

# ADSORPTION OF HEXAVALENT URANIUM ON DUNITE

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## ABSTRACT

Pollution of the environment with uranium and associated health effects to human have recently become of major concern, particularly due to the use of depleted uranium in armourbreaking bullets. Indeed, uranium in environmentally significant concentrations is found near to uranium mining and processing facilities and usually involves large volumes of wastewater. Removal of uranium from such large volumes of wastewaters will require a cost effective remediation technology. Conventional wastewater treatment technologies usually rely on mineral adsorbents and chemical flocculating agents. On the other hand chemical behaviour and migration of uranium species in the geosphere is strongly governed by adsorption/desorption phenomena on the underlying rock formations. Hence, studies regarding uranium adsorption on natural minerals and the evaluation of the corresponding thermodynamic data is of fundamental importance with respect to the treatment of contaminated waters and uranium migration in the geosphere.

The present paper reports about the adsorption of hexavalent uranium on dunite at various experimental conditions (e.g. uranium concentration, amount of adsorbent, ionic strength, pH, temperature and contact time) and discusses the effect of these parameters on uranium adsorption. Evaluation of the experimental data shows that the optimum pH regarding uranium adsorption on dunite is about 6.5. The experimental adsorption data are well fitted by the langmuir isotherm and there is a linear correlation between adsorbent mass and amount of uranium, indicating on the formation of inner-sphere complexes. Moreover, adsorption experiments at various temperatures indicate on a spontaneous, entropy-driven processes and kinetic measurements show that the adsorption process follows a first order rate expression.

**KEYWORDS:** Uranium, Dunite, Sorption, Isotherms, Thermodynamics.

## INTRODUCTION

Uranium, a toxic and weak radioactive heavy metal, is relatively widespread in the environment, and as a naturally occurring element it is found at low levels in virtually all rocks, soils and waters (Shawky *et al.*, 2005). Increased amounts of uranium in the biosphere originate from mining, beneficiation of uranium ores and various processes related to the production of nuclear reactor fuel as well as the use of depleted uranium (DU) in civil and military applications (Bleise *et al.*, 2003). Uranium is of fundamental importance in the nuclear fuel cycle, where it starts as a source and ends up as a final waste component. Pollution of the environment with uranium and associated health effects to human have recently become of major concern, particularly due to the use of DU in armour-breaking bullets. Nevertheless, uranium in environmentally relevant concentrations is found near to uranium mining and processing facilities and usually involves large volumes of wastewater. In aquatic solutions and aquifers uranium exists predominantly in its hexavalent oxidation state e.g.  $UO_2^{2^+}$ .

Hexavalent uranium is highly mobile and migrates basically in the form of very stable carbonate complexes under near surface conditions (Kilincarslan and Akyil, 2005).

Removal of uranium from large volumes of wastewaters requires a cost effective remediation technology. Several methods are utilized to remove uranium from wastewater and process effluents. These include reduction followed by chemical precipitation, ion exchange, reduction, electrochemical precipitation, solvent extraction, membrane separation, biosorption etc. However, these technologies are both costly and ineffective, particularly when the concentration of uranium is a very low (Blazquez *et al.*, 2005). Adsorption of uranium on mineral adsorbents is an effective and versatile method for removing uranium. Up to now, numerous experimental studies on uranium adsorption on various minerals and rocks have been published (Kilincarslan and Akyil, 2005; Waite *et al.*, 1994; Ames *et al.*, 1983; Aksoyoglu, 1989; Wersin *et al.*, 1994; Donat and Aytas, 2005; Arnold *et al.*, 1998; Zuyi *et al.*, 2000; Zhijun *et al.*, 2004; Hongxia and Zuyi, 2002).

This study is focused on uranium adsorption on dunite, which is a very abundant mineral. Dunite is an igneous, plutonic rock, of ultramafic composition, with coarse grained or phaneritic texture. The mineral assemblage is typically greater than 90% olivine with minor pyroxene and chromite. Dunite is the olivine rich end member of the peridotite group of mantle-derived rocks. The present paper reports about the adsorption of hexavalent uranium on dunite at various experimental conditions (e.g. uranium concentration, amount of adsorbent, pH, temperature and contact time) and discusses the effect of these parameters on uranium adsorption.

### EXPERIMENTAL

A periodically mixed batch technique was selected for the batch adsorption experiments. All experiments were carried out under normal atmospheric conditions at  $25 \pm 1$  °C. Test solutions were prepared by dissolution of uranyl nitrate (UO<sub>2</sub>(NO<sub>3</sub>)<sub>2</sub> 6H<sub>2</sub>O, 99.99%, Merck Co) in aqueous solution. The ionic strength (0.1 M and 1.0 M) in the test solutions was adjusted by addition of sodium perchlorate (NaClO<sub>4</sub>, Aldrich Co). Solutions without background electrolyte (electrolyte-free solutions) are denoted by I = 0.0 M. Dunite used in this study originated from a mountainous area of Cyprus (Troodos massif). Prior application the material was sieved and the particle fraction of 80 mesh was selected for the adsorption experiments and was used without any further purification or other pre-treatment. The BET surface area of the adsorbent (granulated material) was measured by N<sub>2</sub>-adsorption (Micromeritics Co, ASAP 2000) and has shown that dunite has small internal surface (5.7 m<sup>2</sup> g<sup>-1</sup>), indicating that adsorption of uranium occurs on its external surface. Further characterization of the material was done using FTIR (8000 Series, Shimadzu), XRD (6000, Shimadzu) and XRF (Spectrace, Shimadzu).

Immediately after the addition of 100 ml of the test solutions to the adsorbent, the bottles were shaken and left to reach equilibrium. During the equilibration period the bottles with the test solutions were shaken regularly. Following three days equilibration, the solutions were first centrifuged at 5000 rpm (Lab centrifuge, Memmert Co), then passed through a 0.45-µm Millex filter (Type GV) and the concentration of uranium in solution was determined by spectrophotometry by means of arsenazo III (Savvin, 1961).

To investigate the effect of various parameters (e.g. pH, initial uranium concentration, amount of adsorbent etc.) on uranium adsorption, five different classes of experiments were conducted. In these experiments the parameter under investigation was varied while other experimental parameters were kept constant. The effect of pH was studied in an adsorption system (0.05 g adsorbent and 100 ml of the test solution:  $[U(VI)] = 1 \times 10^{-5} \text{ mol } \Gamma^{-1}$ ) in which pH was varied between 2 and 12 by addition of HClO<sub>4</sub> or NaOH. For studying the effect of initial uranium concentration, the latter was varied between 7.5x10<sup>-5</sup> mol  $\Gamma^{-1}$  and 5x10<sup>-6</sup> mol  $\Gamma^{-1}$ , at a prefixed amount of adsorbent (adsorbent dosage = 0.05 g per 100 ml). The effect of the amount of dunite was investigated by adding different amounts of adsorbent (between 0.0005 and 0.1 g) into a 125-ml polyethylene screw capped bottle, containing 100 ml test solutions of constant uranium concentration (1x10<sup>-5</sup> mol  $\Gamma^{-1}$ ).

The effect of temperature was studied between 25 and 70 °C and measurements were carried out after an equilibration time of three days. The amount of adsorbent (0.5 g  $I^{-1}$ ), initial uranium concentration (1x10<sup>-5</sup> mol  $I^{-1}$ ) and pH in the test solutions (100 ml) were kept constant. For kinetic studies certain amount of dunite (0.5 g  $I^{-1}$ ) was mixed with uranium solution (1x10<sup>-5</sup> mol  $I^{-1}$ ). Samples withdrawn at time intervals were centrifuged and the uranium concentration was determined by photometry.

## RESULTS

#### The effect of pH

The pH of an aqueous solution is an important parameter that governs the adsorption of metal ions on mineral surfaces. Variation in pH affects speciation and stability of soluble species as well as surface properties (e.g. the charge of functional groups responsible for surface sorption). Figure 1 shows the effect of pH (in the range between 2 and 12) on the K<sub>d</sub> value and hence on the uranium removal by adsorption on dunite.

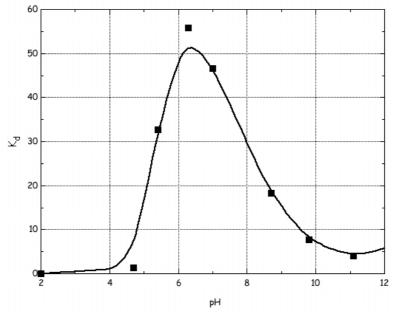


Figure 1. K<sub>d</sub> values as a function of pH for the uranium adsorption onto dunite at I=0.1M

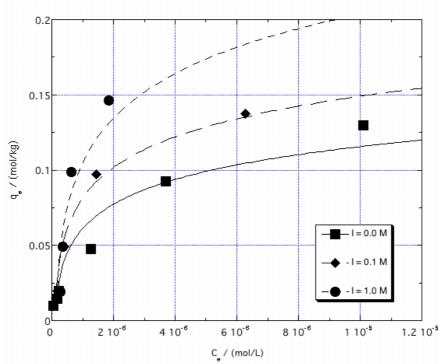
According to Figure 1, increased proton concentration leads to gradual protonation of the surface groups and destabilization of the surface adsorbed uranium species (pH < 5). On the other hand, uranium adsorption decreases in alkaline test solutions because of the higher carbonate concentrations in these solutions. Increased carbonate concentrations lead to desorption of uranium from the solid surface by stabilizing soluble uranium carbonate species (Grenthe *et al.*, 1992). The destabilization of adsorbed uranium in acidic and alkaline solutions can be described by following scheme of equations:

$$UO_2^{2+} + =S-OH \implies =S-O-UO_2^+ \implies =S-O^- + UO_2(CO_3)_2^{2-}$$

The optimum pH for the removal of uranium by dunite was found to be pH 6.5 and hence, following investigations were performed at pH = 6.5.

#### The effect of the initial Uranium Concentration

Figure 2 illustrates the effect of initial uranium concentration on adsorption of uranium on dunite (adsorption isotherms) at various ionic strengths. The experimental data indicate that the amount of uranium uptake is increased as a function of the uranium concentration in solution. The adsorption data, irrespective of the ionic strength, follow the Langmuir isotherm model (Figure 2), indicating that the maximum adsorption capacity is governed by the amount of active sites on the mineral surface.



*Figure 2.* Sorption of uranium on dunite as a function of initial uranium concentration at various ionic strengths

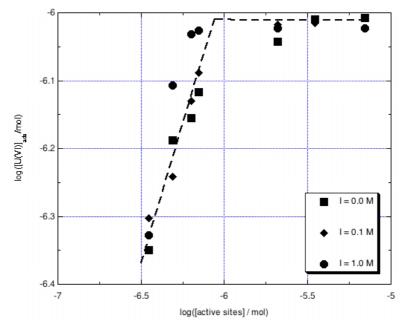
The corresponding Langmuir equation is defined as follows:

$$\frac{1}{q} = \frac{1}{q_{\text{max}} \cdot K_{\text{L}} \cdot C_{\text{e}}} + \frac{1}{q_{\text{max}}}$$

where  $q_{max}$  is the maximum adsorption capacity corresponding to complete monolayer coverage (mol kg<sup>-1</sup>), K<sub>L</sub> is the Langmuir constant related to the energy of adsorption and C<sub>e</sub> is the equilibrium concentration of the adsorbate in solution. Evaluation of the data showed no significant difference between the Langmuir parameters corresponding to solutions of different salinity. The mean values of  $q_{max}$  (mol kg<sup>-1</sup>) and logK<sub>L</sub> were calculated to be 0.07±0.03 and 6.4, respectively.

#### The effect of the amount of adsorbent

In Figure 3 the adsorbate amount is expressed in moles uranium (logarithmic scale) per mass of the adsorbent (logarithmic scale). Increasing the adsorbent concentration results in a linear increase in the uranium adsorption, indicating on the formation of inner-sphere complexes. The curves corresponding to the solutions of different salinity are identical and point out similar adsorption mechanism in solutions of different salinity. Furthermore, the absence of any significant effect of the ionic strength on the adsorption efficacy is characteristic for the formation of inner-sphere complexes. Furthermore, according to the data in Figure 3, the saturation of the adsorbent surface is reached when the amount of adsorbed uranium is almost equal to amount of the active sites of the surface. This is a clear indication on a 1:1 surface complex formation



*Figure 3.* log ([U(VI)]) as a function of log (mass<sub>adsorbent</sub>) for the uranium adsorption onto dunite at various ionic strengths

According to literature data on uranium hydrolysis,  $UO_2(OH)^+$  predominates at pH 6.5 among the soluble monomeric species of hexavalent uranium (Grenthe *et al.*, 1992). Hence, the equation for the adsorption reaction could be formulated as:

$$UO_2OH^+ + \equiv SO^- \iff \equiv SOUO_2OH$$

The equilibrium constant of the above reaction is given by following equation:

$$\mathbf{K} = \frac{[\equiv \text{SOUO}_2\text{OH}]}{[\equiv \text{SO}^-] \cdot [\text{UO}_2\text{OH}^+]}$$

where  $[UO_2OH^+]$  corresponds to the concentration of uranium in solution, [=SOUO\_2OH] equals to the amount of adsorbed uranium and [=SO<sup>-</sup>] equals to the amount of non-occupied surface sites, which are available for uranium complexation and correspond to the q<sub>max</sub> value of the Langmuir isotherm. When q<sub>max</sub> is much higer than [=SOUO\_2OH], the equilibrium constant (K) equals to the linear distribution coefficient (K<sub>d</sub>), which is a key constant used in contaminant dispersion models.

#### The effect of temperature

The temperature dependence of uranium adsorption on dunite was investigated to evaluate the thermodynamical parameters ( $\Delta G^{\circ} \Delta H^{\circ}$  and  $\underline{\Delta} S^{\circ}$ ) of the adsorption reaction based on following equations:

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$$\log K = \frac{\Delta S^{\circ}}{2.303 \cdot R} - \frac{\Delta H^{\circ}}{2.303 \cdot R \cdot T}$$

T In IZ

where T is temperature in Kelvin, R is the gas constant and K is the equilibrium constant of the adsorption reaction. The graphical presentation of the van't Hoff plot is shown in Figure 4 and the thermodynamical data evaluated are summarized in Table 1. The values for  $\Delta H^{\circ}$  and  $\Delta S^{\circ}$  were obtained from the slop and the intercept of log K vs 1/T. The positive value of  $\Delta H$  shows that the adsorption of uranium is endothermic. However, adsorption of uranium on dunite is a spontaneous, entropy-driven process. The large and positive value of  $\Delta S$  originates from the metal ion dehydration due to surface sorption.

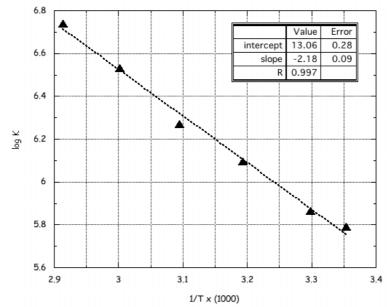


Figure 4. Effect of temperature on uranium adsorption on dunite

Table 1. Thermody	namic parameters	for the adsorption	on dunite as a	function temperature

ΔH°	ΔS°	ΔG° (KJ/mol)					
(kJ /mol)	(J /K.mol)	298K	303K	313K	323K	333K	343K
41.7 ± 2	250 ± 5	-32.8	-34.1	-36. 6	-39.1	-41. 6	-44.1

#### The effect of contact time

Figure 5 shows the relative amount of adsorbed uranium as a function of time under atmospheric conditions, pH 6.5 and I = 0.0 M (without background electrolyte). According to Figure 5 the adsorption of uranium on dunite occurs in two steps, indicating that adsorption of uranium on dunite takes place as well on the external as on the internal surface of the adsorbent. In first rapid step, which is completed within 100 minutes, almost 70% of the total uranium is adsorbed. After the second step, which is somewhat slower and is completed at about 500 minutes, the adsorption process is completed and the equilibrium corresponds to 95% adsorption efficiency. This suggests that the bonding of uranyl ion to active sites occurs preferably on the solid surface, with restricted ion diffusion towards the internal surface of the particles. The latter can be attributed to the relatively small internal surface area of the adsorbent, which is about 6 m<sup>2</sup> g<sup>-1</sup>.

The kinetics of uranium adsorption on dunite regarding the first step follows the first order rate expression given by Lagergren (Namasivayam and Senthilkumar, 1998). The apparent  $k_{ad}$  value evaluated at 25 °C and pH 6.5 is found to be about 3.0 x 10<sup>-3</sup> min<sup>-1</sup> for solutions of I = 0 M and I= 0.1 M.

#### CONCLUSIONS

The results obtained from this study lead to the following conclusions: (a) the optimum pH for uranium removal by dunite is pH 6.5, (b) the experimental data can be fitted by the Langmuir isotherm, (c) there is a linear correlation between adsorbent mass and amount of uranium which does not depend on the ionic strength, indicating on the formation of inner-sphere complexes and (d) the adsorption of U(VI) on dunite is an endothermic, entropy-driven process and follows a first order rate expression.

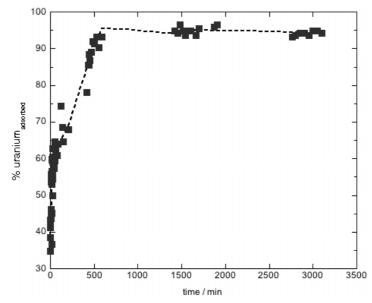


Figure 5. Effect of time of contact on uranium adsorption on dunite

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