

**Abatement of odour emissions by UV/Ozone oxidation process****OLIVA G.\*, NADDEO V., ZARRA T. and BELGIORNO V.**<sup>1</sup>Sanitary and Environmental Engineering Division (SEED), Department of Civil Engineering, University of Salerno

\*corresponding author: G. Oliva

e-mail: [goliva@unisa.it](mailto:goliva@unisa.it)

**Abstract** The growing expectations of the population and the increasingly stringent regulations about air pollution have resulted in the need to minimize and conveniently treat the waste gas from different emission sources. The emissions from a large variety of plants, including waste and wastewater treatment plants, result mainly from the degradation of organic matter. These emissions are composed of a complex of substances emitted at low concentrations from diffusive sources. These characteristics make complex their treatment in economically efficient conditions. The design and management of environmental protection and industrial plants, therefore, require the implementation of focused processes for the control of the target compounds. The present study shows the applicability of an UV-Ozone lab-scale system for odours and VOCs removal. An artificial gaseous stream contaminated by toluene, at different incoming concentrations, was treated evaluating the abatement efficiencies in terms of odours and total VOCs as a function of power and contact time. The residue ozone concentrations was determined in order to optimize the set-up conditions. The results were discussed with the aim of evaluating the feasibility of the investigated solution for the advanced treatment of the waste gas from environmental facilities. Removal efficiencies up to 91% were reached for the investigated conditions. Lower inlet concentrations resulted in high residue ozone outgoing the processes and, thus, it resulted over dimensioned for inlet load lower than 1,22 mg per minute.

**Keywords: VOCs, odours, AOPs, UV, Ozone****1. Introduction**

The emission of Volatile Organic Compounds (VOCs) is of great concern in the management of a variety of facilities including wastewater treatment, composting, industrial and CAFO (Concentrated Animal Feeding Operations) plants, and landfill, due to their toxicity, odour pollution and contribution to photochemical oxidants (Navia and Muñoz, 2015; Wang et al., 2013). Beside the effects on environment and human health, these emissions may cause odour annoyance among the population living surrounding the plants. The odour

management is always more becoming a major issue for industrial operators (Belgiorno et al., 2012). The urbanized areas have been expanding increasingly closer to industrial sites and, consequently, it results no longer effective to rely on buffer distances to avoid odour pollution (Holub, 2014; Naddeo et al., 2016a; Zarra et al., 2008).

Odours can substantially result in an environmental discomfort which may cause psychophysiological disorders, such as nausea, headaches, insomnia, loss of appetite or respiratory problems, and to a general worsening of life quality (Lucernoni et al., 2016; Naddeo et al., 2016a; Zarra et al., 2009).

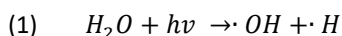
These aspects have led to the need of defining suitable tools to face the increasing number of administrative and legal complaints, merged in stricter regulations regarding emission and exposure levels (Estrada et al., 2015; Naddeo et al., 2013; Naddeo et al., 2016b; Zarra et al., 2012).

The necessity to address compliance to regulations and good public image has forced the polluting plants to adopt effective off-gas abatement technologies (Lebrero et al., 2011; Mudliar et al., 2010). The most widespread technologies for odour abatement are biological and chemical-physical processes (Bindra et al., 2015; Iranpour et al., 2005). Biotechnologies represent an economic and environmental-friendly waste gas treatment solution. These technologies result also suitable for high concentrations of compounds containing sulphur, chlorine, and/or nitrogen, showing a high efficiency for biodegradable compounds. However, biomass builds up have to be disposed as waste and percolate water needs treatment; furthermore, poorly soluble components result difficult to abate and toxic compounds inhibit the process. Chemical-physical processes, instead, represent proven and tested technologies, resulting effective for large air volumes. These processes, however, promote the transfer of the contaminants from gaseous phase to liquid or solid phases, with the need of further treatments (Alfonsín et al., 2015; Bindra et al., 2015; Estrada et al., 2015).

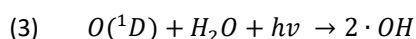
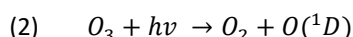
To overcome the limitations of the conventional processes, the scientific literature has focused the attention on the Advanced Oxidation Processes (AOPs) as alternative technologies applicable to a wide variety of polluting compounds and at different range of concentrations (Idi et al., 2015; Paz, 2010; Swetha et al., 2017; Yao and Feilberg, 2015).

Among the AOPs, the UV/O<sub>3</sub> process addresses the decomposition of gaseous VOCs providing direct photolysis by UV, direct oxidation by ozone molecules, and indirect oxidation by hydroxyl radicals. 185 and 254 nm dominant UV wavelengths are usually investigated to study the photochemical reactions of organic compounds in liquid and gas phases. The presence of water vapor allow the absorption at UV range of 100–

200 nm. The dissociation of water vapor into hydrogen and hydroxyl radicals follows the equation (1) (Chou et al., 2005).



Moreover, at wavelengths of 300 nm it is possible to detect also the conversion of ozone molecule into an oxygen molecule and an  $O(^1D)$  atom and reacts with water vapor to form two hydroxyl radicals. These mechanisms are described by equation (2) and (3) (Chou et al., 2005).



The hydroxyl radicals generated as showed in the equation 2 and 3 may, consequently, react with organic compounds, addressing their decoposition (Chou et al., 2005).

The present work illustrates the applicability of an UV-Ozone lab-scale system for odours abatement and VOCs removal from an artificial gaseous stream contaminated by toluene, selected as target VOC.

The preliminary results of the study were discussed in terms of toluene and odours concentrations reduction, aiming at evaluating the performances of the investigated configurations as a function of the applied voltage and the incoming toluene concentrations.

The main results highlight the suitability of the advanced ozonation UV-induced process for the treatment of off-gas from a great variety of odours emitting plants.

## 2. Materials and methods

### 2.1. Experimental set-up

The experiments were carried out in a lab-scale plant consisting in a steel photo-reactor composed of a central body (48.6 cm length x 33.7 cm height x 17.8 cm

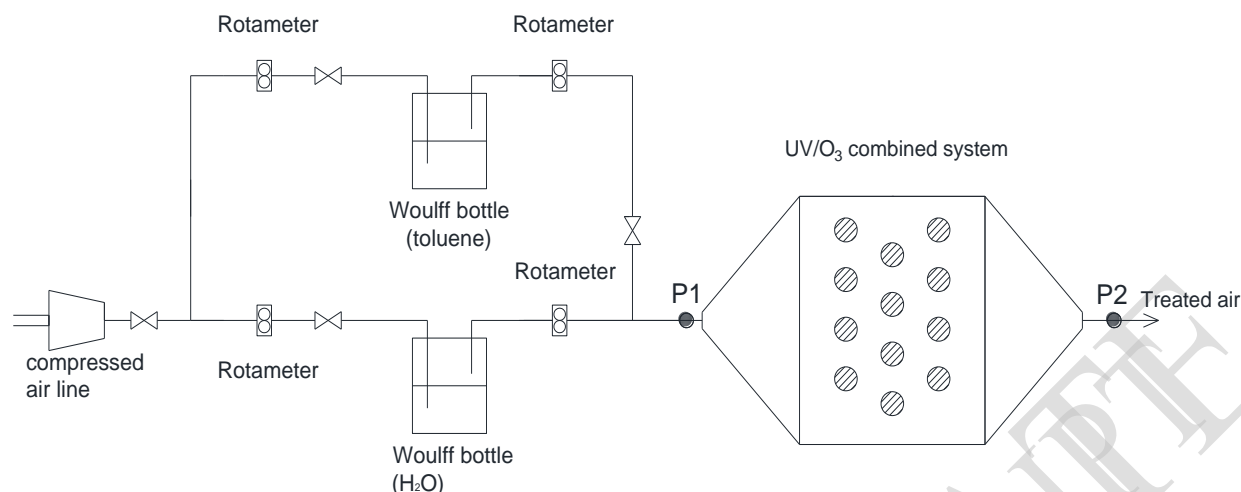
width) in which are located four UV lamps and two pyramidal-truncated hoods (25 cm height). The UV lamps are able to generate ozone. The scheme of the experimental system is shown in **Figure 1**. For the generation of the synthetic odorous waste stream, a metered stream of oil-free compressed air was passed through a Woulff-bottle pure toluene (Sigma Aldrich; CAS: 108-88-3) containing. This concentrated vapor was diluted to the expected concentration with oil-free water-saturated compressed air (Wang et al., 2013). The waste gas stream was then fed to the reactor. In **Table 1** are reported the main operating parameters of the realized experimental set-up. In the **Table 2** are reported the main parameter of the lamps used for the experimental activity.

### 2.2. Analytical methodology

Gas phase toluene concentration was measured using a Photoionization Detector (PID, Tiger, Ion Science) at point P1 and P2. Toluene removal efficiency ( $\eta$ ) was calculated as follows:

$$(4) \quad \eta = \frac{C_{toluene,in} - C_{toluene,out}}{C_{toluene,in}} \cdot 100\%$$

The ozone generated by the UV lamps and the output residue ozone were measured by the Standard Method 2350E 106 (Ozone Demand/Requirement-Semi-Batch Method). In Table 3 is reported the dependence of ozone generation rate on the applied voltage, obtained for an airflow rate equal to 13 lpm. The ozone generated resulted not linear dependent from the number of lamps on, expressed as applied voltage. This effect was probably related to the position of the lamps on and to the geometry of the reactor. The lamps which were not directly invested from the airflow contributed least to the ozone production. In the investigated conditions of airflow and humidity, the maximum value of ozone produced was obtained with four lamps on and it was equal to 57.6 mg of ozone per minute.



**Figure 1.** Experimental set-up system

**Table 1.** Operating parameters

| Parameter                   | Value                 |
|-----------------------------|-----------------------|
| Flow rate                   | 13 lpm                |
| Volume of reactor           | 0.0776 m <sup>3</sup> |
| Overall Length of each lamp | 287 mm                |
| Lamp Wattage                | 14 W                  |

**Table 2.** UV lamps parameter

| Parameter             | Value   |
|-----------------------|---------|
| Overall Length (OL)   | 287 mm  |
| Bulb Diameter (BD)    | 15 mm   |
| Radiating Length (RL) | 212 mm  |
| Base Material         | ceramic |
| Wattage               | 14 W    |
| Current               | 425 mA  |
| Voltage               | 34 V    |

**Table 3.** Ozone production rate

| Number of lamps on | Voltage [V] | Ozone rate [mg/min] |
|--------------------|-------------|---------------------|
| 1                  | 34          | 45.6                |
| 2                  | 68          | 52.8                |
| 4                  | 136         | 57.6                |

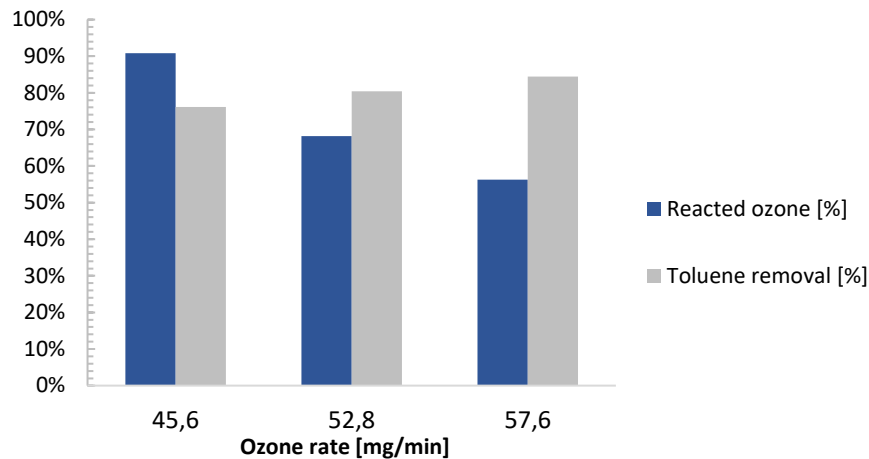
### 3. Results and discussion

In **Figure 2** are reported the results in terms of toluene removal and reacted ozone percentages as function of the ozone dose. Increasing the applied voltage from 34 to 136 V, which resulted corresponding to an increasing of ozone rate from 45.6 mg/min to 57.6 mg/min, the removed toluene moved from the 76% to the 84%. In the same time, the reacted ozone decreased from 91% to the 56%.

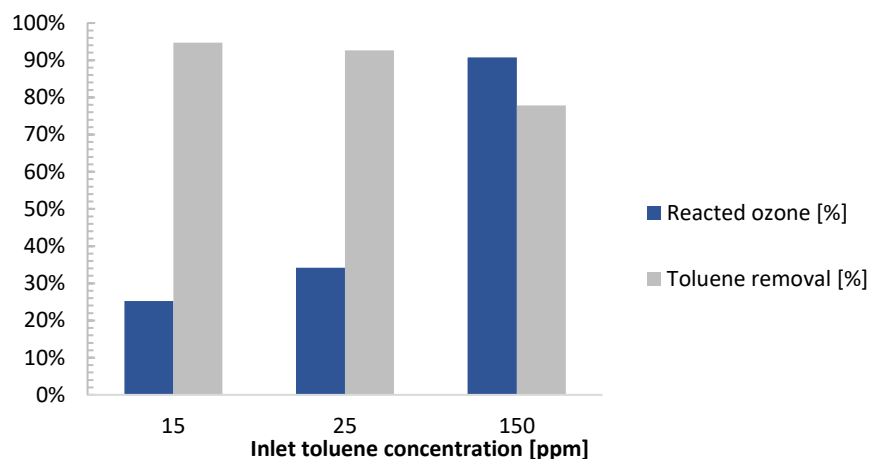
Toluene removals up to 84% were obtained with regards to the contaminated stream at concentrations between 150 and 170 ppm, corresponding to an incoming load of 7,34 – 8,32 mg of toluene per minute. For the range of toluene concentration between 150 and 170 ppm, in the investigated operating conditions, the ozone did not constitute a limiting factor. For this reason, the efficiencies in terms of toluene removal resulted quite similar varying the applied power. In **Figure 3** are reported the results as a function of the incoming

toluene concentration, for an applied voltage of 34 V (“A” lamp on). The results showed, even for an incoming concentration of 150 ppm, a removal of 78% of toluene, obtained turning on only the “A” lamp. The flow rate and, consequently, the residence time were maintained constant for the whole set of

experiments. The preliminary results obtained in the above-mentioned operating conditions highlighted the removal of the odours for the investigated streams.



**Figure 2.** Toluene removal efficiencies and reacted ozone as a function of the ozone rate



**Figure 3.** Toluene removal efficiencies and reacted ozone as a function of the inlet toluene concentration

#### 4. Conclusions

The preliminary results of the present work highlighted as the investigated process may be suitable with the aim at treating waste gas from environmental and industrial facilities in which are involved processes of organic degradation. In the investigating conditions, referring to inlet toluene concentrations in the range between 10-20 ppm of toluene, the results showed as the reactor may be considered over dimensioned; the ozone in the outlet stream, indeed, resulted over the 60% of the ozone produced. For incoming concentration equal to 150 ppm, also with the lowest ozone dose, a significant removal of toluene was obtained. The combination

with an additional treatment may be implemented, with a view at reducing the emissions of oxidants and maximizing the removal of organic compounds.

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