Removal of emerging contaminants in wastewater by sonolysis, photocatalysis and ozonation

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Abstract

Three different advanced oxidation processes (AOPs) were applied to investigate the removal of emerging contaminants (ECs) i.e. sulfamethoxazole (SMX), diclofenac (DCF) and carbamazepine (CBZ) in synthetically prepared aqueous solutions. The degradation of these substances was carried out by ozonation, sonolysis and photocatalytic oxidation, as well as by different combinations of these processes. The objectives of this work were to evaluate the removal efficiency of each method and to assess the performance variation of sonolysis in combination with other AOPs. The best performances were achieved by sonocatalysis, which resulted in the removal of the selected pharmaceuticals in the range between 37% and 47%. Under similar experimental conditions, the removal of the selected ECs by single compounds by ozonation was slightly lower than the removal of respective compounds in the mixture. Moreover, pseudo first-order removal rate constants of photocatalytic mineralization were determined as 9.33×10^{-2}, 4.90×10^{-3}, 1.06×10^{-2} min^{-1} for SMX, DCF and CBZ, respectively.

Keywords: Advanced oxidation processes, catalyst, ozone, ultrasound, UV irradiation.

1. Introduction

Pharmaceuticals and personal care products (PPCPs) have appeared as a new class of pollutants which have been frequently detected at trace levels in wastewater effluents, rivers, lakes, seawater, groundwater and drinking water. They may accumulate in soils and sediments due to their physical and chemical properties. The occurrence of these organic emerging contaminants (ECs) in surface water and groundwater has raised an increasing attention to many researchers in the field of water engineering. With the development of advanced analytical techniques, most of these ECs at low concentrations have recently been quantified and acknowledged as potential ecological risk.

Studies on the occurrence of pharmaceuticals show that sulfamethoxazole (SMX), diclofenac (DCF) and carbamazepine (CBZ), which are among the most widely used, are present in considerable concentrations in the environment (Ternes, 1998). Diclofenac and carbamazepine are non-steroidal anti-inflammatory drugs, used against pain, fever and inflammation, and can be used without prescription. They are ubiquitously present in both municipal wastewater effluents and receiving surface waters ranging from ng/L to mg/L (Ternes, 1998; Heberer, 2002b). As part of the group of sulfonamides, sulfamethoxazole is a bacteriostatic antibiotic, largely used for diverse types of illness, thus causing the release of both unmetabolized and active metabolites that have a strong potential to affect organisms (Nicolle, 2002; Dantas *et al.*, 2008). It can be found in surface waters at concentrations from 30 to 480 ng/L (Herber *et al.*, 2008; Luo *et al.*, 2010) and as high as 2000 ng/L in many municipal wastewater treatment plants (Andreozzi *et al.*, 2003). The concentrations of SMX, DCF and CBZ in wastewater were reported in the range of 0.02 to 0.58 µg L^{-1}, 0.01-510 µg L^{-1} and 0.1-1.68 µg L^{-1}, respectively (Klavarioti *et al.*, 2009). Biodegradability of these compounds is generally recognized to be low and most of them cannot be removed from wastewater by conventional treatment methods (Ternes, 1998; Kümmerer *et al.*, 2000; Heberer, 2002a).

At present, it has been widely demonstrated that advanced oxidation processes (AOPs), on the basis of a series of selective and fast oxidative reactions through the application of combinations of reactive oxidants, are effective in the removal of PPCPs (Boncz *et al.*, 2003; Gogate and Pandit, 2004; Kunkel and Radke, 2008; Oller *et al.,* 2011; Langenhoff *et al.*, 2013). The efficacy of AOPs depends on the production of extremely reactive and unselective species such as hydroxyl radicals ($^\bullet$OH), which degrade recalcitrant molecules into biodegradable oxidation products and eventually convert them into CO_2, H_2O, and inorganic ions (Langenhoff *et al.*, 2013).

Recent studies report the removal of SMX, DCF, and CBZ by different AOPs (Doll and Frimmel, 2005; Dalrymple *et al.*, 2007; Dantas *et al.*, 2008; Beltrán *et al.*, 2009; Beltrán *et al.*, 2012; Carbonaro *et al.*, 2013). The applicability of ozonation and advanced oxidation technologies to remove endocrine disrupting chemicals, pharmaceuticals and personal care products in water effluents was reviewed in detail by Esplugas *et al.* (2007). A very recent critical review by Hübner *et al.* (2015) also reports on the ozonation of several ECs and evaluates the persistence of transformation products.

The objective of this study was to investigate the removal of DCF, SMX, CBZ by three AOPs, specifically, sonolysis, ozonation and TiO_2 photocatalysis. Combinations of these AOPs were also investigated to compare the efficiencies of combined processes on the basis of the removal of target organic contaminants.

2. Materials and methods

2.1. Chemicals

In this study, diclofenac (DCF, $C_{14}H_{10}Cl_2NNaO_2$, molecular weight: 318.13 g), sulfamethoxazole (SMX, $C_{10}H_{11}N_3O_3S$, molecular weight: 253.28 g) and carbamazepine (CBZ, $C_{15}H_{12}N_2O$, molecular weight: 236.27 g) were used as model compounds for pharmaceuticals. They were spiked into distilled water to prepare working solutions with concentrations ranging from 4 to 10 mg L^{-1} to be used for experiments. The concentrations detected in real wastewater of this type of pharmaceuticals, as previously mentioned, are normally in range of 0.02 to 0.58 µg L^{-1}, 0.01-510 µg L^{-1} and 0.1-1.68 µg L^{-1}, for SMX, DCF and CBZ respectively. As this work was carried out on synthetic aqueous solutions, also based on previous studies from the authors (Naddeo *et al.*, 2015), higher concentrations were chosen for analytical requirements, in order to assess the process efficiency within a measurable time scale as well as an accurate analytical determination with the applied methods at bench scale. Moreover, as the removal of such high concentrations by sonolysis demonstrated zero-order kinetics in previous studies (Naddeo *et al.*, 2009b), the prediction of treatment efficiency at lower concentrations in wastewater is reasonable.

2.2. Experimental set-up

Ozonation was conducted with a UV system (model Ozone - Procom srl), which produced ozone by UV splitting of the oxygen molecules in the provided ambient air. The air flow was constant over time and the ozone working rate was determined by Standard Method 2350E 106 (Ozone Demand/Requirement-Semi-Batch Method). The ozone dose was set at 3.3 g h^{-1} for the individual process (Naddeo *et al.*, 2015) and treatment duration was controlled within 40 min. Photocatalytic oxidation experiments were performed using 0.5 g L^{-1} of Degussa P-25 TiO_2 which was irradiated from the top by a 125-W BLF lamp. The light intensity measured by potassium

ferrioxalate actinometry was 4.7×10^{-7} Einstein•s^{-1}. The optimal TiO_2 dose was determined based on previous studies (Uyguner *et al.*, 2007). The TiO_2 suspension was continuously stirred by a magnetic stirrer. Sonolysis experiments were conducted with a Sonics Vibracell TM VCX-750 (Sonics Material Inc., USA) ultrasound generator operating at a fixed frequency of 20 kHz and equipped with a titanium horn with a tip of 1.3 cm diameter. The applied power was set constant at 60% of amplitude. The tests were carried out at different sonication times (10 and 30 min) with an ultrasonic density of 370 W L^{-1}. A Thermocouple immersed in solution was employed to measure bulk temperature of the sample that was kept constant by the use of a water bath. The same devices were used to study the combined ozone/sonolysis process and sonolysis/TiO_2 photocatalysis (i.e., sonocatalysis). Operating conditions are given in Table 1.

Table 1. Investigated operating conditions for combined processes

	Combined process	Sonolysis amplitude	Treatment time	
O_3 Dose	1.3 g h^{-1}	O_3+US	30%	20 min
	2.4 g h^{-1}			
	3.3 g h^{-1}		60%	40 min
TiO_2 Dose	0.5 mg L^{-1}	TiO_2+US	60%	10 min
				30 min

The combined ozone/sonolysis tests were performed without pH adjustment of the synthetic solutions. The natural pH of the samples was between 4.5 and 5.0, which decreased to a pH in the range of 3.5 and 4.0 after the application of ultrasound. All the tests were performed in triplicate, using 200 mL of sample at different concentrations.

2.3. Analytical methods

The quantification of the selected ECs was conducted with UV-vis spectrophotometry (Perkin Elmer Lambda 12). Concentrations of DCF, SMX and CBZ were analyzed by 4000 Q Trap LC-MS/MS System (Applied Biosystems, Foster City, USA) with electrospray ionization (ESI) − positive and negative ionization modes. In the LC MS/MS, carbamazepine and diclofenac were analyzed in ESI-positive mode using a mobile phase composed of A: 0.1% formic acid in water and B: acetonitrile-water (1:1 v/v) solution. An Inertsil ODS-3 C18 column was used for the separation step (Secondes *et al.*, 2014). Temperature all throughout the process and pH at certain points were monitored by pH211 microprocessor pH meter (Hann Instruments, USA). Shimadzu VWP-TOC Total Organic Carbon analyzer was used to determine the dissolved organic carbon contents (DOC) of the samples. Moreover, the quantification of anions formed during photocatalytic oxidation was carried out using Dionex ICS-3000 Ion Chromatography.

3. Results and discussion

### 3.1. Ozonation

The performance of ozonation on the degradation of pharmaceuticals was evaluated based on the removal efficiency in the presence of a single compound as well as in a mixture of three compounds (Naddeo *et al.*, 2015). After 40 minutes of reaction, ozonation at a dosage of 10 mg O_3 L^{-1} resulted in approximately 51%, 73%, and 59% removal of SMX, DCF and CBZ, respectively. These results are consistent with those reported by Naddeo *et al.* (2015). The highest removal rate was observed for DCF, followed by CBZ. This evidence suggests that a lower ozone dosage is needed to remove DCF and CBZ than SMX. This trend is likely associated with the distinct molecular structure of the three compounds. The aromatic amino groups in DCF and SMX are likely exposed to the ozone attack (Dantas *et al.*, 2008), but different ring positions are responsible for the highest reactivity of DCF upon SMX. In the case of CBZ, ozone tends react rapidly with the double bonds in yielding several ozonation products containing quinazoline-based functional groups (McDowell *et al.*, 2005). The high reactivity of CBZ with ozone has a second order rate constant of 3×105 M^{-1} s^{-1} (Huber *et al.*, 2003). The experimental activity performed on the mixture of pharmaceuticals showed that, despite the simultaneous presence of all target compounds, a significant reduction of DCF was obtained after 40 minutes, as already found in previous studies (Naddeo *et al.*, 2015). Under similar experimental conditions, the removal of single compounds by ozonation was slightly higher than the removal of respective compounds in the mixture. This was due to the competitive kinetics of three compounds reacting with ozone. In addition, the ozonation reaction can proceed via both direct and indirect pathways. In the direct ozonation, the ozone molecule reacts with the target compound, while in the indirect ozonation, the reaction take place in the presence of hydroxyl radicals, which are the products of the dissociation of ozone in aqueous solution at high pH values (Rodríguez *et al.*, 2008). The direct reactions between ozone and organic compounds in aqueous solutions are essentially limited to unsaturated and aromatic compounds, and the reactivity is governed by the dipolar structure of the ozone molecule. It is very well known that the degradation by ozone can lead to the complete removal of the selected emerging compounds under optimized conditions, but an accumulation of ozonation by-products (e.g., phenolic intermediates and carboxylic acids) in solution can also be observed (Dantas *et al.*, 2008; Hübner *et al.*, 2015).

3.2. Photocatalytic oxidation

Photocatalytic oxidation of pharmaceuticals in the presence of a single compound as well as in a mixture of three was investigated. UV spectra of the photocatalytic degradation profile of 10 mg L^{-1} SMX, CBZ and DCF showed a higher removal efficiency with respect to increasing irradiation periods. After 60 mins of irradiation almost complete removal of the broad peak around 260-300 nm was observed. Oxidation leads to the formation of organic intermediate compounds. It would be possible to detect the target compounds by UV absorbance measurement only in the early stage, since these are in higher concentration than the oxidation intermediates. Moreover, DOC analysis could be used to verify the presence of all organic compounds or their mineralization (Rizzo *et al.,* 2009). Under experimental conditions where photocatalytic removal of DCF (10 mg L^{-1}) was studied, 23% and 53% removal of DCF was observed after 30 and 60 mins of UV irradiation, respectively (Figure 1(a)). The same catalyst was studied by Achilleos *et al.* (2010) for the removal of 10 mg L^{-1}DCF: 250 mg L^{-1} of Degussa P25 resulted in 61% conversion of the target compound after 60 minutes. In another study, 50 mg L^{-1} of DCF was almost totally removed using 200 mg $L^{-1}$of TiO_2 loading under extended irradiation (Pérez-Estrada *et al.*, 2005). Such outcomes suggest the importance of the irradiation conditions, not only in terms of treatment time but also with reference to the experimental set up used for the experiments. The same experimental conditions resulted in higher removal of SMX (Figure 1(b)), which reached 55% and 82% after 30 and 60 minutes treatment, respectively. Photocatalytic oxidation studies by Beltrán *et al.* (2008) with SMX in the range of 30 to 80 mg L^{-1}were carried out using 1.5 g L^{-1} TiO_2 where approximately 100% removal of target compound was achieved in less than 20 min (Beltrán *et al.*, 2008). Using different reaction conditions and TiO_2 loading, various removals were reported in literature (Abellán *et al.*, 2007; Nasuhoglu *et al.*, 2011; Xekoukoulotakis *et al.*, 2011). The removal yields obtained for CBZ (Figure 1(c)) were comparable to those observed for SMX. The photocatalytic removal of the mixture of pharmaceuticals containing 10 mg L^{-1} of DCF, SMX and CBZ revealed 20% of DOC removal after 60 min (Figure 1(d)). Even from the initial periods of photocatalysis, the concentration of both chloride and sulfate gradually increased with irradiation time. On the other hand, the nitrate level increased steadily from 0 to 60 minutes.
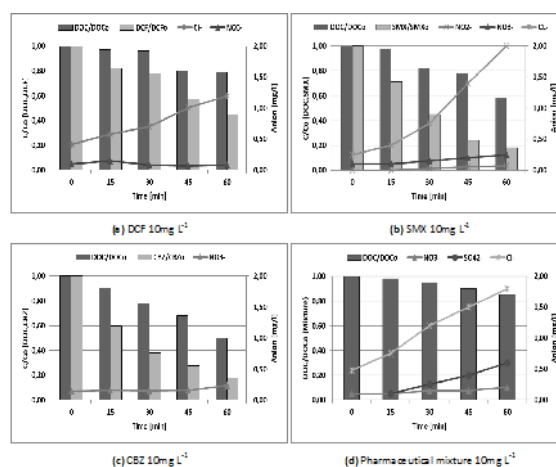
Figure 1. DOC removal, anion and pharmaceutical concentrations during photocatalytic oxidation

As for the removal rates, the photocatalytic degradation of pharmaceuticals generally followed pseudo first-order kinetics. The photocatalytic removal rate constants (k) of each compound were evaluated and presented in Table 2. As pointed out in previous studies (Jelic *et al.,* 2013; Rao *et al.,* 2013; Wang *et al.,* 2018), the photocatalytic oxidation of carbamazepine also revealed pseudo first-order rate constants that confirmed a beneficial effect on the process kinetics due to the increased number of TiO_2 active sites. It should be highlighted that for higher concentrations these effects tended to stabilise. This behavior is a function of the reactor and the used TiO_2 type and loading (Doll and Frimmel, 2004).

Table 2. Pseudo first-order removal rate constants for the photocatalytic degradation of SMX, DCF and CBZ in terms of both DOC and concentration of Emerging Contaminant (EC) (k: rate constant, R^2>0.90)

	KDOC [min^{-1}]	KEC [min^{-1}]
10 mg L^{-1} SMX	9.33×10^{-3}	2.59×10^{-2}
10 mg L^{-1} DCF	4.90×10^{-3}	1.28×10^{-2}
10 mg L^{-1} CBZ	1.06×10^{-2}	2.70×10^{-2}
Mixture	3.60×10^{-3}	---

DOC removal rate constants of ECs followed the order of CBZ>SMX>DCF>mixture (Table 2). In general, mineralization rate was slower than that corresponding to the target compound removal. This is due to the presence of oxidation products in the medium. Considering that DOC embraces the entire organic load of the samples, not only the degradation of the target EC, but also the global degradation of all compounds in the solution is measured. UV254 parameter was chosen to represent aromaticity removal of the residual substrate as well as the reaction intermediates. In a recent study by Jelic *et al.* (2013), pseudo first-order rate constants corresponding to photocatalytic degradation of CBZ (10 mg L^{-1}) was reported as 1.75×10^{-2} min^{-1}. Upon UV-A irradiation (at 25 W L^{-1} intensity) of CBZ and TiO_2 solution in pure water, a DOC reduction of 45% and a CBZ substrate conversion of 75% were observed after 120 mins. In another study conducted by Miranda-Garcia *et al.* (2011) photocatalytic degradation of 15 ECs at low concentrations was investigated in simulated and real municipal wastewater treatment plant using TiO_2 immobilized on glass spheres where 85% of the compounds was degraded within 120 min of illumination time, depending on the water matrix. The results showed that using a 5 mg L^{-1} suspension of Degussa P25 TiO_2 led to a decrease in the removal of the contaminants except for ofloxacin, hydroxybiphenyl, diclofenac, progesterone and triclosan which were degraded in less than 120 min. On the other hand, photocatalytic mineralization rate of an urban wastewater effluent contaminated with a mixture of pharmaceutical compounds composed of amoxicillin (10 mg L^{-1}), carbamazepine (5 mg L^{-1}) and diclofenac (2.5 mg L^{-1}) was found to be really slow ($t_{1/2}$=86.6 min) when compared to those of the same

pharmaceuticals spiked in distilled water ($t_{1/2}$=46.5 min) (Rizzo *et al.*, 2009).

Photocatalysis is a degrading process and, hence, several intermediates of varying reactivity are likely to be formed prior to mineralization; some of them are expected to be quite recalcitrant to further decomposition, suggesting that the complete mineralization rate should be slower than the degradation rate of ECs. Photocatalytic mineralization rate constant of single compounds as determined by DOC removal was higher than the removal rate constant of the mixture.

3.3. Sonolysis-enhanced advanced oxidation processes

3.3.1. Sonolysis

Preliminary studies were performed with model compounds to optimize sonolysis operating conditions. The results showing the removal of each compound after sonolysis application for 10 and 30 min are shown in Figure 2. Using 4 mg L^{-1} mixture (Figure 2(a)), application of sonolysis for 10 min led to 12%, 3% and 13% removal of SMX, DCF and CBZ, respectively. Extending the application time to 30 min resulted in an enhanced removal of 27%, 26% and 29% of the respective ECs. With the increase in mixture concentration to 10 mg L^{-1} (Figure 2(b)), no significant change was observed after 10 min application of ultrasound. However, after 30 min, 13%, 9% and 2% removal in concentrations of SMX, DCF and CBZ were attained. Recent research on the degradation of SMX, DCF and CBZ as single compounds revealed no significant change in the removal rate of compound and DOC, although conversion of the compound to more readily biodegradable forms could be achieved (Naddeo *et al.*, 2010).
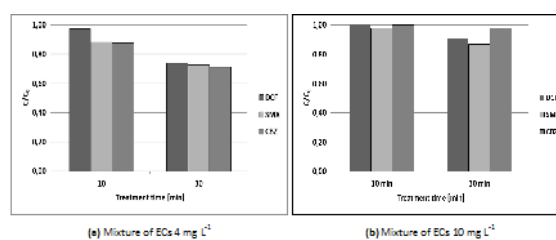
Figure 2. Treatment process for the removal of mixture of ECs (60% amplitude)

Different results were reported in literature regarding the application of sonolysis for the removal of SMX, DCF and CBZ. However, most of the studies were based on sonolysis application for the removal of single compounds in aqueous solutions. The simultaneous presence of different pharmaceuticals could affect the ultrasonic degradation of respective compounds in single solutions that was assumed to occur by the hydroxyl radicals present in the bubble–liquid interface due to the hydrophobic and low volatile properties of the target compounds (Méndez-Arriaga *et al.*, 2008; Liwei Hou, 2013).

3.3.2. Combined ozonation and sonolysis

Tables 3 and 4 present the results of the combined ozonation/sonolysis process on the selected pharmaceuticals both as single compounds and in mixture.

Table 3. Removal % of single compounds of SMX, DCF and CBZ (10 mg L^{-1} each) by combined ozonation and sonolysis

Treatment		SMX [% removal]		DCF [% removal]		CBZ [% removal]	
Ozone dose [g/h]	Ultrasound amplitude [%]	20 min	40 min	20 min	40 min	20 min	40 min
1.3	30	30	50	54	75	28	44
1.3	60	42	51	62	86	32	41
2.4	30	38	55	63	89	41	49
2.4	60	44	52	72	91	41	46
3.3	30	26	34	66	90	47	54
3.3	60	54	61	80	94	50	52

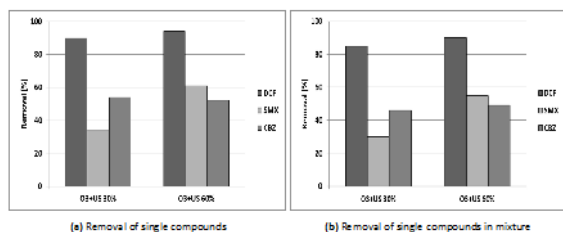Table 4. Removal % of SMX, DCF and CBZ (10 mg L^{-1} each) mixture by combined ozonation and sonolysis

Treatment		SMX [% removal]		DCF [% removal]		CBZ [% removal]	
Ozone dose [g h^{-1}]	Ultrasound amplitude [%]	20 min	40 min	20 min	40 min	20 min	40 min
1.3	30	22	45	37	62	21	35
1.3	60	36	45	54	85	29	37
2.4	30	33	50	54	84	34	43
2.4	60	41	46	64	88	35	42
3.3	30	21	30	59	85	40	46
3.3	60	51	55	73	90	44	49

In both cases, the combined effect of ozonation and sonolysis synergetically improved the removal efficiency of the studied compounds. This is due to the fact that the ultrasonic waves homogenized the sample and improved the solubility of ozone by high energy and vibration, as extensively proved in other studies (Kidak and Dogan, 2012).
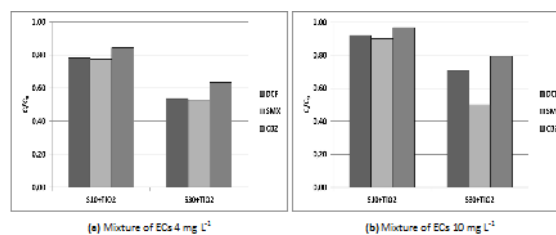
For the three pharmaceuticals, respective removal of the target compound in the mixture also relevantly increased with increasing ozone dose as well as time. In general, the percentage removal of each emerging compound in the mixture is lower than the removal percentage of the compound in a single-compound matrix. The results carried out at 60% amplitude confirmed those reported by Naddeo *et al.* (2015).

Figure 3 compares pharmaceutical removal after the application of the combined ozonation/sonolysis process both in single solution and in mixture.

Higher removals were attained using the combined process operating under high ultrasonic amplitude. As the amplitude increased from 30% to 60%, the removal of SMX and DCF improved up to 61% and 94%, respectively. The observed synergy was mainly due to an enhanced rate of O_3 diffusion to the bulk solution and into the cavity bubbles, which upon collapse lead to thermal decomposition of the contents for an additional and major route of $^{\bullet}$OH production.

Figure 4. Treatment process for the removal mixture of ECs (S10+TiO$_2$: 10 min sonolysis in the presence of TiO$_2$, S30+TiO$_2$: 30 min sonolysis in the presence of TiO$_2$)

The increase in efficiency in hybrid processes is related to factors such as enhanced mass transfer rates of gases and solutes, enlarged surface areas of solids, excess bubble nuclei and excess $^{\bullet}$OH formation. Hybrid processes of ozone and sonolysis were shown to be effective, as they provide complete degradation and appreciable mineralization of the compound (Naddeo *et al.*, 2009a). It was reported that approximately 5%, 30% and 50% mineralization was achieved by 100 W L^{-1}, 200 W L^{-1} and 400 W L^{-1} power densities within 60 min,

Figure 3. Comparison of the percent removals of single compounds and mixture of SMX, DCF, CBZ by combined ozonation (O$_3$) and sonolysis (US) at 30 and 60 % of amplitude (ozone flow 3,3 g h^{-1}, time 40 min)

at an initial concentration of 40 mg L^{-1} of DCF (Naddeo *et al.*, 2009a). Similar results were reported by Hou *et al.* (2013) and Guo *et al.* (2015) for the removal of SMX under various operating conditions.

3.3.3. Sonocatalysis

To study the effect of TiO$_2$ on the sonolytic degradation of the selected pharmaceuticals, sonolysis experiments were performed in the presence of 0.5 mg mL^{-1} TiO$_2$. At initial concentration of 4 mg L^{-1} and 10 minutes sonocatalysis of the EC mixture revealed 23%, 22% and 15% removal of SMX, DCF and CBZ respectively. Increasing sonication time to 30 min resulted in 47%, 46% and 37% removal in respective pharmaceuticals, as shown in Figure 4.

This evidence highlights a synergistic effect in the degradation of the studied compounds by the combined effect of catalyst and sonolysis, which was attributed to the additional cavitation activity (Méndez-Arriaga *et al.*, 2008). Ultrasound has a mechanical effect that may lead to the fragmentation of catalyst and the consequent increase of the surface area and active sites. Another possible effect is the increase of the mass transfer between the reactants and the catalyst (Pandit *et al.*, 2001). In contrast to our findings, no significant difference on the removal efficiency of SMX (50 mg L^{-1}) was reported by Hou *et al.* (2013) in the presence of ultrasound (85.7 W L^{-1}) and Fe$_3$O$_4$ catalyst (0.3 g L^{-1}). On the other hand, in parallel with the decrease in concentration, for both mixtures (4 and 10 mg L^{-1}), UV-vis spectra specifically in 250-300 nm region also revealed a slight decrease in absorbance intensity after the application of sonolysis and sonocatalysis (Figure 5). Although sonolysis and sonocatalysis resulted in around 10% and 40% removal in the concentration of ECs, smooth decrease of the UV-vis spectra accompanied by any significant change in DOC values (data not shown) indicated inefficient mineralization and formation of new products by the degradation of SMX, DCF and CBZ.
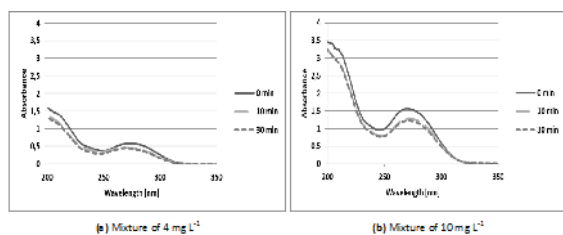

Figure 5. UV-vis spectra of mixture during sonocatalysis: sonication time 10 and 30 min

4.   Conclusion

AOPs are effective in the removal of the most widely used pharmaceuticals, i.e., SMX, DCF and CBZ, which have been recognized as ECs. Different results were obtained as a consequence of different operating conditions. The simultaneous presence of selected compounds in mixture led to a slight reduction in the removal efficiency provided by 40 minutes of ozonation. The process yields were found to be enhanced by the combined application of ozone and ultrasound. The combined ozonation and sonolysis process resulted in DCF elimination in the range of 90 to 94% according to the applied ultrasonic amplitude. The photocatalytic removal of the mixture of pharmaceuticals containing 10 mg L^{-1} of DCF, SMX and CBZ revealed 20 % of DOC removal after 60 min. Pseudo first order removal rate constants of photocatalytic mineralization were determined as 9.33×10^{-2}, 4.90×10^{-3}, 1.06×10^{-2} min^{-1} for SMX, DCF and CBZ, respectively. On the other hand, sonocatalysis results showed that, despite the reduction in target compound concentrations, no significant variation occurred as DOC, indicating inefficient mineralization and the formation of other products from the degradation of ECs. The formation of intermediates was confirmed as one of the most important issue related to the application of AOPs. Further studies should be addressed to the characterization of the products from the treatment of different pharmaceuticals, either as single compounds or in mixture, in order to extrapolate research findings to the whole class of pharmaceuticals and promote the wider application of AOPs.

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