

Investigation of adsorptive properties of Ag₂CO₃-polyaniline composite for environmental pollution control

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ABSTRACT

In this research, the Ag₂CO₃-PANI composite was synthesized with a simple precipitation method and then used as an effective adsorbent for adsorption of Methylene Blue cationic dyes from aqueous solution. Characterization of the adsorbent was carried out using UV-visible diffuse reflectance spectroscopy (UV-Vis DRS), X-ray diffraction (XRD), Fourier transform infrared spectroscopy (FT-IR) and scanning electron microscopy (SEM). The various parameters such as pH, contact time, sorbent dosage, initial dye concentration, and dye solution temperature were investigated. The optimum photo-catalytic activity of Ag₂CO₃-PANI at a weight content of 50% PANI for the degradation of MB was almost 86% that is much higher than the pure Ag₂CO₃ and PANI. The results showed an efficient removal at pH 10.0, within 60 min, and by using 1 g L⁻¹ Ag₂CO₃-PANI composite at the temperature of 32 °C. The kinetic and equilibrium data fit into pseudo-second-order kinetic ($R^2 > 0.84$) and Freundlich isotherm ($R^2 > 0.99$) models, respectively. Adsorption capacity (q_0) calculated from Langmuir isotherm was found to be 55 mg/g. Thermodynamic studies indicated that the adsorption process was endothermic ($\Delta H^\circ > 0$). The adsorption/desorption experiments were carried out attaining regenerations of up to 97% from MB, using distilled water and 0.1N HCl. The composite indicated high efficiency adsorptive properties and high reusability.

KEYWORDS: Adsorption, Ag₂CO₃-PANI composite, Adsorbent, Methylene Blue.

Background

Investigations show that more than 10,000 synthetic dyes are available annually at with over 7×10⁵ ton. Many dye pollutants exhibit a high degree of sustainability against biological degradation and remain stable for a long time. These compounds and their derived products are poisonous or carcinogenic agents; they can cause a genetic mutation. Also, these the contaminations prevent the growth of bacteria that can destroy the impurities and causing an imbalance in the environment (Yao et al., 2015; Cheng et al., 2014; Wang et al., 2014 a; Gupta et al., 2015). Many different methods, including biological treatment, coagulation/flocculation, membrane filtration, electrochemical methods, advanced oxidation processes and adsorption, have been used for the dye removal from water and wastewaters (Yao et al., 2015; Ayad and El-Nasr, 2012; Ai et al., 2010; Mittal et al., 2010; Saleh et al., 2014; Robati et al., 2016). Among the various techniques for removal

of dye, the adsorption method has been considered the most cost-effective method for environmental problems and it can remove classes of pollutants that are not easily degradable (Xiong et al., 2013; Yao and Liu, 2014; Bao et al., 2011; Gupta et al., 2013; Gupta et al., 2011; Ahmaruzzaman and Gupta, 2011). Photocatalytic degradation method has been applied for treatment of wastewater. This method has advantages such as low consumption of chemicals, no sludge production, relatively high mineralization, but by-products may be formed in this process (Crini, 2006; Yu et al., 2014; Yu et al., 2016; Ghaedi et al., 2015; Saravanan et al., 2016; Saravanan et al., 2013a). Traditional semiconductors can only absorb the small amounts of photons in the visible region and need to irradiation of UV light for excitation, while sunlight irradiation is composed of 3–5% UV light and approximately 43% visible light. Moreover, the high recombination rate of the photo-excited electrons

and holes are their drawback (Di-Paola et al., 2012; McEvoy and Zhang, 2014; Wang et al., 2010; Saravanan et al., 2013b). Silver-containing compounds such as Ag_2CO_3 possess distinct advantages as photocatalyst due to SPR effect of metallic silver nanoparticles that are produced in visible light (Ai et al., 2013; Dai et al., 2014; Wang et al., 2014 b; Xu et al., 2011; Xu et al., 2015; Dai et al., 2012). The formation of silver semiconductor and other compounds can produce heterojunctions that greatly decrease the recombination of photogenerated electron and hole pairs (Shifu et al., 2008; Liu et al., 2015). The conjugated polymers can be excited upon visible-light and correct the wide bandgap semiconductors. Also, they are stable photosensitizers (Wang et al., 2010). Among the conjugated polymers, polyaniline (PANI) has been considered for non-toxicity, corrosion prevention, proper stability, special oxidation-reduction properties, simple synthesis and reasonable prices, high absorption coefficient in the visible region and the high mobility of the load carriers. (Behniafar et al., 2016; Gu et al., 2016; Saleh et al., 2012a; Saleh and Gupta, 2011). Meanwhile, supports such as activated carbons, clays, siliceous materials, zeolites and conjugated polymers were applied as adsorption of pollutants (Sohrabnezhad et al., 2014; Padervand et al., 2011; Devaraj et al., 2016, Saravanan et al., 2013c; Saravanan et al., 2013d; Gupta et al., 2014a; Khani et al., 2010; Gupta and Saleh, 2013). PANI can be used as an appropriate adsorbent for removal of pollutants in separation and purification systems also as support for immobilization of photocatalyst. It can increase the adsorption of pollutants (Ai et al., 2010; Xiong et al., 2013; Di-Paola et al., 2012; Bhaumik et al., 2014; Saravanan et al., 2015a; Rajendran et al., 2016; Robati et al., 2016). Herein, Ag_2CO_3 and Ag_2CO_3 -PANI were prepared *via* a simple precipitation method. The influences of important parameters such as support amount, pH effect, dye concentration, adsorbent dosage and contact time on the adsorption were investigated. Isotherm, kinetic and thermodynamic models were evaluated *via* the removal of MB as a model dye.

Materials and methods

Materials

Silver nitrate (AgNO_3), sodium carbonate (Na_2CO_3), aniline (An) monomer, ammonium persulfate ($(\text{NH}_4)_2\text{S}_2\text{O}_8$, APS), Hydrochloric acid and sodium hydroxide were used. Methylene blue (C.I. name: Basic Blue 9, $\text{C}_{16}\text{H}_{18}\text{ClN}_3\text{S}\cdot 3\text{H}_2\text{O}$), was used as received.

Synthesis of Ag_2CO_3 , PANI, and Ag_2CO_3 -PANI

The synthesis of Ag_2CO_3 was according to the literature (Asadollahi et al., 2017). For polymerization of aniline, 100 mL of freshly distilled aniline monomer with a concentration of 0.2 M was taken in HCl solution and cooled up to 5° C. Then, ammonium persulfate was added into the mixture slowly, and the reaction mixture continues for 4 hours under stirring. The blackish green precipitation after 1 hour was filtered and dried in an oven at 70°C (Ramkumar and Chandramouleeswaran, 2013; Asadollahi et al., 2018; Saleh and Gupta, 2012b). According to the previous work for preparation of Ag_2CO_3 -PANI, 0.1g PANI was dispersed into distilled water. Then, AgNO_3 was added to the suspension and was stirred for 1 hour. The Na_2CO_3 solution was added dropwise into the mentioned suspension and stirred for 3h. The precipitate was collected by centrifugation, thoroughly washed with distilled water and dried at room temperature (Asadollahi et al., 2018).

Characterization

For determination of functional groups, Fourier transforms infrared (FT-IR) spectra was used on a Brucek spectrophotometer in the 400-4000 cm^{-1} spectral range. The powder X-ray diffraction patterns were recorded by (XRD, Philips PW 1840) from 10° to 70° (2 θ). UV-Vis diffuse reflectance spectra (DRS) of the prepared products were taken in the region of 330-950 nm. The morphology and size of the as-synthesized samples were characterized using scanning electron microscopy (SEM) on a JEM-100 CX microscope.

Evaluation of adsorption efficiency and photocatalytic activity of sampels

The adsorption and photodegradation of MB dye were investigated for as-prepared PANI and composite. Batch experiments were carried out at a cylindrical pyrex-glass cell with 250 mL capacity. The whole reactor was cooled with a water-cooled jacket on its outside and the temperature was kept at 25°C. At adsorption experiment, the specified amount of composite (0.04-1.2 g/L) was added into 50 mL of aqueous solution of MB (10-100 mg/L) under stirring in the dark for 60 min to complete the adsorption-desorption equilibrium between the dye and the surface of the support and composite. Then, the composites at intervals of 15 min were collected and separated by centrifugation. The filtrate solutions were analyzed spectrophotometrically by measurement of the absorbance at $\lambda = 664$ nm.

Owing to the importance of pH, it was the first parameter for investigation at the adsorption experiment. Different amounts of pH were studied.

In the adsorption isotherm tests, the initial MB concentrations were investigated. In addition, the effect of contact time and temperature on adsorption was checked out with an assessment of kinetic data and thermodynamic parameters.

After completion of the adsorption-desorption equilibrium between the dye and the surface of the composite, the solution was irradiated with a 200 W tungsten filament Philips lamp ($\lambda \geq 400$ nm) under stirring. In a separate control experiment, the photodegradation of MB was measured under visible light irradiation at $\lambda=664$ nm in the absence of photo-catalyst (photolysis). In the absence of PANI and composite, MB self-degradation was almost negligible under visible light irradiation.

The values of percentage removal (%Removal) and amount of dye adsorbed (q_e) were calculated using the following relationships:

$$\text{Removal(\%)} = \frac{C_0 - C_e}{C_0} \times 100 \quad (\text{Eq. 1})$$

$$q_e = \frac{(C_0 - C_e)V}{m} \quad (\text{Eq. 2})$$

Where C_0 and C_e are the initial and equilibrium dye concentration in the liquid phase (mg L^{-1}) respectively, q_e is the amount of MB adsorbed into per unit weight of the adsorbent, V is the volume of the dye solution (L) and m is the mass of the used adsorbent (g) (Ayad and El-Nasr, 2012; Chen et al., 2014).

Results

Characterization of the structure of support, photo-catalyst, and composite

The FT-IR spectra of the PANI and Ag_2CO_3 -PANI composite were represented in figure 1 (Asadollahi et al., 2018). It was observed that after the formation of composite between Ag_2CO_3 and PANI, the absorption bands assigned to all of the vibrations have shifted to higher wavenumbers and the absorption band in 1385 cm^{-1} is assigned to the presence of CO_3^{2-} (Yu et al., 2014). These results confirmed the hybridization of the Ag_2CO_3 and PANI.

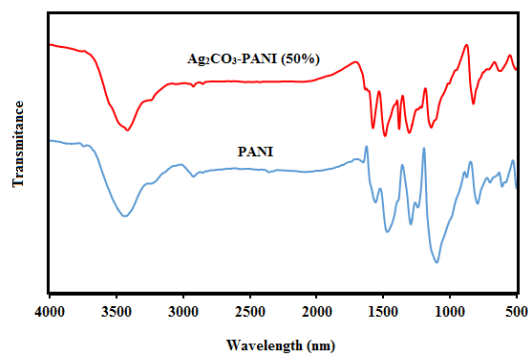


Figure 1. FT-IR spectra of PANI and Ag_2CO_3 -PANI (50%) composite

Figure 2 showed the XRD patterns of PANI, Ag_2CO_3 and Ag_2CO_3 -PANI composite. In Fig. 2.a, the broad bands appearing at $2\theta \approx 20^\circ$ and 25° are corresponding to the PANI chains (Jeong et al., 2014; Zhang et al., 2014). The XRD pattern of Ag_2CO_3 -PANI was represented in Fig. 2.b. A short broad peak below $2\theta = 35^\circ$ can be depending on the amorphous nature of the polymer structure (Shifu et al., 2008). Diffraction peaks for monoclinic-phase Ag_2CO_3 were confirmed with XRD patterns (JCPDS No. 26-0339) (Yao and Liu, 2014). For the metallic silver, the peaks at $2\theta = 38.32^\circ$, 44.37° and 64.67° were indicated.

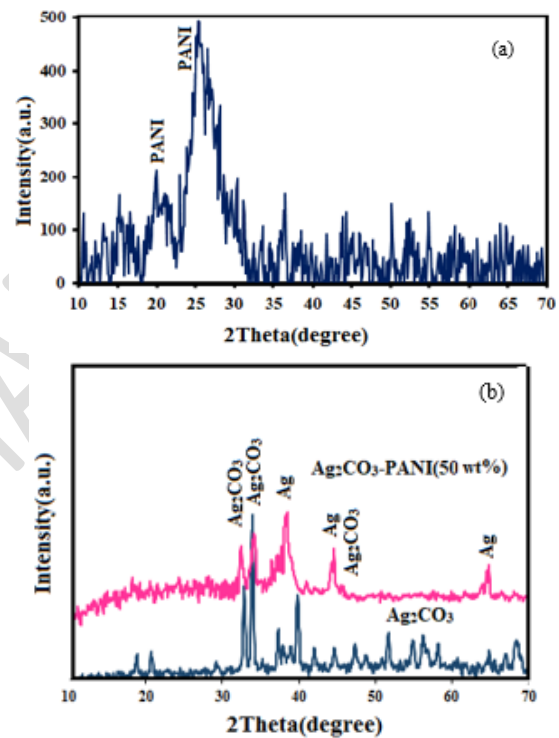


Fig. 2. XRD patterns of a) PANI and b) Ag_2CO_3 and Ag_2CO_3 -PANI. Inset shows XRD patterns of PANI

Figure 3 presented DRS spectra of doped PANI, Ag_2CO_3 , and Ag_2CO_3 -PANI composite. Based on previous studies, the acid-doped form of PANI display three characteristic absorption bands at 320–390, 400–450, and 740–950 nm. The formation of polarons (quinoid segments) of the PANI has happened in the visible range (about 440 nm). Two bands have appeared at 860 nm and 440 nm were related to π -polaron and polaron- π^* transition in the acid-doped form of PANI. (Gülce et al., 2013; Che, 2007). For the pure Ag_2CO_3 , a wide absorption band from 480–750 nm was assigned to the localized surface plasmon resonance (LSPR) of Ag nanoparticles (Figure 3.a) (Dai et al., 2012; Tonda et al., 2015). The absorption band of Ag_2CO_3

and PANI in the Ag_2CO_3 -PANI composite were shown in Fig. 3.b.

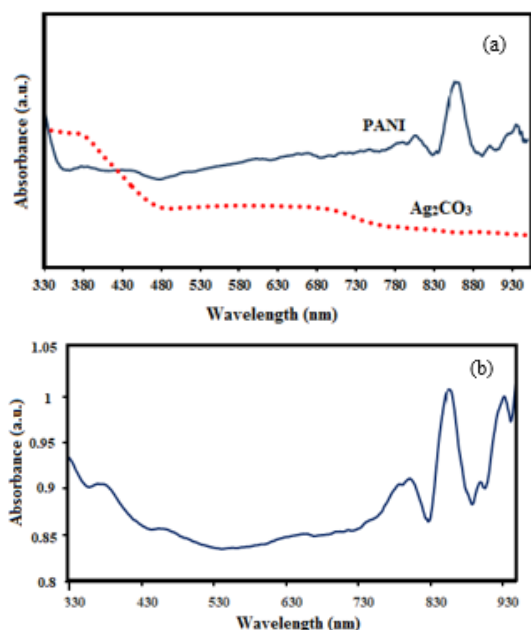


Fig. 3. Diffuse reflectance spectra of a) PANI, Ag_2CO_3 and b) Ag_2CO_3 -PANI

The morphology and structure of PANI and Ag_2CO_3 -PANI samples were characterized by SEM images in Fig. 4. According to the SEM images, PANI exhibits a sphere-like morphology (Fig. 4.a) and Ag_2CO_3 sample with a smooth surface is located along the PANI (Fig. 4.a).

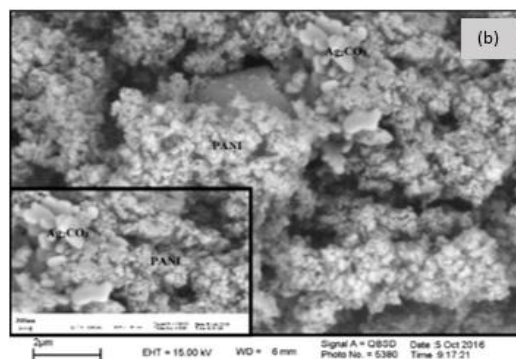
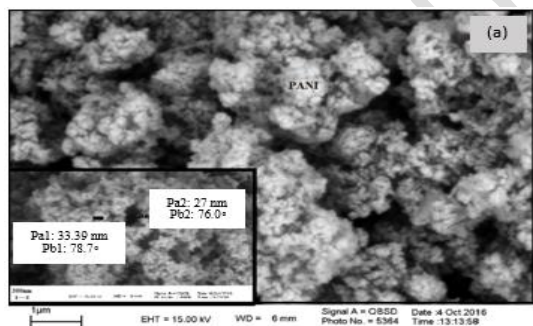


Fig. 4. SEM images of the samples (a) PANI; (b) Ag_2CO_3 -PANI

The effect of PANI percentages in composite

The effect of PANI percentages in composite on the removal of MB cationic dye was investigated. Adsorption of PANI was studied in three amounts of pH (pH =4, 7 and 11). For Ag_2CO_3 -PANI composites adsorption and photocatalytic degradation were checked out in two amounts of pH (pH = 7 and 11) with the various percentages of PANI. The adsorption for PANI and the removal efficiency of Ag_2CO_3 -PANI (50%) composite were shown in Table 1 and 2, respectively.

The adsorption of PANI was increased to 98% at alkaline pH but didn't show special adsorption at acidic pH (pH ~3) (Table 1). According to Table 3, for Ag_2CO_3 -PANI composites, high removal (adsorption and photodegradation) efficiency were gained under alkaline pH conditions. At alkaline medium, the surface of the composites becomes slightly negatively charged, thus the coordinative interactions with positively charge $R_2 = N^+ = R'$ group of MB dye is increased. Ag_2CO_3 -PANI (50%) composite was selected as an optimal sample because the photocatalytic degradation of dye increased in this sample (Saravanan et al., 2015b). In other samples with higher percentages of PANI decrease in photocatalytic activity may be the result of the reduction of the amount of photocatalyst in composite due to a large amount of support in the sample.

Table 1. The adsorption for PANI sample ($C_{MB}=50 \text{ mg L}^{-1}$, the amounts of PANI: 1 g L^{-1} , adsorption time: 60min, T: $32 \text{ }^\circ\text{C}$).

	%Adsorption
	8 (The solution natural pH=3)
PANI	60 (pH=7)
	98.5(pH=11)

Table 2. The effect of different weight percentages of PANI in composite on adsorption, photodegradation efficiency and removal for Ag₂CO₃-PANI samples (C_{MB}=50 mg L⁻¹, the amounts of Ag₂CO₃-PANI (50%): 1 g L⁻¹, adsorption time: 60min, photocatalytic degradation time: 90 min, T: 32 °C).

	Ag ₂ CO ₃ -PANI (10%)	Ag ₂ CO ₃ -PANI (30%)	Ag ₂ CO ₃ -PANI (50%)	Ag ₂ CO ₃ -PANI (60%)	Ag ₂ CO ₃ -PANI (80%)
%Adsorption (The solution natural pH)	0	3	10	8	3
%Adsorption (pH=11)	8.5	45	81.4	94	98.1
%Photodegradation (pH =11)	24	27.5	87.4	54.7	0
% Removal (pH=11)	32	60.9	97.7	98	98.1

The effect of pH

The pHPZC can be determined using the immersion technique. The adsorption of anions and cations is favored at pH < pHPZC and pH > pHPZC, respectively (Zheng et al., 2012; Chingombe et al., 2005). Using the immersion technique the pHPZC values for PANI and composite were determined 10.5 and 6.5. The

pH studies for PANI and Ag₂CO₃-PANI are summarized in Table 3. At the alkaline pH, samples were increasingly deprotonated, thus adsorption of dye was increased. The positively charged dye is attracted to the negatively charged surface sites of the PANI and Ag₂CO₃-PANI (50%) at pH=10.

Table 3. The effect of pH on adsorption, photodegradation efficiency and removal for Ag₂CO₃-PANI sample (50%) in (C_{MB}=50 mg L⁻¹, the amounts of Ag₂CO₃ and Ag₂CO₃-PANI (50%): 1 g L⁻¹, adsorption time: 60min, photocatalytic degradation time: 90 min, T: 32 °C).

	pH=3	pH=6	pH=7	pH=9	pH=10	pH=11
%Adsorption for PANI	8.24	32	60	87.32	98	98.5
q _e of PANI (mg g ⁻¹)	4.12	15.2	27.91	40.48	45.6	45.65
%Adsorption for Ag ₂ CO ₃ -PANI (50%)	0	9.76	43.67	57	62.85	81.40
q _e of Ag ₂ CO ₃ -PANI(50%)	0	4.7	22	28.88	30.17	39.18
%Photodegradation for Ag ₂ CO ₃ -PANI (50%)	0	0	48.83	55	85.75	87.38
% Removal for Ag ₂ CO ₃ -PANI (50%)	0	9.76	71.29	80	94.38	97.67

According to table 3, adding of Ag₂CO₃ into PANI cause to decrease the percentage and capacity adsorption for composite rather than the pure support but the comparison of %adsorption for PANI and removal percentage for Ag₂CO₃-PANI (50%) indicated that there isn't any significant difference between adsorbents at pH≥10. Thus pH=10 was selected as optimized pH.

Effect of different composite dosages on the removal of MB dye by Ag₂CO₃-PANI (50%) composite

For investigating the effect of composite dosage on the adsorption of MB dye, different weights of Ag₂CO₃-PANI (50%) varied between 0.02 and 0.06 g were exposed to the 50 mL of the dye solution with 50.0 mg/L concentration for 60 min in the dark and 90 min under a light. The other operational parameters were kept at the optimum (pH=10). The obtained results have been summarized in Table 4 and Fig. 5, respectively.

Table 4. The effect of adsorbent dosage on % adsorption, % photodegradation and % removal of MB by Ag₂CO₃-PANI (50%) Adsorption experiments (C₀ =50 mg L⁻¹, PANI and Ag₂CO₃-PANI (50%), equilibration time = 60 min, T= 32 °C, pH=10).

Dosage(g)	%Adsorption	q _e	%Photodegradation	%Removal
0.02	26.14	12.52	36.4	53
0.03	42	20.62	50	71
0.04	57.6	27.94	65.3	85.29
0.05	62.85	30.17	85.75	94.38
0.06	64.6	31.65	76.2	95.81

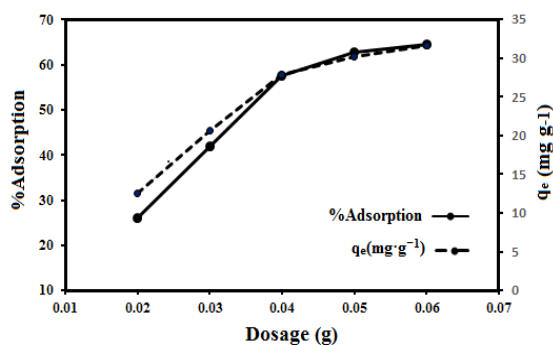


Fig. 5. Effect of adsorbent dosage on q_e and adsorption percentage of MB by Ag₂CO₃-PANI (50%)

As seen in Fig. 10 %adsorption is increased gradually with increasing the amount of sorbent due to increase in sportive surface area and availability of more exchangeable sites for dy (Asfaram et al., 2015; Gupta et al., 2014b). Adsorption of dye was observed at 62.85% for 0.050 g of the composite dosage and then increased slowly but photodegradation percent was decreased when 0.060 g of the composite was employed. This reduction could be attributed to the turbidity of solution and diminution of incident radiation into photo-catalyst (Saravanan et al., 2013e).

Discussion

Adsorption kinetics

The adsorption kinetics was used for determination of the optimum time for the adsorption of MB by PANI and Ag₂CO₃-PANI (50%). Fig. 5 shows the effect of contact time on the adsorption of MB onto PANI and Ag₂CO₃-PANI (50%) composite. As it is shown, the adsorption capacity for PANI increases rapidly and reaches equilibrium after 30 min, while for Ag₂CO₃-PANI (50%), this time is prolonged to 60 min.

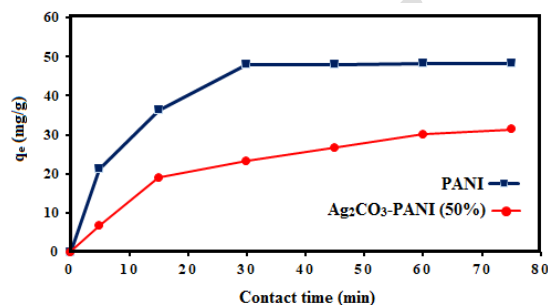


Fig. 6. Effect of contact time on adsorption capacity of MB using PANI and Ag₂CO₃-PANI (50%). Adsorption experiments (C₀=50 mg L⁻¹, pH= 10, PANI and Ag₂CO₃-PANI (50%) dosage= 1 g L⁻¹, equilibration time= 60 min, T= 32 °C).

In order to evaluate the adsorption behavior of MB by the used adsorbents, the pseudo-first-order and pseudo-second-order models were applied to interpret the experimental data, as shown below (Lagergren, 1898; Ho and McKay, 1998):

Pseudo-first-order equation:

$$\text{Log}(q_e - q_t) = \text{log}q_e - k_1/2.303 \quad (\text{Eq. 3})$$

Pseudo-second-order equation:

$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{t}{q_e} \quad (\text{Eq. 4})$$

Where q_e and q_t are the amounts of dye adsorbed (mg g⁻¹) at equilibrium, t is the exposure time (min) and K is the rate constant, respectively. The validities of kinetic models are checked and verified by the linear equation analysis in Fig. 7 (a, b).

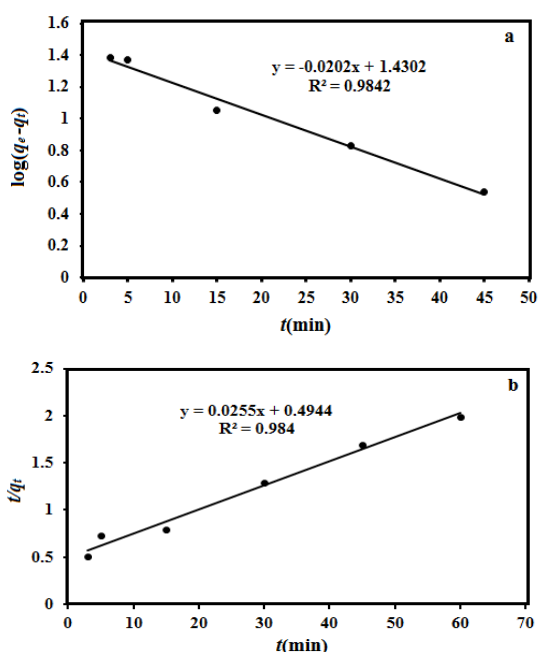


Fig. 7. Adsorption kinetic MB onto PANI and Ag₂CO₃-PANI (50%): (a) pseudo-first order model, (b) pseudo-second order model ($C_0 = 50 \text{ mg L}^{-1}$, PANI and Ag₂CO₃-PANI (50%) dosage = 1 g L^{-1} , equilibration time = 60 min, $T = 32 \text{ }^\circ\text{C}$)

The kinetic parameters (k_1 , k_2 and q_e), and the correlation coefficients (R_2) values were determined and summarized in Table 5.

Table 5. Kinetic parameters for the adsorption of MB onto Ag₂CO₃-PANI (50%) composite ($C_0 = 50 \text{ mg L}^{-1}$, pH=10, PANI and Ag₂CO₃-PANI (50%) dosage = 1 g L^{-1} , equilibration time = 60 min, $T = 32 \text{ }^\circ\text{C}$).

Models	Model coefficients	R^2
Pseudo-first-order	$q_{e,cal} = 27 \text{ mg g}^{-1}$	0.9842
	$q_{e,exp} = 30.17 \text{ mg g}^{-1}$	
	$k_1 = 0.0465 \text{ min}^{-1}$	
Pseudo-second-order	$q_e = 39.22 \text{ mg g}^{-1}$ $k_2 = 0.0013 \text{ g mg}^{-1} \text{ min}^{-1}$	0.984

Good correlation with the kinetic data explains the dye adsorption mechanism in the solid phase. There is no significant difference between R^2 for the pseudo-first-order model and the pseudo-second-order model, while the obtained $q_{e,cal}$ value was very close to the $q_{e,exp}$ value for the pseudo-first-order model, implying that the pseudo-first-order model is suitable for describing the adsorption kinetics of MB onto Ag₂CO₃-PANI(50%) photocatalyst (Ai et al., 2010; Xiong et al., 2013; Karthikeyan et al., 2012). As shown in Fig. 7 for PANI and Ag₂CO₃-PANI (50%) the external surface

adsorption is very fast before 15 min. Then, the adsorption increased very slowly. This observation can be justified in this way: the saturation of the active sites decreases the rate of adsorption after 15 min.

Adsorption isotherm

The results of initial concentration studies of dye on the percentages of adsorption, photodegradation, and removal of MB by PANI and Ag₂CO₃-PANI (50%) are summarized in Table 6.

Table 6. The effect of initial concentration on %adsorption, %photodegradation and % removal of MB by Ag₂CO₃-PANI (50%). (the amount of Ag₂CO₃-PANI (50%): 1 g L^{-1} , adsorption time=60min, photocatalytic degradation time=90 min, $T = 32 \text{ }^\circ\text{C}$)

Support and catalyst	$C_0 = 30 \text{ mg L}^{-1}$	$C_0 = 50 \text{ mg L}^{-1}$	$C_0 = 60 \text{ mg L}^{-1}$	$C_0 = 80 \text{ mg L}^{-1}$	$C_0 = 100 \text{ mg L}^{-1}$
%Adsorption for Ag ₂ CO ₃ -PANI (50%)	75.96	62.85	63	55.08	43.29
%Photodegradation for Ag ₂ CO ₃ -PANI (50%)	68.24	85.75	65.42	61.92	56.79

% Removal for Ag ₂ CO ₃ -PANI (50%)	92.3	94.38	87.2	82.89	75.5
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The adsorption isotherm models were applied to determine the specific relation between the concentration of adsorbate and the adsorption capacity of adsorbent, the maximum adsorption capacity of adsorbent and predictive modeling for analysis and design of adsorption systems. Two important isotherms (The Langmuir and Freundlich isotherm models) were selected to describe the mechanism of the adsorption process. The linear equation of the Langmuir (Eq. 5), Freundlich (Eq. 6) isotherm models are expressed as follows (Ai et al., 2010; Xiong et al., 2013; Bhaumik et al., 2014; Ansari et al., 2011):

$$\frac{1}{q_e} = \frac{1}{q_m} + \frac{1}{bq_m C_e} \quad (\text{Eq. 5})$$

$$\text{Log} q_e = \log k_f + \frac{1}{n} \log C_e \quad (\text{Eq. 6})$$

Where the constant b is related to the energy of adsorption ($L \text{ mg}^{-1}$), and q_m is the Langmuir monomolecular adsorption capacity (mg g^{-1}); k_f ($\text{mg}^{(1-1/n)} \text{ g}^{-1} \text{ L}^{-n}$) and n are the Freundlich constants related to adsorption capacity (mg g^{-1}) and intensity of adsorption, respectively. The n value between 2 and 10 indicates that the adsorption system is desirable, between 1 and 2 is fairly difficult, and less than 1 is poor (Yao et al., 2010).

Figs. 8 (a, b) shows a linear plot of $1/q_e$ against $1/C_e$ for Langmuir isotherm and $\log q_e$ against $\log C_e$ for Freundlich isotherm. The Langmuir and Freundlich isotherm parameters were summarized in Table 7.

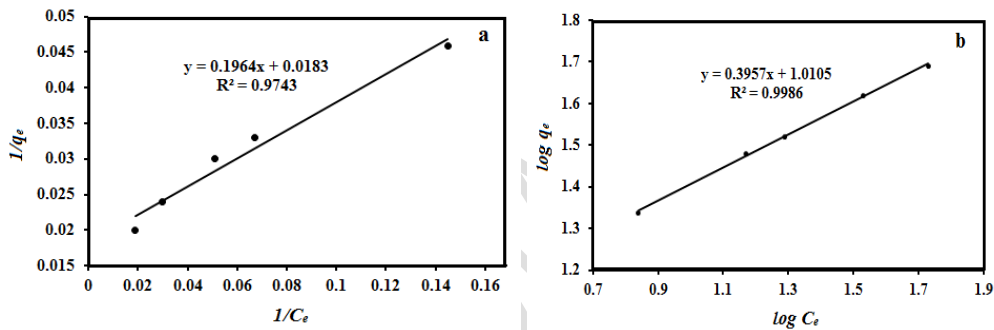


Fig. 8. Adsorption isotherm models: (a) linear Langmuir model (b) linear Freundlich model for MB adsorption

Table 7. Isotherm parameters for the Adsorption of MB onto Ag₂CO₃-PANI (50%) composite

Catalyst	Langmuir			Freundlich		
	$q_m (\text{mg g}^{-1})$	$b (L \text{ mg}^{-1})$	R^2	$K_f (\text{mg g}^{-1})$	n	R^2
Ag ₂ CO ₃ -PANI (50%)	55	0.091	0.976	9.97	2.53	0.999

The Langmuir isotherm makes several assumptions, such as the monolayer adsorption occurs on specific homogeneous sites of the adsorbent. The essential characteristics of the Langmuir isotherm can be expressed in terms of a dimensionless constant that called the separation factor or equilibrium parameter R_L and defined by the (Eq. 7).

$$R_L = \frac{1}{(1 + bC_0)} \quad (\text{Eq. 7})$$

The R_L value indicates the shape of the isotherm: $R_L > 1$ (unfavorable isotherm), $R_L = 1$ (linear isotherm), $0 < R_L < 1$ (favorable isotherm), $R_L = 0$ (irreversible isotherm) (Foo and Hameed, 2010). Another isotherm for adsorption processes on heterogeneous surfaces is the Freundlich isotherm that can be used for non-ideal adsorption. The

calculated R_L values are in the range of 0.102-0.272 indicating that MB adsorption onto the Ag₂CO₃-PANI (50%) is favorable (Fig. 9).

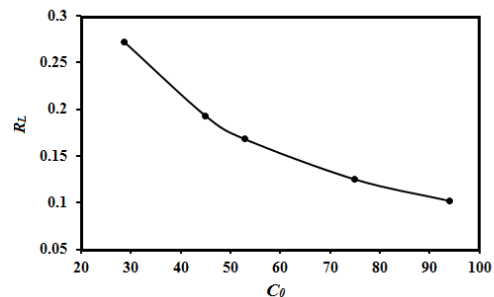


Fig. 9. The plot of R_L value vs. C_0 for linear Langmuir model

The higher value of correlation coefficients (R^2) obtained for the Freundlich model (0.999) indicates that the Freundlich model fitted with the isotherm data better than the Langmuir model ($R^2 = 0.976$). Furthermore, the calculated n value (2.53) indicates that the Freundlich model is favorable for describing the adsorption process. These results are in good agreement with the Pseudo-first-order model in kinetics studies.

Here, it should be mentioned that the adsorption capacity of Ag_2CO_3 for MB is negligible compared to PANI. Then it is anticipated that compared with PANI, the Ag_2CO_3 -PANI (50%) will exhibit a decreasing adsorption capacity for MB. However, the decreased percentage is far less than the Ag_2CO_3 content in Ag_2CO_3 -PANI (50%). As seen in Fig. 10, if the adsorption capacity is calculated based on per gram of PANI, the adsorption capacity of Ag_2CO_3 -PANI (50%) for MB is observed to be higher than that of PANI (Zheng et al., 2012).

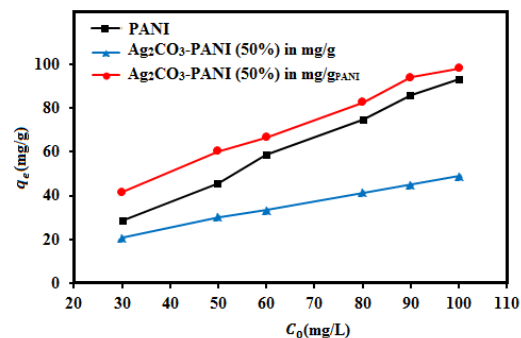


Fig. 10. The plot of the adsorption capacity against initial concentration of MB. Adsorption experiments ($C_0 = 50 \text{ mg L}^{-1}$, PANI and Ag_2CO_3 -PANI (50%) dosage = 1 g L^{-1} , equilibration time = 60 min, $T = 32 \text{ }^\circ\text{C}$, $\text{pH} = 10$).

The comparison of the adsorbent capacity of different low cost and commercially available adsorbents is shown in Table 8. When compared with other adsorbents, the results of the present study indicate that Ag_2CO_3 -PANI composite as an adsorbent has better adsorption capacity in almost all cases and proves to be a cost-effective adsorbent that can be used for the removal of Methylene Blue cationic dyes from aqueous solution.

Table 8. The maximum adsorption capacity of various commercial adsorbents

Adsorbents	Adsorption Capacity (mg/g)	Reference
polyacrylonitrile (PAN) based activated carbon nanofibers (ACNFs)	72.46	(Ibupoto et al., 2018)
graphene nanosheet/magnetite (Fe_3O_4) composite	43.82	(Ai et al., 2011, a)
Carbonized citrus fruit peel	25.51	(Dutta et al., 2011)
Fly ash	5.72	(Kumar et al., 2005)
magnetite-loaded multi-walled carbon nanotubes (M-MWCNTs)	48.06	(Ai et al., 2011, b)
Fe_3O_4 @ZIF8-heterostructure	20.20	(Zheng et al., 2014)
Raw KT3B kaolin (Algeria)	52.76	(Mouni et al., 2018)
Natural zeolite	21.78	(Wang et al., 2006)
Zeolites from kaolin (Egypt)	11.13 to 21.41	(EL-Mekkawi et al., 2016)
Ag_2CO_3 -PANI composite	55.00	Present study

Thermodynamic parameters

The thermodynamic studies were performed with calculation of the change in Gibb's free energy (ΔG°), the change in entropy (ΔS°) and the change in enthalpy (ΔH°) for adsorbent using following relations (Zheng et al., 2012; Mohammadi et al., 2011):

$$\Delta G^\circ = -RT \ln K_c \quad (\text{Eq. 8})$$

$$\Delta G^\circ = \Delta H^\circ - T \Delta S^\circ \quad (\text{Eq. 9})$$

$$K_c = \frac{C_{Ae}}{C_e} \quad (\text{Eq. 10})$$

$$\ln K_c = -\frac{\Delta H^\circ}{RT} + \frac{\Delta S^\circ}{R} \quad (\text{Eq. 11})$$

Where T is the absolute temperature in Kelvin (K), K_c is the equilibrium constant, C_{Ae} is the amount of dye adsorbed on the adsorbent per liter of the solution at equilibrium (mg L^{-1}), C_e is the

equilibrium concentration of the dye in the solution (mg L^{-1}) and R is the gas constant ($8.314 \text{ J mol}^{-1}\text{K}^{-1}$). The plot of $\ln K_c$ against $1/T$ (1 K^{-1}) (the van't Hoff plot) was used to calculate thermodynamic adsorption parameters (ΔH° and ΔS°) at solid-solution interface (Vadivelan and Kumar, 2005).

The van't Hoff plot for the adsorption of MB onto $\text{Ag}_2\text{CO}_3\text{-PANI}$ (50%) is given in Fig. 11. The calculated values of the thermodynamic parameters are calculated and presented in Table 9.

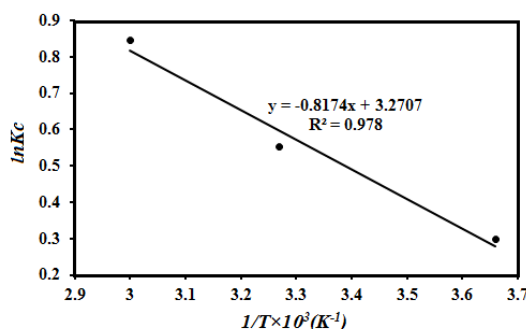


Fig. 11. The plot of $\ln K_c$ against reciprocal temperature for the adsorption of MB by $\text{Ag}_2\text{CO}_3\text{-PANI}$ (50%). Adsorption experiments: $C_0=50 \text{ mg L}^{-1}$, $t= 60 \text{ min}$; $\text{pH}=10$, adsorbent amount= 1 g L^{-1}

Table 9. The adsorption and photodegradation efficiency for $\text{Ag}_2\text{CO}_3\text{-PANI}$ (50%) samples in different temperature. Adsorption experiments= 1 g L^{-1} , $C_{\text{MB}}= 50 \text{ mg L}^{-1}$, $\text{pH}=10$, adsorption time= 60 min , photocatalytic degradation time= 90 min)

T (K)	%Adsorption	%Photodegradation	%Removal
273	57.4	48.49	79.43
306	63.43	72.65	90
333	70	83.36	94.65

Table 10 indicates thermodynamic parameters for the adsorption of MB by $\text{Ag}_2\text{CO}_3\text{-PANI}$ (50%). The negative values of ΔG° for the MB adsorption on $\text{Ag}_2\text{CO}_3\text{-PANI}$ (50%) at different temperatures indicate the spontaneous nature and feasibility of the process adsorption. The increase in $-\Delta G^\circ$ indicated that the adsorption of MB on composite was more at the higher temperature. However, the moderate slope of $\ln K_c T^{-1}$ curve indicated that the temperature doesn't have a major effect on the adsorption process. The negative values of ΔG° for physisorption processes are usually between -20 and 0 kJ/mol , whereas that for chemisorption processes is often in the range of -80 to -400 kJ

mol^{-1} . This result was approved by the small numerical value of ΔH° . The positive value for enthalpy changes reveals the endothermic nature of adsorption and it shows the possibility of physical adsorption (the electrostatic attractions such as dipole-dipole, dispersion, London-Vander Waals and H-bonding). The positive value of ΔS° shows the increased randomness at the solid/solution interface (due to replacement of some hydration water molecules adsorbed on the surface of adsorbent with the dye molecules) and reflects the affinity of the $\text{Ag}_2\text{CO}_3\text{-PANI}$ (50%) for MB dye (Ansari et al., 2011; Kara et al., 2015).

Table 10. Thermodynamic parameters for the adsorption of MB by $\text{Ag}_2\text{CO}_3\text{-PANI}$ (50%)

T (K)	K_c	$-\Delta G^\circ (\text{J mol}^{-1})$	$\Delta H^\circ (\text{KJ mol}^{-1})$	$\Delta S^\circ (\text{J mol}^{-1} \text{K}^{-1})$
273	1.347	0.756	0.0067	0.0272
306	1.734	1.653		
333	2.330	2.388		

Regeneration and reusability of $\text{Ag}_2\text{CO}_3\text{-PANI}$ (50%)

According to the previous results, the adsorption of MB on $\text{Ag}_2\text{CO}_3\text{-PANI}$ (50%) was a physical process. Thus desorption is expected to occur

under the neutral or the acidic environments. In addition, some of the adsorbed MB dye molecules photodegraded in the presence of photo-catalyst, so the calculated desorption percentage was lower than the expected value. One procedure for batch

desorption of dye was as follows: at first, the adsorption experiment was done in ideal condition, and then the used composite in adsorption process was collected by centrifuge and dried at room temperatures. The dried solid was then added into the deionized water and then the acidic solution in two steps with stirring in dark for 1hour. It was observed that a large amount of the previously adsorbed dye the composite was desorbed. Desorption efficiency was measured using the following equations (Ansari et al., 2013; Zhao et al., 2011; Yan et al., 2016; Christopher et al., 2012):

$$\text{Desorption ratio} = \frac{\text{Amount of dye desorbed to the desorption medium}(m^*)}{\text{Amount of dye adsorbed on the composite}(m_o)} \times 100 \quad (\text{Eq. 12})$$

$$m^* = C_e \times V' \quad (\text{Eq. 13})$$

$$m_o = (C_o - C_e) \times V \quad (\text{Eq. 14})$$

Where, m_o (mg) of the adsorbed dye onto the adsorbent, m^* (mg) of the released dye in the regenerated solution; V' is the volume of eluent solution (L). C_o and C_e are the initial (inlet) and equilibrium (outlet) concentrations (mg L^{-1}) of dye, respectively (Shang et al., 2009; Mehradj et al., 2014). The results indicated the regeneration of up to 97% from an adsorbed dye, using water and 0.1 M HCl.

Conclusion

A highly efficient Ag_2CO_3 -PANI heterojunction has been prepared successfully by a facile precipitation method. The using PANI with Ag_2CO_3 influenced the adsorption capacity and the degradation rate of dye molecules on the surface of the composite. The Freundlich isotherm model provided the best fits to predict the adsorption equilibrium for the MB onto the photocatalyst. The kinetic study confirmed the pseudo-first-order model for the adsorption process. Owing to the thermodynamic study the adsorption process was spontaneous and endothermic ($\Delta G < 0$ and $\Delta H > 0$). The adsorption-desorption cycle experiments demonstrated the possibility of desorption for frequent application. The excellent photocatalytic activity for the degradation of MB was superior to those of pure Ag_2CO_3 and PANI under visible light irradiation. Thus PANI as a good support influences on photocatalytic activity and stability of photocatalyst and provide a promising insight into the application of various photosensitive Ag-based materials with enhanced adsorption, photocatalytic activity, and photo stability.

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Figures Caption:

Fig. 1. FT-IR spectra of PANI and Ag₂CO₃-PANI (50%) composite

Fig. 2. XRD patterns of a) Pani and b) Ag₂CO₃ and Ag₂CO₃-PANI. Inset shows XRD patterns of PANI

Fig. 3. Diffuse reflectance spectra of a) PANI, Ag₂CO₃ and b) Ag₂CO₃-PANI

Fig. 4. SEM images of the samples (a) PANI; (b) Ag₂CO₃-PANI

Fig. 5. Effect of adsorbent dosage on q_e and adsorption percentage of MB by Ag₂CO₃-PANI (50%)

Fig. 6. Effect of contact time on adsorption capacity of MB using PANI and Ag₂CO₃-PANI (50%). Adsorption experiments ($C_0=50 \text{ mg L}^{-1}$, pH= 10, PANI and Ag₂CO₃-PANI (50%) dosage= 1 g L^{-1} , equilibration time= 60 min, T= 32 °C).

Fig. 7. Adsorption kinetic MB onto PANI and Ag₂CO₃-PANI (50%): (a) pseudo-first order model, (b) pseudo-second order model ($C_0 =50 \text{ mg L}^{-1}$, PANI and Ag₂CO₃-PANI (50%) dosage = 1 g L^{-1} , equilibration time = 60 min, T= 32 °C)

Fig. 8. Adsorption isotherm models: (a) linear Langmuir model (b) linear Freundlich model for MB adsorption

Fig. 9. The plot of R_L value vs. C_0 for linear Langmuir model.

Fig. 10. The plot of the adsorption capacity against initial concentration of MB. Adsorption experiments ($C_0 =50\text{mg/L}$, PANI and Ag₂CO₃-PANI (50%) dosage = 1 g L^{-1} , equilibration time = 60 min, T= 32 °C, pH=10).

Fig. 11. The plot of $\ln K_c$ against reciprocal temperature for the adsorption of MB by Ag₂CO₃-PANI (50%). Adsorption experiments: $C_0=50 \text{ mg L}^{-1}$, t= 60 min; pH=10, adsorbent amount= 1 g L^{-1} .

Tables Caption:

Table 1. The adsorption for PANI sample ($C_{MB}=50 \text{ mg L}^{-1}$, the amounts of PANI: 1 g L^{-1} , adsorption time: 60min, T: $32 \text{ }^{\circ}\text{C}$).

Table 2. The effect of different weight percentages of PANI in composite on adsorption, photodegradation efficiency and removal for Ag_2CO_3 -PANI samples ($C_{MB}=50 \text{ mg L}^{-1}$, the amounts of Ag_2CO_3 -PANI (50%): 1 g L^{-1} , adsorption time: 60min, photocatalytic degradation time: 90 min, T: $32 \text{ }^{\circ}\text{C}$).

Table 3. The effect of pH on adsorption, photodegradation efficiency and removal for Ag_2CO_3 -PANI sample (50%) in ($C_{MB}=50 \text{ mg L}^{-1}$, the amounts of Ag_2CO_3 and Ag_2CO_3 -PANI (50%): 1 g L^{-1} , adsorption time: 60min, photocatalytic degradation time: 90 min, T: $32 \text{ }^{\circ}\text{C}$).

Table 4. The effect of adsorbent dosage on % adsorption, % photodegradation and % removal of MB by Ag_2CO_3 -PANI (50%) Adsorption experiments ($C_0 = 50 \text{ mg L}^{-1}$, PANI and Ag_2CO_3 -PANI (50%), equilibration time = 60 min, T= $32 \text{ }^{\circ}\text{C}$, pH=10).

Table 5 Kinetic parameters for the adsorption of MB onto Ag_2CO_3 -PANI (50%) composite ($C_0=50 \text{ mg L}^{-1}$, pH=10, PANI and Ag_2CO_3 -PANI (50%) dosage = 1 g L^{-1} , equilibration time = 60 min, T= $32 \text{ }^{\circ}\text{C}$).

Table 6. The effect of initial concentration on %adsorption, %photodegradation and % removal of MB by Ag_2CO_3 -PANI (50%). (The amount of Ag_2CO_3 -PANI (50%): 1 g L^{-1} , adsorption time=60min, photocatalytic degradation time=90 min, T: $32 \text{ }^{\circ}\text{C}$)

Table 7. Isotherm parameters for the Adsorption of MB onto Ag_2CO_3 -PANI (50%) composite

Table 8. The maximum adsorption capacity of various commercial adsorbents

Table 9. The adsorption and photodegradation efficiency for Ag_2CO_3 -PANI (50%) samples in different temperature. Adsorption experiments= 1 g L^{-1} , $C_{MB}= 50 \text{ mg L}^{-1}$, pH=10, adsorption time=60min, photocatalytic degradation time=90 min)

Table 10. Thermodynamic parameters for the adsorption of MB by Ag_2CO_3 -PANI (50%)