in HCl solution and cooled up to  $5^\circ\text{C}$ . Then, ammonium persulfate was added into the mixture slowly, and the reaction mixture continues for 4 hours under stirring. The blackish green precipitation after 1 hour was filtered and dried in an oven at  $70^\circ\text{C}$  (Saleh and Gupta, 2012b; Ramkumar and Chandramouleeswaran, 2013; Asadollahi *et al.*, 2018). According to the previous work for preparation of  $\text{Ag}_2\text{CO}_3$ -PANI, 0.1 g PANI was dispersed into distilled water. Then,  $\text{AgNO}_3$  was added to the suspension and was stirred for 1 hour. The  $\text{Na}_2\text{CO}_3$  solution was added dropwise into the mentioned suspension and stirred for 3 h. The precipitate was collected by centrifugation, thoroughly washed with distilled water and dried at room temperature (Asadollahi *et al.*, 2018).

### 2.3. Characterization

For determination of functional groups, Fourier transforms infrared (FT-IR) spectra was used on a Brucek spectrophotometer in the  $400\text{--}4000\text{ cm}^{-1}$  spectral range.

The powder X-ray diffraction patterns were recorded by (XRD, Philips PW 1840) from  $10^\circ$  to  $70^\circ$  (2 $\theta$ ). UV-Vis diffuse reflectance spectra (DRS) of the prepared products were taken in the region of 330-950 nm. The morphology and size of the as-synthesized samples were characterized using scanning electron microscopy (SEM) on a JEM-100 CX microscope.

### 2.4. Evaluation of adsorption efficiency and photocatalytic activity of samples

The adsorption and photodegradation of MB dye were investigated for as-prepared PANI and composite. Batch experiments were carried out at a cylindrical pyrex-glass cell with 250 mL capacity. The whole reactor was cooled with a water-cooled jacket on its outside and the temperature was kept at  $25^\circ\text{C}$ . At adsorption experiment, the specified amount of composite (0.04-1.2 g/L) was added into 50 mL of aqueous solution of MB (10-100 mg/L) under stirring in the dark for 60 min to complete the adsorption-desorption equilibrium between the dye and the surface of the support and composite. Then, the composites at intervals of 15 min were collected and separated by centrifugation. The filtrate solutions were analyzed spectrophotometrically by measurement of the absorbance at  $\lambda = 664\text{ nm}$ .

Owing to the importance of pH, it was the first parameter for investigation at the adsorption experiment. Different amounts of pH were studied. In the adsorption isotherm tests, the initial MB concentrations were investigated. In addition, the effect of contact time and temperature on adsorption was checked out with an assessment of kinetic data and thermodynamic parameters.

After completion of the adsorption-desorption equilibrium between the dye and the surface of the composite, the solution was irradiated with a 200 W tungsten filament Philips lamp ( $\lambda \geq 400\text{ nm}$ ) under stirring. In a separate control experiment, the photodegradation of MB was measured under visible light irradiation at  $\lambda = 664\text{ nm}$  in the absent of photo-catalyst (photolysis). In the absence of PANI and composite, MB self-degradation was almost negligible under visible light irradiation.

The values of percentage removal (%Removal) and amount of dye adsorbed ( $q_e$ ) were calculated using the following relationships:

$$\text{Removal}(\%) = \frac{C_0 - C_e}{C_0} \times 100 \quad (1)$$

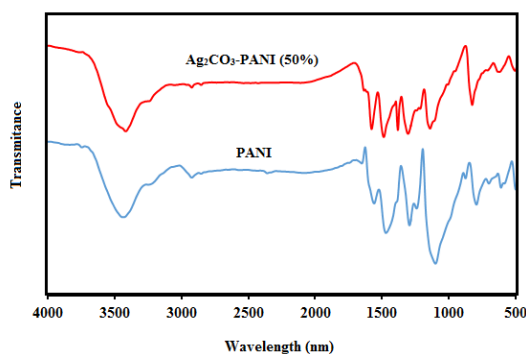
$$q_e = \frac{(C_0 - C_e)V}{m} \quad (2)$$

Where  $C_0$  and  $C_e$  are the initial and equilibrium dye concentration in the liquid phase ( $\text{mg L}^{-1}$ ) respectively,  $q_e$  is the amount of MB adsorbed into per unit weight of the adsorbent, V is the volume of the dye solution (L) and m is the mass of the used adsorbent (g) (Ayad and El-Nasr, 2012; Chen *et al.*, 2014).

### 3. Results

#### 3.1. Characterization of the structure of support, photocatalyst, and composite

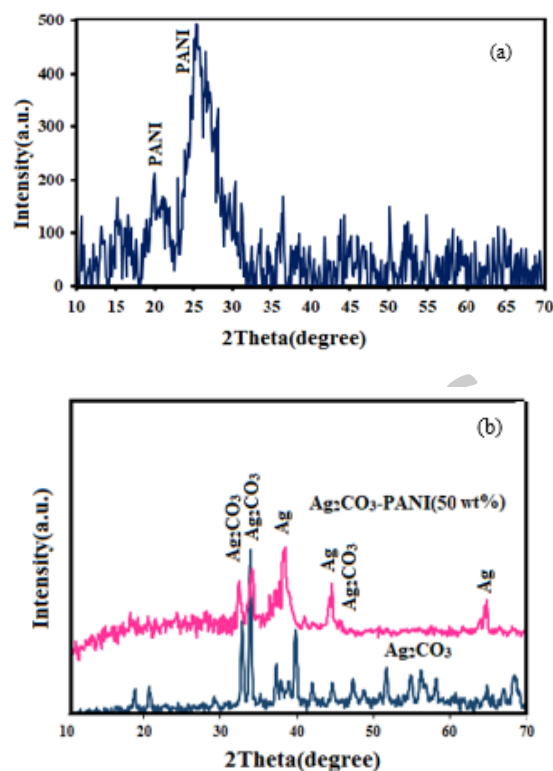
The FT-IR spectra of the PANI and  $\text{Ag}_2\text{CO}_3$ -PANI composite were represented in Figure 1 (Asadollahi *et al.*, 2018). It was observed that after the formation of composite between  $\text{Ag}_2\text{CO}_3$  and PANI, the absorption bands assigned to all of the vibrations have shifted to higher wavenumbers and the absorption band in  $1385\text{ cm}^{-1}$  is assigned to the presence of  $\text{CO}_3^{2-}$  (Yu *et al.*, 2014). These results confirmed the hybridization of the  $\text{Ag}_2\text{CO}_3$  and PANI.



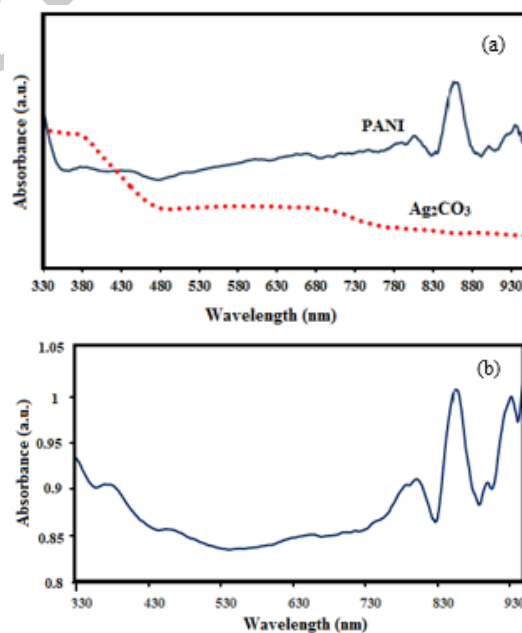
**Figure 1.** FT-IR spectra of PANI and  $\text{Ag}_2\text{CO}_3$ -PANI (50%) composite

Figure 2 showed the XRD patterns of PANI,  $\text{Ag}_2\text{CO}_3$  and  $\text{Ag}_2\text{CO}_3$ -PANI composite. In Figure 2a, the broad bands appearing at  $2\theta \approx 20^\circ$  and  $25^\circ$  are corresponding to the PANI chains (Jeong *et al.*, 2014; Zhang *et al.*, 2014). The XRD pattern of  $\text{Ag}_2\text{CO}_3$ -PANI was represented in Figure 2b. A short broad peak below  $2\theta = 35^\circ$  can be depending on the amorphous nature of the polymer structure (Shifu *et al.*, 2008). Diffraction peaks for monoclinic-phase  $\text{Ag}_2\text{CO}_3$  were confirmed with XRD patterns (JCPDS No. 26-0339) (Yao and Liu, 2014). For the metallic silver, the peaks at  $2\theta = 38.32^\circ$ ,  $44.37^\circ$  and  $64.67^\circ$  were indicated.

Figure 3 presented DRS spectra of doped PANI,  $\text{Ag}_2\text{CO}_3$ , and  $\text{Ag}_2\text{CO}_3$ -PANI composite. Based on previous studies, the acid-doped form of PANI display three characteristic absorption bands at 320–390, 400–450, and 740–950 nm. The formation of polarons (quinoid segments) of the PANI has happened in the visible range (about 440 nm). Two bands have appeared at 860 nm and 440 nm were related to  $\pi$ -polaron and polaron- $\pi^*$  transition in the acid-doped form of PANI. (Gölce *et al.*, 2013; Che, 2007). For the pure  $\text{Ag}_2\text{CO}_3$ , a wide absorption band from 480–750 nm was assigned to the localized surface plasmon resonance (LSPR) of Ag nanoparticles (Figure 3a) (Dai *et al.*, 2012; Tonda *et al.*, 2015). The absorption band of  $\text{Ag}_2\text{CO}_3$  and PANI in the  $\text{Ag}_2\text{CO}_3$ -PANI composite were shown in Figure 3b.

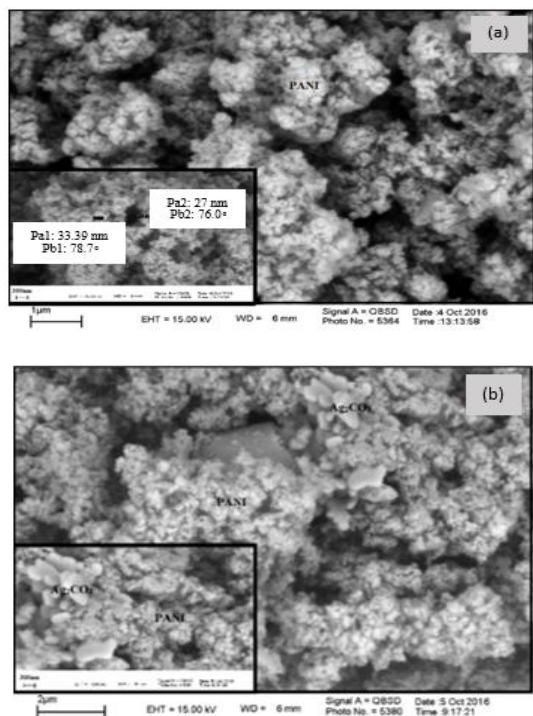


**Figure 2.** XRD patterns of a) PANI and b)  $\text{Ag}_2\text{CO}_3$  and  $\text{Ag}_2\text{CO}_3$ -PANI. Inset shows XRD patterns of PANI



**Figure 3.** Diffuse reflectance spectra of a) PANI,  $\text{Ag}_2\text{CO}_3$  and b)  $\text{Ag}_2\text{CO}_3$ -PANI

The morphology and structure of PANI and  $\text{Ag}_2\text{CO}_3$ -PANI samples were characterized by SEM images in Figure 4. According to the SEM images, PANI exhibits a sphere-like morphology (Figure 4a) and  $\text{Ag}_2\text{CO}_3$  sample with a smooth surface is located along the PANI (Figure 4a).



**Figure 4.** SEM images of the samples (a) PANI; (b)  $\text{Ag}_2\text{CO}_3$ -PANI

### 3.2. The effect of PANI percentages in composite

The effect of PANI percentages in composite on the removal of MB cationic dye was investigated. Adsorption of PANI was studied in three amounts of pH (pH = 4, 7 and 11). For  $\text{Ag}_2\text{CO}_3$ -PANI composites adsorption and photocatalytic degradation were checked out in two amounts of pH (pH = 7 and 11) with the various percentages of PANI. The adsorption for PANI and the removal efficiency of  $\text{Ag}_2\text{CO}_3$ -PANI (50%) composite were shown in Tables 1 and 2, respectively.

The adsorption of PANI was increased to 98% at alkaline pH but didn't show special adsorption at acidic pH

**Table 2.** The effect of different weight percentages of PANI in composite on adsorption, photodegradation efficiency and removal for  $\text{Ag}_2\text{CO}_3$ -PANI samples ( $C_{\text{MB}} = 50 \text{ mg L}^{-1}$ , the amounts of  $\text{Ag}_2\text{CO}_3$ -PANI (50%):  $1 \text{ g L}^{-1}$ , adsorption time: 60 min, photocatalytic degradation time: 90 min, T:  $32^\circ\text{C}$ )

	$\text{Ag}_2\text{CO}_3$ -PANI (10%)	$\text{Ag}_2\text{CO}_3$ -PANI (30%)	$\text{Ag}_2\text{CO}_3$ -PANI (50%)	$\text{Ag}_2\text{CO}_3$ -PANI (60%)	$\text{Ag}_2\text{CO}_3$ -PANI (80%)
%Adsorption (The solution natural pH)	0	3	10	8	3
%Adsorption (pH = 11)	8.5	45	81.4	94	98.1
%Photodegradation (pH = 11)	24	27.5	87.4	54.7	0
% Removal (pH = 11)	32	60.9	97.7	98	98.1

**Table 3.** The effect of pH on adsorption, photodegradation efficiency and removal for  $\text{Ag}_2\text{CO}_3$ -PANI sample (50%) in ( $C_{\text{MB}} = 50 \text{ mg L}^{-1}$ , the amounts of  $\text{Ag}_2\text{CO}_3$  and  $\text{Ag}_2\text{CO}_3$ -PANI (50%):  $1 \text{ g L}^{-1}$ , adsorption time: 60 min, photocatalytic degradation time: 90 min, T:  $32^\circ\text{C}$ )

	pH = 3	pH = 6	pH = 7	pH = 9	pH = 10	pH = 11
%Adsorption for PANI	8.24	32	60	87.32	98	98.5
$q_e$ of PANI ( $\text{mg g}^{-1}$ )	4.12	15.2	27.91	40.48	45.6	45.65
%Adsorption for $\text{Ag}_2\text{CO}_3$ -PANI (50%)	0	9.76	43.67	57	62.85	81.40
$q_e$ of $\text{Ag}_2\text{CO}_3$ -PANI(50%)	0	4.7	22	28.88	30.17	39.18
%Photodegradation for $\text{Ag}_2\text{CO}_3$ -PANI (50%)	0	0	48.83	55	85.75	87.38
% Removal for $\text{Ag}_2\text{CO}_3$ -PANI (50%)	0	9.76	71.29	80	94.38	97.67

(pH  $\sim 3$ ) (Table 1). According to Table 3, for  $\text{Ag}_2\text{CO}_3$ -PANI composites, high removal (adsorption and photodegradation) efficiency were gained under alkaline pH conditions. At alkaline medium, the surface of the composites becomes slightly negatively charged, thus the coordinative interactions with positively charge  $R_2 = N^+ = R'$  group of MB dye is increased.  $\text{Ag}_2\text{CO}_3$ -PANI (50%) composite was selected as an optimal sample because the photocatalytic degradation of dye increased in this sample (Saravanan *et al.*, 2015b). In other samples with higher percentages of PANI decrease in photocatalytic activity may be the result of the reduction of the amount of photocatalyst in composite due to a large amount of support in the sample.

**Table 1.** The adsorption for PANI sample ( $C_{\text{MB}} = 50 \text{ mg L}^{-1}$ , the amounts of PANI:  $1 \text{ g L}^{-1}$ , adsorption time: 60 min, T:  $32^\circ\text{C}$ )

	%Adsorption
	8 (The solution natural pH = 3)
PANI	60 (pH = 7)
	98.5 (pH = 11)

### 3.3. The effect of pH

The  $\text{pH}_{\text{PZC}}$  can be determined using the immersion technique. The adsorption of anions and cations is favored at  $\text{pH} < \text{pH}_{\text{PZC}}$  and  $\text{pH} > \text{pH}_{\text{PZC}}$ , respectively (Chingombe *et al.*, 2005; Zheng *et al.*, 2012). Using the immersion technique the  $\text{pH}_{\text{PZC}}$  values for PANI and composite were determined 10.5 and 6.5. The pH studies for PANI and  $\text{Ag}_2\text{CO}_3$ -PANI are summarized in Table 3. At the alkaline pH, samples were increasingly deprotonated, thus adsorption of dye was increased. The positively charged dye is attracted to the negatively charged surface sites of the PANI and  $\text{Ag}_2\text{CO}_3$ -PANI (50%) at pH = 10.



According to Table 3, adding of  $\text{Ag}_2\text{CO}_3$  into PANI cause to decrease the percentage and capacity adsorption for composite rather than the pure support but the comparison of %adsorption for PANI and removal percentage for  $\text{Ag}_2\text{CO}_3$ -PANI (50%) indicated that there isn't any significant difference between adsorbents at  $\text{pH} \geq 10$ . Thus  $\text{pH} = 10$  was selected as optimized pH.

### 3.4. Effect of different composite dosages on the removal of MB dye by $\text{Ag}_2\text{CO}_3$ -PANI (50%) composite

For investigating the effect of composite dosage on the adsorption of MB dye, different weights of  $\text{Ag}_2\text{CO}_3$ -PANI (50%) varied between 0.02 and 0.06 g were exposed to the 50 mL of the dye solution with 50.0 mg/L concentration for 60 min in the dark and 90 min under a light. The other operational parameters were kept at the optimum ( $\text{pH} = 10$ ). The obtained results have been summarized in Table 4 and Figure 5, respectively.

**Table 4.** The effect of adsorbent dosage on % adsorption, % photodegradation and % removal of MB by  $\text{Ag}_2\text{CO}_3$ -PANI (50%) Adsorption experiments ( $C_0 = 50 \text{ mg L}^{-1}$ , PANI and  $\text{Ag}_2\text{CO}_3$ -PANI (50%), equilibration time = 60 min,  $T = 32^\circ\text{C}$ ,  $\text{pH} = 10$ )

Dosage(g)	%Adsorption	$q_e$	%Photodegradation	%Removal
0.02	26.14	12.52	36.4	53
0.03	42	20.62	50	71
0.04	57.6	27.94	65.3	85.29
0.05	62.85	30.17	85.75	94.38
0.06	64.6	31.65	76.2	95.81

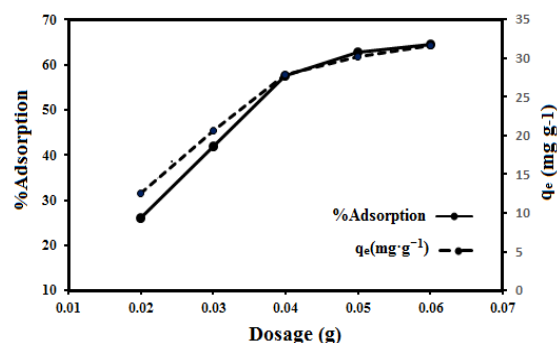
As seen in Figure 10 %adsorption is increased gradually with increasing the amount of sorbent due to increase in sportive surface area and availability of more exchangeable sites for dy (Asfaram *et al.*, 2015; Gupta *et al.*, 2014b). Adsorption of dye was observed at 62.85% for 0.050 g of the composite dosage and then increased slowly but photodegradation percent was decreased when 0.060 g of the composite was employed. This reduction could be attributed to the turbidity of solution and diminution of incident radiation into photo-catalyst (Saravanan *et al.*, 2013e).

## 4. Discussion

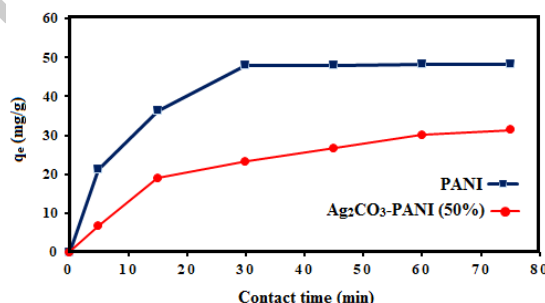
### 4.1. Adsorption kinetics

The adsorption kinetics was used for determination of the optimum time for the adsorption of MB by PANI and  $\text{Ag}_2\text{CO}_3$ -PANI (50%). Figure 5 shows the effect of contact time on the adsorption of MB onto PANI and  $\text{Ag}_2\text{CO}_3$ -PANI (50%) composite. As it is shown, the adsorption capacity for PANI increases rapidly and reaches equilibrium after 30 min, while for  $\text{Ag}_2\text{CO}_3$ -PANI (50%), this time is prolonged to 60 min.

In order to evaluate the adsorption behavior of MB by the used adsorbents, the pseudo-first-order and pseudo-second-order models were applied to interpret the experimental data, as shown below (Lagergren, 1898; Ho and McKay, 1998):



**Figure 5.** Effect of adsorbent dosage on  $q_e$  and adsorption percentage of MB by  $\text{Ag}_2\text{CO}_3$ -PANI (50%)



**Figure 6.** Effect of contact time on adsorption capacity of MB using PANI and  $\text{Ag}_2\text{CO}_3$ -PANI (50%). Adsorption experiments ( $C_0 = 50 \text{ mg L}^{-1}$ ,  $\text{pH} = 10$ , PANI and  $\text{Ag}_2\text{CO}_3$ -PANI (50%) dosage = 1 g  $\text{L}^{-1}$ , equilibration time = 60 min,  $T = 32^\circ\text{C}$ )

Pseudo-first-order equation:

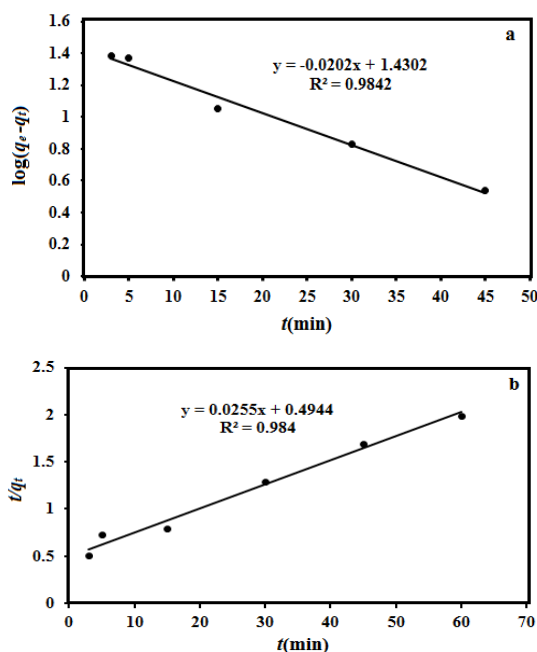
$$\log(q_e - q_t) = \log q_e - k_1/2.303 \quad (3)$$

Pseudo-second-order equation:

$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{t}{q_e} \quad (4)$$

Where  $q_e$  and  $q_t$  are the amounts of dye adsorbed ( $\text{mg g}^{-1}$ ) at equilibrium,  $t$  is the exposure time (min) and  $K$  is the rate constant, respectively. The validities of kinetic models are checked and verified by the linear equation analysis in Figure 7(a, b).

The kinetic parameters ( $k_1$ ,  $k_2$  and  $q_e$ ), and the correlation coefficients ( $R^2$ ) values were determined and summarized in Table 5.



**Figure 7.** Adsorption kinetic MB onto PANI and  $\text{Ag}_2\text{CO}_3$ -PANI (50%): (a) pseudo-first order model, (b) pseudo-second order model ( $C_0 = 50 \text{ mg L}^{-1}$ , PANI and  $\text{Ag}_2\text{CO}_3$ -PANI (50%) dosage =  $1 \text{ g L}^{-1}$ , equilibration time = 60 min,  $T = 32^\circ\text{C}$ )

**Table 5.** Kinetic parameters for the adsorption of MB onto  $\text{Ag}_2\text{CO}_3$ -PANI (50%) composite ( $C_0 = 50 \text{ mg L}^{-1}$ ,  $\text{pH} = 10$ , PANI and  $\text{Ag}_2\text{CO}_3$ -PANI (50%) dosage =  $1 \text{ g L}^{-1}$ , equilibration time = 60 min,  $T = 32^\circ\text{C}$ )

Models	Model coefficients	$R^2$
Pseudo-first-order	$q_{e,\text{cal}} = 27 \text{ mg g}^{-1}$ $q_{e,\text{exp}} = 30.17 \text{ mg g}^{-1}$ $k_1 = 0.0465 \text{ min}^{-1}$	0.9842
Pseudo-second-order	$q_e = 39.22 \text{ mg g}^{-1}$ $k_2 = 0.0013 \text{ mg g}^{-1} \text{ min}^{-1}$	0.984

Good correlation with the kinetic data explains the dye adsorption mechanism in the solid phase. There is no significant difference between  $R^2$  for the pseudo-first-order model and the pseudo-second-order model, while the obtained  $q_{e,\text{cal}}$  value was very close to the  $q_{e,\text{exp}}$  value for the pseudo-first-order model, implying that the pseudo-first-order model is suitable for describing the adsorption kinetics of MB onto  $\text{Ag}_2\text{CO}_3$ -PANI(50%) photo-catalyst (Ai *et al.*, 2010; Karthikeyan *et al.*, 2012; Xiong *et al.*, 2013). As shown in Figure 7 for PANI and  $\text{Ag}_2\text{CO}_3$ -PANI (50%) the external surface adsorption is very fast before 15 min. Then, the adsorption increased very slowly. This observation can be justified in this way: the saturation of the active sites decreases the rate of adsorption after 15 min.

#### 4.2. Adsorption isotherm

The results of initial concentration studies of dye on the percentages of adsorption, photodegradation, and removal of MB by PANI and  $\text{Ag}_2\text{CO}_3$ -PANI (50%) are summarized in Table 6.

**Table 6.** The effect of initial concentration on %adsorption, %photodegradation and % removal of MB by  $\text{Ag}_2\text{CO}_3$ -PANI (50%). (the amount of  $\text{Ag}_2\text{CO}_3$ -PANI (50%):  $1 \text{ g L}^{-1}$ , adsorption time = 60 min, photocatalytic degradation time = 90 min,  $T: 32^\circ\text{C}$ )

Support and catalyst	$C_0 = 30 \text{ mg L}^{-1}$	$C_0 = 50 \text{ mg L}^{-1}$	$C_0 = 60 \text{ mg L}^{-1}$	$C_0 = 80 \text{ mg L}^{-1}$	$C_0 = 100 \text{ mg L}^{-1}$
%Adsorption for $\text{Ag}_2\text{CO}_3$ -PANI (50%)	75.96	62.85	63	55.08	43.29
%Photodegradation for $\text{Ag}_2\text{CO}_3$ -PANI (50%)	68.24	85.75	65.42	61.92	56.79
% Removal for $\text{Ag}_2\text{CO}_3$ -PANI (50%)	92.3	94.38	87.2	82.89	75.5

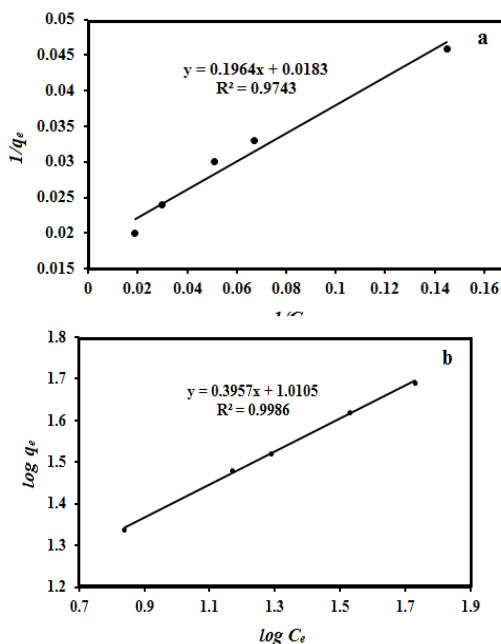
The adsorption isotherm models were applied to determine the specific relation between the concentration of adsorbate and the adsorption capacity of adsorbent, the maximum adsorption capacity of adsorbent and predictive modeling for analysis and design of adsorption systems. Two important isotherms (The Langmuir and Freundlich isotherm models) were selected to describe the mechanism of the adsorption process. The linear equation of the Langmuir (Eq. 5), Freundlich (Eq. 6) isotherm models are expressed as follows (Ai *et al.*, 2010; Ansari *et al.*, 2011; Bhaumik *et al.*, 2014; Xiong *et al.*, 2013):

$$\frac{1}{q_e} = \frac{1}{q_m} + \frac{1}{b q_m C_e} \quad (5)$$

$$\text{Log } q_e = \text{log } k_f + \frac{1}{n} \text{log } C_e \quad (6)$$

Where the constant  $b$  is related to the energy of adsorption ( $\text{L mg}^{-1}$ ), and  $q_m$  is the Langmuir monomolecular adsorption capacity ( $\text{mg g}^{-1}$ );  $k_f$  ( $\text{mg}^{(1-1/n)} \text{ g}^{-1} \text{ L}^{-n}$ ) and  $n$  are the Freundlich constants related to adsorption capacity ( $\text{mg g}^{-1}$ ) and intensity of adsorption, respectively. The  $n$  value between 2 and 10 indicates that the adsorption system is desirable, between 1 and 2 is fairly difficult, and less than 1 is poor (Yao *et al.*, 2010).

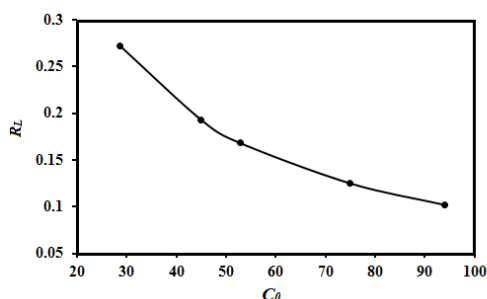
Figure 8(a, b) shows a linear plot of  $1/q_e$  against  $1/C_e$  for Langmuir isotherm and  $\text{log } q_e$  against  $\text{log } C_e$  for Freundlich isotherm. The Langmuir and Freundlich isotherm parameters were summarized in Table 7.



**Figure 8.** Adsorption isotherm models: (a) linear Langmuir model (b) linear Freundlich model for MB adsorption

**Table 7.** Isotherm parameters for the Adsorption of MB onto  $\text{Ag}_2\text{CO}_3$ -PANI (50%) composite

Catalyst	Langmuir			Freundlich		
	$q_m (\text{mg g}^{-1})$	$b (\text{L mg}^{-1})$	$R^2$	$K_f (\text{mg g}^{-1})$	$n$	$R^2$
$\text{Ag}_2\text{CO}_3$ -PANI (50%)	55	0.091	0.976	9.97	2.53	0.999



**Figure 9.** The plot of  $R_L$  value vs.  $C_0$  for linear Langmuir model

The higher value of correlation coefficients ( $R^2$ ) obtained for the Freundlich model (0.999) indicates that the Freundlich model fitted with the isotherm data better than the Langmuir model ( $R^2 = 0.976$ ). Furthermore, the calculated  $n$  value (2.53) indicates that the Freundlich model is favorable for describing the adsorption process. These results are in good agreement with the Pseudo-first-order model in kinetics studies.

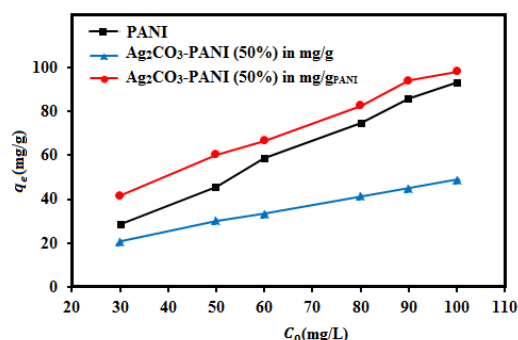
Here, it should be mentioned that the adsorption capacity of  $\text{Ag}_2\text{CO}_3$  for MB is negligible compared to PANI. Then it is anticipated that compared with PANI, the  $\text{Ag}_2\text{CO}_3$ -PANI (50%) will exhibit a decreasing adsorption capacity for MB. However, the decreased percentage is far less than the  $\text{Ag}_2\text{CO}_3$  content in  $\text{Ag}_2\text{CO}_3$ -PANI (50%). As seen in

The Langmuir isotherm makes several assumptions, such as the monolayer adsorption occurs on specific homogeneous sites of the adsorbent. The essential characteristics of the Langmuir isotherm can be expressed in terms of a dimensionless constant that called the separation factor or equilibrium parameter  $R_L$  and defined by the (Eq. 7).

$$R_L = \frac{1}{(1 + bC_0)} \quad (7)$$

The  $R_L$  value indicates the shape of the isotherm:  $R_L > 1$  (unfavorable isotherm),  $R_L = 1$  (linear isotherm),  $0 < R_L < 1$  (favorable isotherm),  $R_L = 0$  (irreversible isotherm) (Foo and Hameed, 2010). Another isotherm for adsorption processes on heterogeneous surfaces is the Freundlich isotherm that can be used for non-ideal adsorption. The calculated  $R_L$  values are in the range of 0.102-0.272 indicating that MB adsorption onto the  $\text{Ag}_2\text{CO}_3$ -PANI (50%) is favorable (Figure 9).

Figure 10, if the adsorption capacity is calculated based on per gram of PANI, the adsorption capacity of  $\text{Ag}_2\text{CO}_3$ -PANI (50%) for MB is observed to be higher than that of PANI (Zheng *et al.*, 2012).



**Figure 10.** The plot of the adsorption capacity against initial concentration of MB. Adsorption experiments ( $C_0 = 50 \text{ mg L}^{-1}$ , PANI and  $\text{Ag}_2\text{CO}_3$ -PANI (50%) dosage =  $1 \text{ g L}^{-1}$ , equilibration time = 60 min,  $T = 32^\circ\text{C}$ ,  $\text{pH} = 10$ )

The comparison of the adsorbent capacity of different low cost and commercially available adsorbents is shown in Table 8. When compared with other adsorbents, the results of the present study indicate that  $\text{Ag}_2\text{CO}_3$ -PANI composite as an adsorbent has better adsorption capacity in almost all cases and proves to be a cost-effective adsorbent that can be used for the removal of Methylene Blue cationic dyes from aqueous solution.

**Table 8.** The maximum adsorption capacity of various commercial adsorbents

Adsorbents	Adsorption Capacity (mg/g)	Reference
Polyacrylonitrile (PAN) based activated carbon nanofibers (ACNFs)	72.46	(Ibupoto <i>et al.</i> , 2018)
Graphene nanosheet/magnetite (Fe <sub>3</sub> O <sub>4</sub> ) composite	43.82	(Ai <i>et al.</i> , 2011a)
Carbonized citrus fruit peel	25.51	(Dutta <i>et al.</i> , 2011)
Fly ash	5.72	(Kumar <i>et al.</i> , 2005)
Magnetite-loaded multi-walled carbon nanotubes (M-MWCNTs)	48.06	(Ai <i>et al.</i> , 2011b)
Fe <sub>3</sub> O <sub>4</sub> @ZIF8-heterostructure	20.20	(Zheng <i>et al.</i> , 2014)
Raw KT3B kaolin (Algeria)	52.76	(Mouni <i>et al.</i> , 2018)
Natural zeolite	21.78	(Wang <i>et al.</i> , 2006)
Zeolites from kaolin (Egypt)	11.13 to 21.41	(EL-Mekkawi <i>et al.</i> , 2016)
Ag <sub>2</sub> CO <sub>3</sub> -PANI composite	55.00	Present study

#### 4.3. Thermodynamic parameters

The thermodynamic studies were performed with calculation of the change in Gibbs's free energy ( $\Delta G^\circ$ ), the change in entropy ( $\Delta S^\circ$ ) and the change in enthalpy ( $\Delta H^\circ$ ) for adsorbent using following relations (Mohammadi *et al.*, 2011; Zheng *et al.*, 2012):

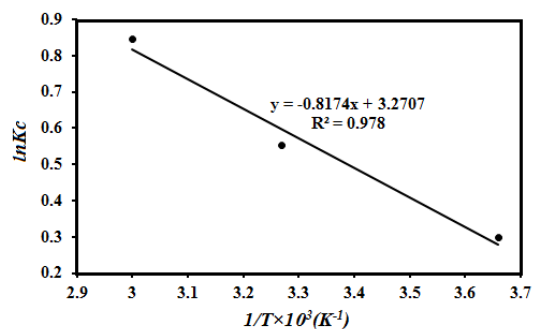
$$\Delta G^\circ = -RT \ln K_c \quad (8)$$

$$\Delta G^\circ = \Delta H^\circ - T\Delta S^\circ \quad (9)$$

$$K_c = \frac{C_{Ae}}{C_e} \quad (10)$$

$$\ln K_c = -\frac{\Delta H^\circ}{RT} + \frac{\Delta S^\circ}{R} \quad (11)$$

Where T is the absolute temperature in Kelvin (K),  $K_c$  is the equilibrium constant,  $C_{Ae}$  is the amount of dye adsorbed on the adsorbent per liter of the solution at equilibrium (mg L<sup>-1</sup>),  $C_e$  is the equilibrium concentration of the dye in the solution (mg L<sup>-1</sup>) and R is the gas constant (8.314 J mol<sup>-1</sup> K<sup>-1</sup>). The plot of  $\ln K_c$  against  $1/T$  (1 K<sup>-1</sup>) (the van't Hoff plot) was used to calculate thermodynamic adsorption parameters ( $\Delta H^\circ$  and  $\Delta S^\circ$ ) at solid-solution interface (Vadivelan and Kumar, 2005). The van't Hoff plot for the adsorption of MB onto Ag<sub>2</sub>CO<sub>3</sub>-PANI (50%) is given in Figure 11. The calculated values of the thermodynamic parameters are calculated and presented in Table 9.

**Figure 11.** The plot of  $\ln K_c$  against reciprocal temperature for the adsorption of MB by Ag<sub>2</sub>CO<sub>3</sub>-PANI (50%). Adsorption experiments:  $C_0 = 50$  mg L<sup>-1</sup>,  $t = 60$  min; pH = 10, adsorbent amount = 1 g L<sup>-1</sup>**Table 9.** The adsorption and photodegradation efficiency for Ag<sub>2</sub>CO<sub>3</sub>-PANI (50%) samples in different temperature. Adsorption experiments = 1 g L<sup>-1</sup>,  $C_{MB} = 50$  mg L<sup>-1</sup>, pH = 10, adsorption time = 60 min, photocatalytic degradation time = 90 min)

T (K)	%Adsorption	%Photodegradation	%Removal
273	57.4	48.49	79.43
306	63.43	72.65	90
333	70	83.36	94.65

Table 10 indicates thermodynamic parameters for the adsorption of MB by Ag<sub>2</sub>CO<sub>3</sub>-PANI (50%). The negative values of  $\Delta G^\circ$  for the MB adsorption on Ag<sub>2</sub>CO<sub>3</sub>-PANI (50%) at different temperatures indicate the spontaneous nature and feasibility of the process adsorption. The increase in  $-\Delta G^\circ$  indicated that the adsorption of MB on composite was more at the higher temperature. However, the moderate slope of  $\ln K_c$  T<sup>-1</sup> curve indicated that the temperature doesn't have a major effect on the adsorption process. The negative values of  $\Delta G^\circ$  for physisorption processes are usually between -20 and 0 kJ/mol, whereas that for chemisorption processes is often in the range of -80 to -400 kJ mol<sup>-1</sup>. This result was approved by the small numerical value of  $\Delta H^\circ$ . The positive value for enthalpy changes reveals the endothermic nature of adsorption and it shows the possibility of physical adsorption (the electrostatic attractions such as dipole-dipole, dispersion, London-Vander Waals and H-bonding). The positive value of  $\Delta S^\circ$  shows the increased randomness at the solid/solution interface (due to replacement of some hydration water molecules adsorbed on the surface of adsorbent with the dye molecules) and reflects the affinity of the Ag<sub>2</sub>CO<sub>3</sub>-PANI (50%) for MB dye (Ansari *et al.*, 2011; Kara *et al.*, 2015).

#### 4.4. Regeneration and reusability of Ag<sub>2</sub>CO<sub>3</sub>-PANI (50%)

According to the previous results, the adsorption of MB on Ag<sub>2</sub>CO<sub>3</sub>-PANI (50%) was a physical process. Thus desorption is expected to occur under the neutral or the acidic environments. In addition, some of the



adsorbed MB dye molecules photodegraded in the presence of photo-catalyst, so the calculated desorption percentage was lower than the expected value. One procedure for batch desorption of dye was as follows: at first, the adsorption experiment was done in ideal condition, and then the used composite in adsorption process was collected by centrifuge and dried at room temperatures. The dried solid was then added into the deionized water and then the acidic solution in two steps with stirring in dark for 1 hour. It was observed that a large amount of the previously adsorbed dye the composite was desorbed. Desorption efficiency was measured using the following equations (Zhao *et al.*, 2011; Christopher *et al.*, 2012; Ansari *et al.*, 2013; Yan *et al.*, 2016):

$$\text{Desorption ratio} = \frac{\text{Amount of dye desorbed to the desorption medium}(m^*)}{\text{Amount of dye adsorbed on the composite}(m_0)} \times 100 \quad (12)$$

$$m^* = C_e \times V' \quad (13)$$

$$m_0 = (C_0 - C_e) \times V \quad (14)$$

Where,  $m_0$  (mg) of the adsorbed dye onto the adsorbent,  $m^*$  (mg) of the released dye in the regenerated solution;  $V'$  is the volume of eluent solution (L).  $C_0$  and  $C_e$  are the initial (inlet) and equilibrium (outlet) concentrations ( $\text{mg L}^{-1}$ ) of dye, respectively (Mehraj *et al.*, 2014; Shang *et al.*, 2009). The results indicated the regeneration of up to 97% from an adsorbed dye, using water and 0.1 M HCl.

**Table 10.** Thermodynamic parameters for the adsorption of MB by  $\text{Ag}_2\text{CO}_3$ -PANI (50%)

T (K)	$K_c$	$-\Delta G^\circ$ ( $\text{J mol}^{-1}$ )	$\Delta H^\circ$ ( $\text{KJ mol}^{-1}$ )	$\Delta S^\circ$ ( $\text{J mol}^{-1} \text{K}^{-1}$ )
273	1.347	0.756	0.0067	0.0272
306	1.734	1.653		
333	2.330	2.388		

## 5. Conclusion

A highly efficient  $\text{Ag}_2\text{CO}_3$ -PANI heterojunction has been prepared successfully by a facile precipitation method. The using PANI with  $\text{Ag}_2\text{CO}_3$  influenced the adsorption capacity and the degradation rate of dye molecules on the surface of the composite. The Freundlich isotherm model provided the best fits to predict the adsorption equilibrium for the MB onto the photocatalyst. The kinetic study confirmed the pseudo-first-order model for the adsorption process. Owing to the thermodynamic study the adsorption process was spontaneous and endothermic ( $\Delta G < 0$  and  $\Delta H > 0$ ). The adsorption-desorption cycle experiments demonstrated the possibility of desorption for frequent application.

The excellent photocatalytic activity for the degradation of MB was superior to those of pure  $\text{Ag}_2\text{CO}_3$  and PANI under visible light irradiation. Thus PANI as a good support influences on photocatalytic activity and stability of photocatalyst and provide a promising insight into the application of various photosensitive Ag-based materials with enhanced adsorption, photocatalytic activity, and photo stability.

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